# Fuel from the Field to the Flue: Grass fueled heating equipment combustion optimization project.

By Christopher W. Davis







VERMONT NRCS CONSERVATION INNOVATION GRANT Final Project Report – March 24, 2017

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Grantee Entity Name: Meach Cove Real Estate Trust						
Project Title: Fuel from the Field to the Flue: Grass pellet heating equipment						
combustion optimiza	ation project.					
Agreement Number	69-1644-11-08					
Project Director: Ch	Project Director: Christopher W. Davis					
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Period Covered by this Report: October 11, 2011 – December 31, 2015						
Project End Date: 9/20/2015						

#### **Deliverables**

1. Publish a final report available in printed, electronic and video formats which will summarize the information collected as a result of this project.

The report will contain the operational data for one hot water boiler and one hot air furnace both capable of burning pelletized grass fuel.

The report will contain published results of the combustion testing of several promising species of pelletized grass fuel in this heating equipment.

Provide a detailed summary and diagrams of any modifications or adjustments made to the two types of heating equipment to optimize the combustion of up to four types of pelletized grass fuel in this heating equipment.

- 2. Hold open houses, field days and tours by appointment to showcase the work being done in this project.
- 3. The heating units being evaluated as part of this project will be improved to optimize their operation when using more than one species of pelletized grass. The modifications will be detailed and included in the project report.
- 4. Collaborate with the manufacturers of the two heating units to incorporate modifications that resulted in improved performance into their production designs.
- 5. Evaluate, analyze and report on the composition, combustion and ash production of up to four species of grass fuels. This information will be useful to farmers who wish to grow grass for use as pelletized fuel for Vermont and the region. The information will also be useful to anyone wishing to make grass pellet fuel.
- 6. Conduct continued evaluation and provide updates on the heating equipment after the completion of this project. Provide access to the equipment by appointment.

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#### **Executive Summary**

This project identified and evaluated production heating equipment in the 100,000 – 500,000 BTU output range that had features that would support burning grass biomass fuels in a 1/4" pellet or a 2" diameter "puck" size. We learned that the cost to produce a larger format puck was significantly less to produce than a 1/4" diameter pellet (Wilson, 2014) so we searched for boilers that could handle both fuel sizes which would make the boiler more versatile for facility operators.

Our project took longer than anticipated due to the difficulty locating a production boiler in the < 500,000 BTU/Hour size with the features we identified as necessary to effectively handle grass biomass fuel. We requested an extension to the original September, 2013 grant deadline until September, 2014. We experienced additional delays getting the boiler we purchased certified for operation and we were granted an additional extension of the project end date until September, 2015.

The pricing for two biomass heating units (one hot water boiler and one forced hot air furnace) exceeded the available grant funding so we opted to proceed with just one U.S. made hot water boiler rated at 350,000 BTU/Hour. An Evoworld HC 100 Eco wood chip boiler was purchased and installed in a 4,500 square foot building at Meach Cove in January, 2014.

We met all of the goals and objectives for this project by successfully demonstrating that locally grown grass biomass could be burned efficiently, cleanly and cost effectively in a small commercial U.S. built production boiler. We were surprised that even poor quality mulch hay or agricultural crop residue performed as well or better in the Evoworld boiler than some of the perennial grass species that were grown for their potential as a heating fuel. Other farm operators, small commercial business owners or institutions would benefit from the findings in this report should they wish to use a renewable grass biomass fuel to heat their buildings. We also posted this information on the website created for the project, hosted tours, student visits, open houses, and recorded TV and video reports.

State or Federal programs that incentivize maintaining grass cover crops to reduce nutrient run off and promote converting outdated wood or petroleum fuel heating equipment for farm and small industrial operators would benefit from the findings from this project. This project demonstrated that the technology exists to burn grass biomass cleanly and efficiently in a small commercial boiler which had not been the case previously.

We recommend the continued evaluation of grass, biomass and agricultural field residue fuel sources in a variety of forms and sizes in this and similar boilers.

#### Introduction

This project began in 2011 at Meach Cove by first selecting the most promising grass species and agricultural biomass/field residue sources for fuel, then by growing, harvesting and densifying them, and finally burning them in a small commercial production boiler rated at 350,000 BTU/Hour output. We recorded the emission data while optimizing the boiler's performance on a variety of grass biomass samples.

- Christopher W. Davis, the manager of Meach Cove Farms in Shelburne, Vermont had experience operating biomass heating equipment and was the Project Director. The Project Director assisted with establishing and maintaining the 2008-13 warm season grasses for biomass study plots on the Meach Cove property that were managed by the University of Vermont Extension Service (Bosworth, Kelly 2015). Mr. Davis also assisted with the 2010-11 assessment of grass pellets as boiler fuel that was completed by BERC at the All Souls Interfaith Gathering church in Shelburne, VT (Sherman, 2011).
- Sid Bosworth, a University of Vermont Extension Service Agronomist, was responsible for the grass species test plots research that began in 2008. Meach Cove hosted one of the test plots where a variety of perennial grass species were grown and evaluated for their potential as fuel (Bosworth, Kelly, 2015).
- Christopher W. Callahan, a University of Vermont Extension Service Agricultural Engineer, assisted with the grass and biomass combustion testing and optimization conducted during this project in 2015. The conclusions he reached are summarized in his report (Callahan, 2016) and referenced throughout this report.
- Adam Dantzscher, of South Burlington, Vt., a former partner in Renewable Energy Resources, Inc., represented RER, Inc. in 2013 when they sold the Evoworld HC 100 Eco boiler to Meach Cove. Mr. Dantzscher was contracted to densify the grass and biomass into 2" diameter pucks that were tested in this project. Mr. Dantzscher also assisted with operational issues with the Evoworld boiler throughout this project.
- Dr. Jerry H. Cherney, Cornell University, Department of Crop and Soil Sciences, and Michael J. Newtown, PE, Associate Professor and Dean, Casino School of Engineering Technology, State University of New York, Canton, were consulted throughout this project and their input shaped the focus of the project.
- Louis Okonski, President, Troy Boiler Works, Inc. and Evoworld USA, located in Troy, N.Y., built, installed and supported the Evoworld boiler. Mr. Okonski and his Troy Boiler Works and Evoworld USA team were a critical resource throughout the project.

- Gus Swanson and Jim Trussler of LST Energy, Nova Scotia, Canada, developed a proof of concept boiler that they operated on grass pellets in 2010-11. Their boiler prototype was evaluated by the Nova Scotia Department of Agriculture, Truro, Nova Scotia (Dutta, 2010). Their early success with burning grass pellets in a small commercial boiler provided the inspiration for Meach Cove to seek a USDA-NRCS Conservation Innovation grant to proceed with this project.
- Bob Miller, founder of Enviro Energy in Unadilla, N.Y. (Metz, 2015), densified the Meach Cove harvested biomass into the 1/4" diameter pellets in 2011 that were tested in this project. Without Mr. Miller's production facility we would have been required to develop an alternative method to produce the grass pellets in smaller quantities or only test the 2" diameter puck form.

The goals of this project were to:

- 1. Identify and evaluate production biomass heating equipment in the 100,000 500,000 BTU output range that had features which could handle burning grass biomass fuels in 1/4" diameter pellets and 2" diameter "pucks".
- 2. Purchase and install a small (< 500,000 BTU/Hour) commercial production biomass boiler with ASME and UL certifications that would handle the unique issues with grass fuel combustion in a 4,500 square foot building at Meach Cove.
- 3. Operate and adjust the boiler to optimize the combustion process and ash handling for grass biomass fuels in 1/4" diameter pellets and 2" diameter pucks.
- 4. Collect and analyze emission data obtained from the grass fuel burned in the boiler. Make necessary adjustments to optimize the combustion performance when burning grass biomass and agricultural field residue in two different sizes. Suggest modifications to the boiler to improve performance with these grass biomass fuels.
- 5. Report on the results and recommendations from this project in a report and by posting them on our website, hosting open houses, tours, student classes, and live and taped segments for the local TV media.
- 6. Continue to operate, evaluate, and report on a variety of grass biomass fuels and their performance using the boiler after this project is completed.

The project scope included:

- Identifying, harvesting and densifying three different grass species, three diverse examples of local cool season perennial grass blends, and four samples of these grass species blended with wood chips. Testing two different wood pellet blends as a comparison to the grass samples.
- Selecting the Evoworld HC 100 Eco wood chip boiler from over a dozen commercial boilers and installing it in a building at the Meach Cove.
- Developing a testing method that would accurately evaluate the combustion performance, stack emissions, and the ash residue resulting from burning the grasses and biomass blends in the Evoworld boiler.
- Create a website to display the information gathered by this project. Plan and host a series of open houses, presentations, media reports, student classes, and tours to disseminate the information learned from this project.
- Produce a report to summarize our findings and recommendations for follow up research.
- After completing this project, continue to operate the Evoworld boiler on wood and other biomass blends, monitor and report on its performance. Host tours by appointment.

We have already listed the business and academic relationships that facilitated this project. Most significant among them were Sid Bosworth and Christopher Callahan of the University of Vermont Extension Service, and Bob Kort, CIG Program Manager, Energy Coordinator, USDA NRCS. In addition we must acknowledge the support and contributions of the Meach Cove Directors, the Meach Cove staff members Barbara Mercure who was the project Accounting Manager, Gary Marshall, Jack McGuire, Jesse Addis, Richard Lawrence and Denny DeCoff. We are grateful to Gerry and Betty Guillemette who mowed and baled most of the biomass used in this project. Without the hard work and assistance from these individuals and their institutions this project could not have been completed.

The project was funded by Meach Cove and the USDA NRCS CIG grant. Meach Cove contributed 63.6 %, or \$ 128,341.82 in expenditures or in-kind contributions. The USDA NRCS CIG grant provided 36.4 % or \$ 73,400.00 to cover testing, materials and a portion of the installation of the Evoworld HC 100 Eco boiler (Project Budget, page 84).

#### Project Background

The directors of Meach Cove have been interested in exploring ways to make better use of the natural resources available locally to offset petroleum that is being used on the property for space heating. Being able to economically and dependably burn grass fuel that is raised on this, or other Vermont farms, represents a major step towards identifying another viable renewable biomass fuel source for space heating applications. Data collected in this project demonstrated that grass can be harvested and densified into a 2" diameter puck at a cost that is competitive with the cost of wood pellets and #2 fuel oil (Callahan, 2016).

Research by others showed that grass fuel is a true renewable fuel source containing 90% of the energy content of wood and 70% less greenhouse gas emissions than fossil fuels. This report and previous studies have documented some of the issues and challenges encountered when burning grass fuels in commercially available smaller (<500,000 BTU/Hour) wood heating equipment (Kiraly, 2014, Sherman, 2011; Callahan, 2016).

This project drew from and added to the grass fuel combustion research performed recently by a number of individuals, groups and institutions such as Sherman, 2011, Kiraly, 2014, Wilson, 2014, and Callahan, 2016. When this project began there were many unanswered questions and issues to be resolved from the production of densified grass fuel and how to burn it in small commercial boilers (< 500,000 BTU/Hour). Attempts to burn grass in various forms in these smaller boilers resulted in issues such as clinker formation, high particulate emissions, high ash content and generally poor combustion efficiency (Sherman, 2011, Kiraly, 2014). For these reasons facility operators typically select one of the more reliable and mainstream petroleum fuel heating systems for their space heating needs. Individuals or institutions seeking a more renewable alternative to petroleum fuel have previously only considered selecting wood chip or wood pellet boilers to meet their heating needs.

Prior to learning of the Evoworld HC 100 Eco boiler, we had not identified a small commercial production boiler that had the design features or the combustion control capabilities to effectively deal with the challenges already mentioned when burning grass biomass or agricultural crop residue as a heating fuel.

These essential boiler features include:

- 1. The ability to store and convey an industry standard 1/4" diameter pellet or a larger size "puck".
- 2. Having sufficient combustion control capability to maintain the temperature ranges necessary for successful grass combustion. When the combustion temperatures are too hot it can cause ash fusion which results in clinker and slag formation which typically requires manual removal from the combustion chamber. Combustion temperatures that are too cool can result in unburned residue and inefficient

combustion resulting in higher emission gasses, particulates and unburned residue.

- 3. The ability to automatically remove the high volume of ash (up to 8% of the input volume) that is typical with grass and biomass fuel sources. Because wood pellets or wood chips typically produce ash volumes from 0.3 6%, boilers designed to burn wood typically perform poorly on grass and biomass fuel.
- 4. Designed with the capability to automatically clear clinkers, slag and any residue that may form during combustion.
- 5. Having stainless steel boiler and flue components where there is contact with the combustion gasses to limit the chance of corrosion of these components due to the high mineral content in some biomass fuels.
- 6. A boiler manufacturer that is willing to approve the burning of grass biomass in a boiler designed for wood fuel.

This project demonstrated that the technology exists to allow a farm operator, a municipal or government facility, an industrial complex owner, or a facility with a central heating plant to utilize locally sourced grass, biomass or crop residue to efficiently and cost effectively provide space heat. This project could be especially beneficial to farm operators who have the capability to harvest grass or biomass from their own land. These operators could arrange to have this biomass densified for their own use, or they could sell it to others who wish to use biomass for their space heating needs.

This project also demonstrated that grass biomass of a wide variety and quality could perform acceptably as a fuel source in a small size commercial boiler. It was noteworthy that even grass of a quality too poor for animal feed, which is typically found in abandoned pastures and field buffer areas, could be burned cleanly and economically in this boiler. The use of grass biomass harvested from fallow or non-prime crop land represents an additional resource for a farm operator to use for themselves or to sell to others. Having a market for biomass harvested from these buffer strip areas could help to incentivize the practice of establishing grass buffer strips adjacent to drainage ditches or waterways to help with water quality issues. The value of using marginal agricultural lands and buffer strips to reduce nutrient loss and help improve water quality has been well documented (Stutter, 2012, Helmers, 2006). Harvesting a seasonal grass crop for its fuel potential from marginal agricultural lands is an established concept (Bosworth, 2014, Wilson, 2014) but finding production ready heating equipment in a small commercial size that could handle it was an obstacle. This project demonstrates that this practice can provide a source of heating fuel or a marketable commodity for the farm operator.

Based on the combustion data obtained from the locally sourced grass biomass fuels tested in this project there is no negative side to using grass fuel in a properly equipped, adjusted and maintained boiler with the design features described in this report.

## **Review of Methods**

This project was innovative because prior to our identifying the Evoworld HC 100 Eco wood chip boiler, there were few commercial production boilers under 500,000 BTU/Hour that could effectively handle grass biomass fuel and conform to the current U.S. and EPA standards. The Evoworld boilers are manufactured in the U.S., have UL and ASME certification, and they have features that are essential for grass fuel combustion. The Meach Cove insurance underwriter and the State Fire Marshal would not allow any boiler to be operated in a commercial building without those certifications. This project was a unique success because previous attempts to burn grass in wood chip or wood pellet heating equipment had marginal success, while the Evoworld boiler's performance with challenging biomass fuels produced favorable results. The data obtained also indicated that the weedy Agricultural Biomass samples burned more efficiently and cleaner than most of the other 100% grass samples and were comparable to the wood pellets.

Our original CIG application proposed testing both a hot water boiler and a forced hot air furnace. As part of this project we researched small commercial production boilers that might work for grass it became clear that the grant funding would not be enough to purchase more than one heating unit. We decided to purchase just the hot water boiler because the boiler could handle either typical 1/4" diameter pellets or larger 2" diameter "pucks", and the building at Meach Cove where it would be installed was already configured with baseboard hydronic radiation.

The Evoworld HC 100 Eco boiler we chose was unique because the control processor and software allowed us to pre-set ranges for critical operation functions such as fuel feed, air flow, oxygen levels and temperature of the boiler water or flue gas (Figures 3-7, pages 43-46). Because of these innovative and unique features of the Evoworld HC 100 Eco boiler we were able to set ranges which allowed the boiler to operate with all of the biomass fuels we tested. There was a steep learning curve for us while we experimented with the settings typical for wood chips or wood pellets. To meet the goals of this project the project director worked with Christopher Callahan, an agricultural engineer with the University of Vermont Extension Service, and Adam Dantzscher, to identify boiler settings that optimized the combustion of the grasses and biomass blends we tested.

#### Grass and Biomass Types Tested

Meach Cove has been an active participant in the Grass Energy Partnership since 2008. Meach Cove worked with the University of Vermont Extension Service to establish a perennial energy grass species replicated test plot on the Meach Cove property along with some larger plots of Switchgrass and Reed Canarygrass (Figures 1-2, pages 41-42). Based on the earlier research by Sid Bosworth and Tim Kelly (Bosworth, Kelly, 2015) we selected three perennial energy grass species to test in this project (Cave-N-Rock variety of Switchgrass, Reed Canarygrass, and Giant Miscanthus). We also tested typical "mulch" hay, agricultural crop residue salvaged from abandoned pasture land, and "grass" pellets produced by Enviro Energy, LLC in Wells Bridge, N.Y. We thought it would be useful to retest nine wood and grass blend pellet samples that were originally tested in 2010 by BERC (Sherman, 2011). For comparison we tested one brand of 1/4" diameter 100% softwood pine pellets (Vermont Wood Pellets) and one brand of 50% hardwood / 50% softwood pellets (Energex, Canada).

We grew and harvested the Cave-N-Rock variety of Switchgrass, a native perennial warm season grass that shows promise as a grass energy choice because once it is established it can thrive in a range of soil types and climatic zones and previous research indicated it had a low ash content compared to other perennial grasses (Figure 12, page 49).

We tested Reed Canarygrass because it is a common grass species in the U.S. and it is well adapted to wetter and marginal soils. Reed Canarygrass has a low value for animal feed but it has shown promise as a fuel grass (Bosworth, Kelly 2015).

Giant Miscanthus (miscanthus giganteus) is a warm climate grass that was planted as rhizomes rather than seed in 2010 as part of the UVM Warm Season grass evaluation project (Bosworth, Kelly, 2015). Once we realized that Giant Miscanthus could survive the Vermont climate we felt it was worth testing it along with the other biomass fuel samples because of the limited emission data available on it, and because it is being planted as a land reclamation crop in many parts of the U.S. (Figure 12, page 49).

We felt it was important to test the typical "mulch" quality hay and the coarser and weedier hay harvested from abandoned pasture land that we called "Ag Biomass" because they represent a crop that is not suitable for livestock feed that is widely available throughout the U.S. (Figure 14-15, page 50). Ag Biomass hay is known to cause difficulty when burned in smaller (< 500,000 BTU/Hour) heating equipment due to its higher ash content, and its potential to form clinkers or slag (Kiraly, 2014). Because poor quality Ag Biomass hay is widely available and adapts to all soil conditions we thought it was worth testing in comparison to the cultivated biomass fuel grass species of Switchgrass, Reed Canarygrass, Giant Miscanthus, and the wood pellets.

Sources of the Grass Biomass Tested

The 100% "mulch" hay 1/4" diameter pellets we tested were purchased from Enviro Energy, LLC in Wells Bridge, N.Y. This was mulch quality hay that had been harvested in a late season cut from open land near the Enviro Energy facility. The Enviro Energy facility used a diesel power unit to provide the electricity to run a wood pellet mill and air dryers and their typical production rate was one ton of grass pellets per hour (Figures Figure 22- 24, pages 54-55).

The 100% Reed Canarygrass and Switchgrass pellets that we tested were grown on the Meach Cove property and trucked in 45-65 pound square bales to Enviro Energy where they were pelletized into 50 pound bags (Figure 2, page 42). The blended grass and wood 1/4" diameter pellets were left over samples from the 2010 testing performed by BERC and reported by Adam Sherman in 2011. These pellets were produced from mulch hay grown at Meach Cove and Switchgrass and Reed Canarygrass harvested on the

Borderview Farm in Alburgh, Vermont, and processed into 1/4" diameter pellets at the Vermont Wood Pellet facility in North Clarendon, VT. We thought it would be informative to test these same previously tested samples in the Evoworld HC 100 Eco boiler which we believed was better equipped to handle the combustion issues detailed in the BERC report (Sherman, 2011).

Because the Evoworld HC 100 Eco boiler could handle both a typical 1/4" diameter pellet as well as a larger fuel form, we tested most of these same biomass grass species densified into a 2" diameter puck.

The Switchgrass and Reed Canarygrass used to make these 2" pucks was harvested from the test plot at Meach Cove in 500-700 pound round bales (Figure 2, page 42 and Figure 13, page 49).

The mulch hay and Ag Biomass crop residue was also harvested from areas on the Meach Cove property in 50-70 pound square bales (Figure 2, page 42, Figure 14-15, page 50).

The Giant Miscanthus was harvested in Arkansas and supplied by Adam Dantzscher who manufactured the 2" diameter pucks with a modified BHS "Slugger" machine (Figure 16, page 51). Adam Dantzscher chopped the round and square bales in a tub grinder powered by a tractor PTO, fed the chopped hay into an electric hammer mill and then into the BHS Slugger machine which was also powered by a tractor PTO. The BHS Slugger production of 2" diameter air dried pucks varied from 400-700 pounds per hour depending on the biomass feed source and the moisture content of the materials being densified. These pucks were made in batches weighing 600-700 pounds and they dropped directly from the BHS Slugger drying racks into 48" x 48"x 48" bulk bags which could be moved by forklift or bucket equipped tractor and were stacked three bags high until needed for testing (Figure 18, page 52).

Biomass sample analysis

Once the biomass fuel samples were densified into either the 1/4" pellet or 2" diameter pucks, random samples were obtained from the batches, packaged in 1 gallon Ziploc bags and sent to Twin Ports Testing, Inc. in Superior, Wisconsin for analysis. Twin Ports performed a proximate analysis of the samples to determine their composition by measuring the:

- Moisture Content
- Ash Content
- Volatile Matter
- Fixed Carbon
- Calorific Energy (heating) Value
- Ash Fusion Temperature

Twin Ports also performed an ultimate analysis of the samples to determine the elements in the samples by percentage, weight or volumetric unit which were:

- Carbon
- Hydrogen
- Oxygen
- Nitrogen
- Sulphur
- Chlorine

The data from these reports was summarized in the tables and graphs represented in this report. The compounds and the elements within the samples influence how the biomass performs when it is combusted in a boiler and the results can vary widely as you will see in the Findings section of this report that begins on page 20.

The data we collected compared the combustion and emission data for the grasses and biomass blends we tested with wood pellets, a common and proven biomass fuel source.

The samples tested were:

- 100% Switchgrass (Cane-N-Rock) in 1/4" pellet and 2" puck
- 50% Switchgrass / 50% wood chips in 2" puck
- 100% Giant miscanthus (Miscanthus giganteus) in 2" puck
- 50% Giant miscanthus / 50% wood chips in 2" puck
- 100% Reed Canarygrass in 1/4" pellet and 2" puck
- 100% Enviro Energy mulch hay in 1/4" pellet
- 100% Meach Cove mulch hay in 2" puck
- 50% Meach Cove mulch hay / 50% wood chips in 2" puck
- 100% Ag. Biomass Field Residue in 2" puck
- 100% Reed Canarygrass in1/4" pellet and 2" puck
- 50% Reed Canarygrass / 50% wood chips in 2" puck
- 25%/12%/6% Switchgrass, Reed Canarygrass and Mulch hay in 1/4" pellet
- 100% softwood (pine) Vermont Wood Pellet in 1/4" pellet
- 50% softwood / 50% hardwood (Energex, Canada) in 1/4" pellet

The test samples were weighed into 5 gallon buckets and fed into the chip feed auger on the Evoworld HC 100 Eco boiler (Figure 5, page 45 and Figure 20, page 53). Upper and lower level temperatures in the 550 gallon hot water storage tank and the temperature of the boiler water were recorded before, during and after each test run (Figure 8, page 47). We began each test with a low hot water storage tank temperature to allow the boiler to operate at full load throughout the 60-90 minute duration of the test burn.

Christopher Callahan calculated the gross efficiency of the Evoworld boiler by measuring the temperature change of the boiler water, the storage tank water volume, and the amount of fuel fed into the boiler, measured over a period of time (Callahan, 2016).

To document what was occurring during the combustion of these fuels and to be able to draw comparisons with the data obtained in previous combustion studies with similar grass species we needed to find an easy to use and accurate portable emission analyzers. The minimum combustion parameters we needed to obtain to make adequate comparisons were:

- Combustion input air temperature (F)
- Stack temperature (F)
- Oxygen (O2)
- Carbon Dioxide (CO2)
- Carbon Monoxide (CO)
- Nitrogen Oxide (NO)
- Sulphur Dioxide (SO2)
- Combustion efficiency
- Percent of exhaust air
- Particulate emissions (Smoke number)

We purchased a Wohler A500 digital combustion analyzer which proved to be durable and accurate during the days of biomass sample testing (Figure 26, page 56). The Wohler analyzer was designed to test petroleum heating equipment. The grass and biomass samples often exceeded the typical operating ranges of the sensors in the Wohler analyzer but it still performed well throughout the testing.

To measure the particulate emissions we used a Wohler RP 72 hand operated Smoke Test Pump. The hand operated Smoke Test Pump draws flue gas through a piece of filter paper which leaves a particulate stain on the paper that is removed from the test wand and compared to a color gradient chart numbered from 0 to 9 (Figure 27, page 56). A smoke level number of "0" represents no smoke detected and a smoke level number of "9" represents a solid black sample, or the maximum visible stain on the filter paper. This simple visual method of estimating the level of particulates that represent the stain on the sample filter paper is commonly used by heating equipment service technicians when tuning oil and gas appliances, so we felt it could provide useful data for this project. More refined particulate analysis of flue gasses requires specialized portable laboratory equipment to collect micro weight data such as that recorded in the BERC testing in 2010 (Sherman, 2011). These emission samples were collected from a 1" flue port installed in flue section 20" from the boiler induced draft fan outlet (Figure 28, page 57).

Project Schedule of Events

October through December, 2011: We reviewed the previous research on species of grass used as fuel and small commercial boilers under 500,000 BTU/Hour that had features well suited to burning grass and biomass in 1/4" pellet and a 2" diameter "puck" sizes.

October, 2011: Meach Cove harvested grass from the Meach Cove test plots and delivered it to Enviro Energy, LLC in Wells Bridge, N.Y. where it was densified into 1/4" pellets.

January, 2012: Pellet samples were sent to Twin Ports Testing, Inc. for calorific, chemical and ash testing.

April 2013: Meach Cove collaborated with Renewable Energy Resources, Inc. to identify a boiler that could handle grass and biomass in a 1/4" pellet or a 2" diameter puck form.

September 23, 2013: Original project end date, extended until September 20, 2014.

September 2013: Meach Cove places an order with RER, Inc. for an Evoworld HC 100 Eco wood chip boiler.

December 2013: Meach Cove employees installed the Evoworld wood pellet and wood chip conveyors in the fuel bins that they constructed.

January 29, 2014: Evoworld HC 100 Eco boiler and a 550 gallon hot water buffer tank are delivered and placed in the Meach Cove boiler room.

April 11, 2014: The boiler room installation is completed and the Evoworld boiler is test run. We are still waiting for UL certification and final inspections of the boiler.

August 2014: Project end date extended to September 2015.

September 22, 2014: UL certification received for the Evoworld USA HC 100 Eco boiler.

September 26, 2014: The boiler passes inspection by Hartford Insurance Co. inspector.

October 6, 2014: State Fire Marshal approved operation of the boiler.

October 17, 2014: The Evoworld boiler begins heating the Meach Cove building burning wood pellets.

March 6, 2015: The first round of grass and biomass fuel combustion testing begins.

September 20, 2015: Project end date.

October - November 2015: Christopher Callahan assists the Project Director in the second round of grass and biomass testing which includes 2" dimeter pucks.

October 23 and 24, 2015: Open houses held at Meach Cove Farms.

October 26, 2015: Fox Channel 22/44 reporter on site for six live broadcast segments highlighting the project.

November 4, 2015: WCAX Channel 3 UVM Extension Service show Across the Fence report on Grass to Energy describing this project airs.

October 2015 – April 2016: Evoworld boiler operated on wood pellets. Periods of 3-7 days the boiler was operated on grass biomass 2" pucks or blends of grass and wood pellets.

Project Location & Map showing where the samples were grown and tested

Project location and Natural Resources Inventory maps are provided on pages 41 and 42 showing the Meach Cove Farm, the Warm Season Grass test plots, the building where the Evoworld boiler was installed, and the areas where the mulch hay and Ag Biomass samples were harvested.

Summary of what worked and what did not

The Evoworld HC 100 Eco boiler we installed performed better than we could have anticipated given the range of biomass material we tested for this project. Once we learned how the boiler control software operated, we were able to program operational ranges that allowed the boiler to adjust to variations in the fuel performance during the test burns. We used the combustion data collected with a Wohler A500 emission analyzer to adjust the fuel feed rates and air settings to optimize the boiler's performance with each fuel sample.

The set up for this project took longer than anticipated for a number of reasons.

- It was a challenge to identify a production boiler that had the features necessary to handle the known issues others had experienced when burning grass and other forms of biomass in a small (< 500,000 BTU/Hour) rated commercial boiler.</li>
- Once the Evoworld HC 100 Eco boiler was ordered there were delays while the boiler was built and another seven months to obtain the UL certification for this boiler model.

- We learned that ASME and UL certifications were required by the Meach Cove insurance company and the State Fire Marshal in order to operate a boiler in a commercial building in Vermont. We experienced months of delays resolving boiler room and fuel storage design issues to the satisfaction of both of these authorities.
- During the initial boiler test operation it was discovered that modifications were needed to the way the boiler was plumbed into the building's heat distribution manifold.
- It took time to learn how the Evoworld boiler control software operated. The Evoworld USA construction team in Troy, N.Y. only had experience burning wood in the boilers so the Project Director, with assistance from Adam Dantzscher and Christopher Callahan worked out the settings necessary to optimize the combustion of the grass and biomass fuel blends.

#### What would be done differently

If we started this project today we would have the design for biomass fuel storage bins and the boiler room layout that the Vermont Fire Marshal and the insurance company inspector would approve. All of the Evoworld boiler models are now ASME and UL certified. We have learned how to configure the Evoworld operating system to optimize its performance on a variety of biomass fuels sizes and types. During this project we learned that adding a scraper bar to the combustion shelf in the firebox should allow the boiler to operate with minimal primary air restriction when burning grass pellets or 2" diameter pucks. Activating this scraper bar before each firing should clear any clinkers and residue if they form off the combustion shelf and this should permit repetitive burn cycles with the grass biomass fuels.

One significant limitation to anyone considering burning grass biomass fuels today is locating someone to process the harvested grass biomass into a densified puck or pellet form. Without a demand for grass biomass fuel, there is no incentive for a business to invest in the equipment to densify grass into boiler sized fuel. Without a source of densified grass, potential adopters would have to invest in densifying equipment or seek other wood based biomass fuel. Based on historical evidence, a significant rise in the cost of petroleum fuels should spur renewed interest in grass (and wood) biomass as a space heat fuel source (Kotrba, 2015).

# **Discussion of Quality Assurance**

The Meach Cove property is 1000 acres that is comprised of roughly one-third managed forestland, one-third productive agricultural land, and one-third pasture, riparian buffer areas, wetlands or ponds. In 2008 Meach Cove collaborated with the University of Vermont Extension Service to establish a replicated grass species study plot on a five acre parcel on the Meach Cove property (Figure 1, page 41). The grass study plot provided the Switchgrass and Reed Canarygrass that was densified and tested for this project. Other areas of the Meach Cove property provided the mulch quality hay and the agricultural residue samples that were tested (Figure 2, page 42).

The grass plot study site was selected because it was separate from the certified organic acres that are in active crop production. This location permitted the UVM study to incorporate fertilizer rate trials and test the effect of chemical weed control methods on some of the grass plots without impacting the adjacent certified organic fields. The samples of mulch quality hay and agricultural crop residue were harvested from other areas on the Meach Cove property because they represented abandoned pastureland or buffer areas near drainage ways (Figure 2, page 42). We selected these areas because they are similar to non-prime agricultural land on almost every farm in this region.

We selected Twin Ports Testing, Inc. in Superior, Wisconsin to perform the analysis on the densified grasses we evaluated because they are a lab that specializes in biomass testing with an excellent reputation. Twin Ports Testing, Inc. was the lab used in the 2010-11 testing that is described in the BERC "<u>Technical Assessment of Grass Pellets as Boiler</u> <u>Fuel in Vermont</u>" authored by Adam Sherman (Sherman, 2011) so we wanted to use them so that we could make comparisons with our samples.

1/4" pellet and 2" puck samples were randomly drawn from the bags of the densified grass species and placed in one gallon Ziploc sample bags and mailed to Twin Ports Testing. Twin Ports performed Ultimate and Proximate Analysis, as well as tested the chlorine level of the samples. The Twin Ports Testing website listed on page 39 of the References provides a detailed summary of how they manage the chain of custody of the samples they test.

A Wohler A500 hand held digital combustion analyzer was used to measure and record nine qualities of the combustion emissions of the EVO HC 100 Eco wood chip boiler while burning the wood pellets and the biomass blends. The Wohler A500 analyzer had new sample modules installed and it was calibrated at the Wohler U.S. service center prior to beginning this project. The Wohler unit runs a self-calibrating sequence every time it is turned on. Prior to each test run the sample tubing on the Wohler analyzer was blown out with compressed air to remove any moisture or particulates and the various filters in the Wohler instrument were changed (Figure 26, page 56).Emission samples were collected in a 1" flue port installed in the flue section 20" from the boiler induced draft fan outlet (Figure 28, page 57 and Figure 9, page 47).

Prior to commencing the combustion testing for this project the Evoworld boiler fuel bin and the fuel feed auger were vacuumed clean, the boiler tubes were cleaned, and the firebox was scraped down and vacuumed to minimize residual ash from prior fuel tests.

Every effort was made to perform the combustion testing by following the same series of steps and, if possible, by the same individual. We isolated the heat distribution system so that the boiler was only heating the 550 gallon buffer tank. The temperature of the buffer tank was noted before and after each test burn which allowed estimates of the thermal efficiency of the test burns to be calculated (Callahan, 2016). The boiler was started and allowed to run through the typical self-cleaning cycle prior to start up, it then begins a 5 minute start up and ignition sequence. Once the boiler reached the "full load" combustion stage indicated on the boiler control panel the tester would begin to take emission and smoke samples with the Wohler equipment. Samples were taken at 10-15 minute intervals over the course of 60 to 90 minutes with the boiler operating at "full load". The data was captured by the Wohler instrument and printed using the Wohler wireless printer as each sample was taken. The Wohler RP72 smoke test pump was used to take flue gas samples from the 1" flue port as each emission sample was recorded. The smoke test filters were labeled and stapled to the Wohler printouts. We made adjustments to the air flow and fuel feed rates for the boiler during the test runs to minimize the CO levels and maximize the combustion efficiency and noted these changes on the work sheets used for each test.

Emission measurements with the Wohler A500 and the smoke tests were performed following the same process and as close to the same time interval for each test run by the same person for consistency. The raw data was transferred from the Wohler emission print outs and smoke test paper disks into an Excel spreadsheet. Both the Project Administrator and the Project Director reviewed the data for accuracy after it was entered in the Excel spreadsheet and after it was graphically displayed.

Summaries of the data were used to create the bar graphs visually illustrate and compare the data.

# **Findings**

The initial round of testing performed from March through June of 2015 focused on 1/4" diameter pellet samples of mulch hay, Switchgrass, Reed Canarygrass, and testing the pellet samples of these same perennial grasses mixed at 6%, 12%, and 25% with pine sawdust making up the balance. These were the same samples tested in 2010-11 (Sherman, 2011) in a SolaGen 500,000 BTU/Hour boiler designed to burn wood pellets. We wanted to see how a boiler with the features of the Evoworld HC 100 Eco wood chip boiler performed when burning these same fuel samples.

Following production of 2" diameter pucks by Adam Dantzscher using many of the same grass species, and blends of grass samples with wood chips, we conducted combustion tests in October and November, 2015 with the assistance of Christopher Callahan. The analysis of that round of testing was provided by Christopher Callahan in his report titled "Solid Grass Biomass Fuels in Vermont: An Update" (Callahan, 2016). The experience gained in running the Evoworld boiler March through June, 2015 testing, and Christopher Callahan's expertise in tuning the Evoworld boiler during the October and November 2015 testing yielded sufficient data to draw a number of important conclusions about the variety of biomass types and blends we tested.

#### Optimization of the Boiler Settings

As previously described, the Evoworld HC 100 Eco wood chip boiler has a number of design features that made it well suited to burning other types and form sizes of biomass fuel. The Evoworld control software allowed us to make changes to the performance ranges for the fuel and air delivery rates before and during the boiler's heating cycle. Once we established the upper and lower range for the fuel feed rates, the level of fuel in the combustion chamber, the volume of air being supplied (from below the combustion shelf, mid height in the combustion chamber, and in the upper portion of the combustion chamber), and the draft pressure being applied by the Induced Draft (ID) fan in the flue, the Evoworld software would make instantaneous adjustments as the boiler operated through the ignition, full load, and "after venting" stages of the boiler's programmed combustion cycle (Figure 6, page 46).

We began our testing by using settings for wood chips and wood pellets as recommended in the Evoworld manual. We applied the tuning suggestions for fuel and air adjustments as described in the manual and noted the changes in the performance with the type of fuel we were burning. Through trial and error we arrived at settings that gave us the best range of emission data during the test burns. We got better at making these range adjustments over the period of time we spent with each biomass sample we tested.

We had an easier time getting better combustion performance from the 2" diameter pucks for all the types of biomass we tested. My initial thought is that this was because of the greater air spacing between the pucks which allowed more primary air flow to the fuel pile. Another factor may have been that the density of the pucks was less than the pellets which resulted in them breaking down more readily during the combustion. The 2"

diameter pucks left a lighter weight fluffy ash residue vs. the denser and crusty residue we found after the test burns with the grass pellet samples (Figures 31-32, pages 58-59).

We learned that to get more robust combustion we needed to reduce the rate that grass fuel in either the ¼" pellet or 2" diameter puck forms was fed into the combustion chamber during the ignition phase of the boiler cycle. I believe this was because it took longer to get the grass samples burning hot enough so that new fuel being introduced to the combustion chamber would not smother the fuel pile burning on the combustion shelf.

We found that we needed to increase the amount of air being fed into all levels of the combustion chamber when we were testing the grass samples. With the additional combustion chamber air input we had to increase the draft underpressure range to allow the boiler more latitude to increase or decrease the ID fan speed during the combustion cycle.

We also learned that we needed to run the combustion air fans at higher levels through the entire combustion cycle and the after venting period to provide a more complete combustion of any residual fuel in the combustion chamber.

Because we got better at making adjustments to the boiler settings and ranges we have a higher level of confidence in the later round of test data but we feel both sets of test data contain valuable information.

	Stack Temp		со				NÖ	SO2	Smoke
Avg	۴	02	ppm	CO2	EFF	Ex Air	ppm	ppm	Test
Blend: 100%									
100% VT Wood pine pellets	380	12.23%	518	7.70%	71.38%	144.58%	35	6	>9
100% Egx Wood Blnd pellets	356	11.42%	274	9.25%	80.57%	144.33%	59	2	8
100% Enviro Energy hay pellets	331	13.88%	1724	6.88%	80.21%	323.33%	115	74	>7
100% Switchgrass pellets	302	15.92%	456	5.81%	56.39%	381.10%	89	1	>6
100% Switchgrass pucks (2008)	363	13.58%	423	7.15%	76.92%	199.63%	96	0	7
100% Reed Canary pellets	353	12.70%	892	8.01%	77.84%	180.56%	112	4	7->9
Blend: 25% (Sherman 2011)									
25% Switchgrass/75% pine pellets	360	9.80%	117	10.80%	82.43%	87.67%	94	1	0
25% Reed Canary/75% pine pellets	321	16.50%	254	4.30%	74.10%	367.00%	50	1	0
25% MC Mulch hay/75% pine pellets	339	12.33%	216	8.37%	80.07%	173.67%	104	0	0
Blend: 12% (Sherman 2011)									
12% Switchgrass/88% pine pellets	379	9.27%	123	11.33%	82.00%	79.00%	81	3	0
12% Reed Canary/88% pine pellets	351	12.07%	140	8.63%	81.07%	138.33%	69	0	0
12% MC Mulch hay/88% pine pellets	373	9.80%	169	10.83%	81.83%	89.00%	102	2	0
Blend: 6% (Sherman 2011)									
5% Switchgrass/94% pine pellets	375	9.53%	96	11.07%	82.00%	83.00%	73	1	0
5% Reed Canary/94% pine pellets	380	11.30%	236	9.37%	80.50%	118.33%	61	2	0
6% MC Mulch hay/94% pine pellets	400	10.38%	253	10.28%	80.58%	97.75%	71	1	0

 Table 1 - Summary of Exhaust Gas Measurements March-June 2015. Typically, an average of three readings toward the end of a 1 hour test run. Not representative of optimized performance.

Combustion Residual Comparison March - June 2015							
	Gross Calorific Value BTU/Lb	Ash Moisture free WT %	Ash Fusion Reducing Atmosphere Temp °F	Chlorine Moisture free mg/kg			
Blend: 100%							
100% VT Wood pellets	9043	0.23	2680	27			
100% Energex Wood Blend pellets	8670	0.68	2630				
100% Enviro Energy Hay pellets	8290	4.98	2520	3703			
100% Switchgrass pellets	8117	6.63	2590	2517			
100% Switchgrass pucks (2008)							
100% Reed Canary pellets	8213	4.54	2520	1041			
Blend: 25% (Sherman 2011)							
25% Switchgrass/75% pine pellets	8534	2.22	2460	75			
25% Reed Canary/75% pine pellets	8430	1.69	2540	90			
25% MC Mulch Hay/75% pine pellets	8404	1.63	2210	649			
Blend: 12% (Sherman 2011)							
12% Switchgrass/88% pine pellets	8627	1.31	2230	36			
12% Reed Canary/88% pine pellets	8559	0.90	2495	81			
12% MC Mulch Hay/88% pine pellets	8783	0.90	2360	228			
Blend: 6% (Sherman 2011)							
6% Switchgrass/94% pine pellets	8529	0.91	2400	33			
6% Reed Canary/94% pine pellets	8526	0.56	2385	33			
6% MC Mulch Hay/94% pine pellets	8618	0.56	2240	126			

SOURCE-Twin Ports Testing Inc. Analytical test reports

	Stack Temp		СО				NO	SO2	Smoke
Avg	۴F	02	ppm	CO2	EFF	Ex Air	ppm	ppm	Test
Blend: 100%									
100% VT Wood pellets-Not Tested									
100% Energex Wood Blend pellets	365	9.78%	369	10.83%	82.75%	89.17%	68	1	>9
100% Enviro Energy Hay pellets	234	18.83%	849	2.07%	64.07%	844.00%	46	93	7
100% Switchgrass pucks	350	13.80%	325	6.93%	77.48%	207.40%	97	1	6
100% Reed Canary pucks	347	14.60%	184	6.13%	74.93%	246.33%	107	0	7.0
100% Miscanthus pucks	351	13.98%	87	6.77%	77.83%	200.33%	64	0	5
100% MC Mulch Hay pucks	368	13.90%	227	6.83%	75.95%	205.50%	113	0	5
100% Ag. Biomass pucks	307	12.43%	272	8.30%	81.53%	153.00%	138	0	6
Blend: 50%									
50% Switchgrass/50% Wood pucks	253	17.55%	229	3.18%	73.38%	538.75%	57	0	9
50% Reed Canary/50% Wood pucks	348	14.06%	188	6.68%	77.42%	204.20%	164	0	6
50% Miscanthus/50% Wood pucks	322	16.05%	125	4.75%	73.90%	325.50%	70	0	6
50% MC Mulch Hay/50% Wood pucks	308	16.23%	236	4.58%	74.50%	340.75%	86	0	6

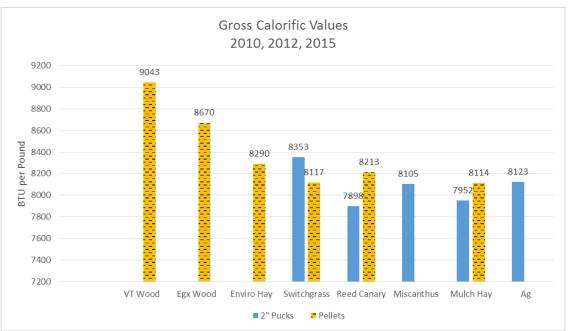
 Table 2 - Summary of Exhaust Gas Measurements October-November 2015. Typically, an average of three readings toward the end of a 1 hour test run. Not representative of optimized performance.

	Gross Calorific Value BTU/Lb	Ash Moisture free WT %	Ash Fusion Reducing Atmosphere Temp °F	Chlorine Moisture free mg/kg
Blend: 100%				
100% VT Wood pellets	9043	0.23	2680	27
100% Energex Wood Blend pellets	8670	0.68	2630	102
100% Enviro Energy Hay pellets	8290	4.98	2520	3703
100% Switchgrass pucks	8353	3.90		973
100% Reed Canary pucks	7898	8.06		3312
100% Miscanthus pucks	8105	3.99		352
100% MC Mulch Hay pucks	7952	6.80		2146
100% Ag. Biomass pucks	8123	5.35		227
Blend: 50%				
50% Switchgrass/50% Wood pucks	8344	4.01		899
50% Reed Canary/50% Wood pucks	7900	8.14		2983
50% Miscanthus/50% Wood pucks	8079	6.25		341
50% MC Mulch Hay/50% Wood pucks	8180	6.15		1211

SOURCE-Twin Ports Testing Inc. Analytical test reports

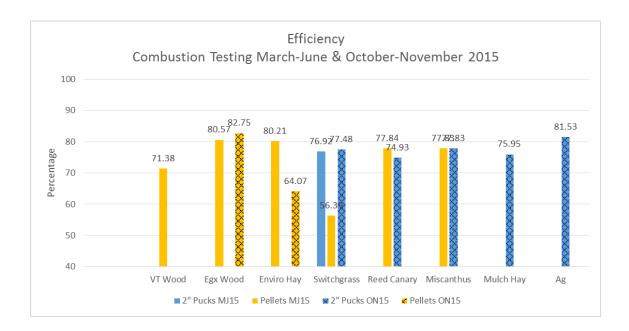
#### **Findings Summary**

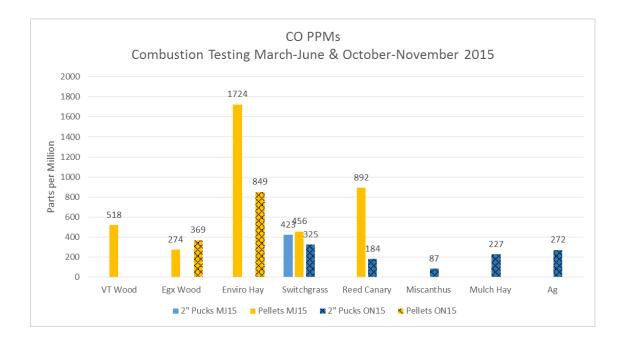
- A small (350,000 BTU/Hour rated) commercial U.S. built, ASME and UL certified, hot water boiler designed to burn wood chips can be adjusted to burn grass fuel and agricultural biomass/field residue in 1/4" pellet and 2" diameter puck forms with emissions and combustion efficiency data comparable to wood pellets. Prior to identifying the Evoworld HC 100 Eco boiler, we were unable to locate a commercial production boiler with ASME and UL certification and the design features that could handle grass or biomass.
- 2. We discovered during the testing that the Evoworld processor and programming was capable of automatically adjusting the air and fuel delivery rates to optimize the combustion performance while burning different species of grass in 1/4" pellets and 2" diameter pucks (Figure 17, page 51). We had to work out the upper and lower ranges for these settings for each phase of the boiler's combustion cycle (start up, ignition, full load, after venting) to get optimal emission performance from the boiler.
- 3. The mulch quality hay harvested from abandoned pasture land we described as "Agricultural Biomass/field residue" in this study, was densified into a 2" diameter pucks and had an energy content and combustion emission properties compared favorably to the perennial fuel grasses (Switchgrass, Reed Canarygrass, Giant Miscanthus) and the two types of wood pellets tested.

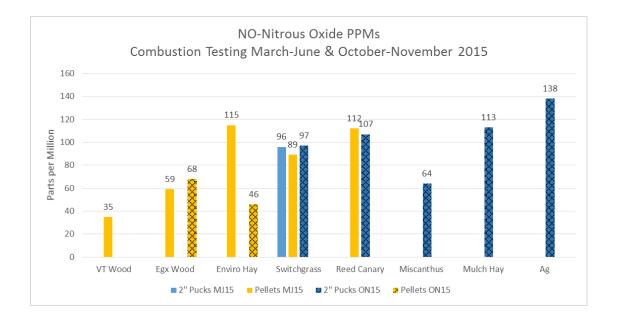


Moisture Free GCV data taken from Twin Ports Testing Analytic test reports; arrival dates 2/22/2010 (VT Wood & Mulch pellets), 1/31/2012 (rest of pellets) & 11/30/2015 (2" pucks)

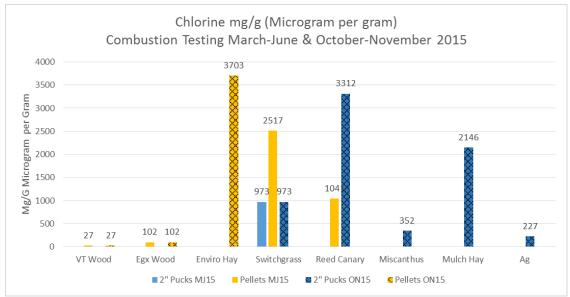
- 4. Some clinker formation and unburned residue occurred when burning the perennial fuel grass and mulch hay in the 1/4" pellet form (Figures 32-33, page 59). We were able to adjust the boiler to minimize clinker formation with the 2" diameter pucks.
- 5. Analysis of the Twin Ports Testing data revealed that the 100% Switchgrass in a 2" puck had the highest Gross Calorific value of the grasses tested (8,353 BTU/Lb.) and it was 7.6% less than the 100% softwood (Vermont Wood Pellet) pellets and only 3.7% lower than the 50% softwood / 50% hardwood (Energex) wood pellets.
- 6. The Evoworld HC 100 Eco boiler is able to efficiently burn the range of 100% grass species and grass/wood blends we tested with combustion efficiency that ranged from 56.3 81.5% as compared with wood pellets with a range of 71-82%. Only a 50% softwood / 50% hardwood (Energex) pellets burned with higher efficiency (82.75%) than the 100% Enviro Energy mulch hay pellets (80.2%) and Agricultural Biomass/field residue 2" diameter pucks (81.5%).
- 7. The Agricultural Biomass/field residue that was harvested from an abandoned pasture on the Meach Cove property (Figure 2, page 42) burned with the highest efficiency of the other grass and biomass types tested at 81.5%, and had lower CO and a lower smoke test number than the wood pellets we tested.
- 8. Giant Miscanthus grass in 2" diameter pucks and pellets burned easily with similar efficiency (77.8%), and had the lowest CO (87 ppm) of any of the grasses, wood, or blends we tested.
- 9. The system thermal efficiency ranged from 38 83% (Callahan, 2016).







10. Chlorine levels varied drastically between samples ranging from a low of 27 mg/g for the 100% softwood pellets to a high of 3,703 mg/g for the Enviro Energy mulch hay pellets. The agricultural biomass/field residue (227 mg/g) and the Giant Miscanthus (352 mg/g) were the lowest of the 100% grasses and grass biomass we tested.



Chlorine data taken from Twin Ports Testing Analytical test report 1/31/2012 Did not test VT Wood pellets in Oct-Nov 2015 Combustion test

- 11. There were some issues with grass in both the 1/4" pellet and 2" diameter puck form blocking the primary combustion air after a burn cycle (Figure 30, page 58). Between burn cycles all of the grasses in the 1/4" pellet form cooled and formed a crust of clinker on the fuel pile. This clinker formation required us to manually clear the accumulated clinker and ash between test runs. I believe that these issues could be eliminated with the addition of a mechanical sweeper arm that would push the remaining fuel off the combustion shelf onto the slated floor of the firebox where the normal cleaning cycle at the beginning of each burn cycle would convey it to the ash container. (Figure 7, page 46).
- 12. Following the conclusion of the grass and biomass testing in November 2015, we continued to heat the building with wood pellets and shut the boiler down for the spring in April, 2016. We intended to clean the boiler tubes, turbulators and firebox after the spring shut down but did not get to the cleaning until the fall of 2016. We discovered at that time that the carbon steel turbulators in the second pass of boiler tubes had become rusted to the tube walls (Figures 10-11, page 48). When the boiler was activated it initiated a cleaning cycle where the turbulators would normally move up and down to clean the tube walls. Because of the rust the turbulators did not move and the cleaning motor continued to run, melting the

motor windings and damaging the control board. After consulting with the Evoworld manufacturer in Troy, N.Y. about this condition, we cannot be sure that the corrosion and rust on the carbon steel turbulators was caused by any byproducts of grass combustion, or because of moisture in the air being drawn through the boiler during the summer and fall months. An additional circuit breaker has been added to these boilers to protect the cleaning motor and the circuit board if this ever occurs again.

- 13. In Christopher Callahan's 2016 report on the combustion of the 2" diameter grass puck samples, he provided calculations showing that the cost to grow, harvest and process grass into a 2" diameter puck is competitive in price with wood pellets at the time of writing this report (\$214 \$265 per ton). The cost to produce the 2" diameter pucks should come down if a steady market demand for these pucks existed (Callahan, 2016).
- 14. The cost to produce 2" diameter pucks using portable equipment such as the BHS "Slugger" machine is similar to the cost to operate a small capacity fixed pellet manufacturing facility such as the Enviro Energy plant but the capital cost to purchase and set up a fixed pellet plant is considerably more expensive +/-\$100,000 (Callahan, 2016) vs. > \$700,000 (Enviro Energy, 2011). From our research we have not identified a portable trailer mounted pelletizing and drying unit that is able to match the output rate, consistent quality or cost of production of a fixed pellet plant to produce standard 1/4" diameter pellets.
- 15. The table below shows that the cost to heat buildings with the types of biomass fuel sources described in this report using the production costs described in Christopher Callahan's 2016 report are comparable to the present cost of wood pellets or wood chips, and less expensive than petroleum fuels available in this region.

Fuel Cost Comparison									
Fuel	Cost	Cost Units	Energy Content	Energy Units	Normalized Fuel Cost \$/million BTU				
Propane	\$2.65	\$/gal	92,000	BTU/gal	28.80				
#2 Fuel Oil	\$2.10	\$/gal	129,500	BTU/gal	16.22				
Wood Pellets	\$277.00	\$/ton bulk	8,670	BTU/lb	15.97				
Wood Chips	\$56.00	\$/ton (green)	9.9	mill BTU/Ton	5.70				
Ag Biomass	\$85-\$214	\$/ton	8,123	BTU/lb	5.20-13.20				
Mulch Hay	\$129-\$228	\$/ton	7,952	BTU/lb	8.11-14.34				
Source: Collabor, 2016 with Eucl prices undeted for NW/Vermont as of 12/1/2016									

**Fuel Cost Comparison** 

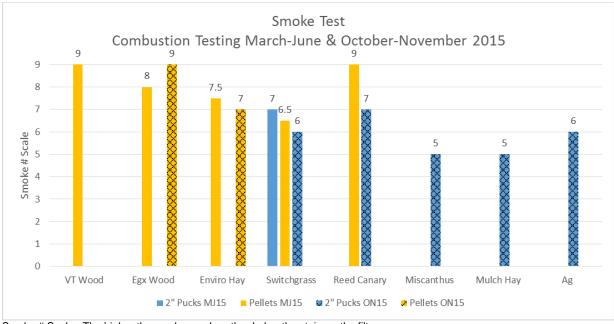
Source: Callahan, 2016 with Fuel prices updated for NW Vermont as of 12/1/2016

#### **Energy Content**

The Gross Calorific Values for the various grass and grass/wood blend samples ranged from 7,898 to 8,353 BTU/lb. for many of the 100% grass species tested and was within 7.6% of the 100% softwood (Vermont Wood Pellet) pellets and 3.66% of the 50% softwood / 50% hardwood (Energex) pellets. Even the Ag. Biomass sample (Figures 14-15, page 50) that was a mix of weeds, orchard grass and oak leaves had only 10.2% less energy value of the 100% softwood (Vermont Wood Pellet) pellets and it was just 6.3% less than the 50% softwood / 50% hardwood (Energex) pellets.

#### Smoke number comparison

A Wohler RP72 smoke test pump was used to collect and compare the level of staining on a filter paper sample drawn from the flue gases during the test burns. We visually match the stain on the filter paper with the standardized smoke level number scale numbered 0 - 9 with "0" representing no smoke detected and "9" representing a solid black stain. We interpreted the darker stains to represent more particulate matter in the flue gases. All of the 100% grass samples produced smoke test numbers that indicated lower smoke test numbers than either of the two wood pellet samples tested. The Giant Miscanthus and the mulch hay samples had the lowest smoke test numbers (5) compared to the wood pellets at 8 and >9. The 50% grass / 50% wood chip 2" diameter puck samples had smoke test numbers of 6, with only the 50% Switchgrass / 50% wood chip 2" diameter puck sample having a smoke number of 8.



Smoke # Scale : The higher the smoke number, the darker the stain on the filter paper. (0= no smoke detected; 9=solid black)

#### Ash

The Twin Ports lab results for the moisture free weight percentage or ash for the 100% grass samples ranged from 3.9% – 8.06% with Switchgrass pucks being the lowest and Reed Canarygrass pucks being the highest. The Mulch hay and Ag Biomass in 2" pucks were 6.8% and 5.35% ash respectively which was not surprising given the findings in previous biomass fuel studies. The 50% grass /50% wood chip 2" diameter puck samples had slightly higher ash percentages than the wood pellets or the 100% grass samples. It is interesting that the higher ash grass samples burned with the lowest smoke test numbers. Further research would be needed to determine the reason for this.

#### Ash Fusion Temperatures

Twin Ports tested each sample for the ash fusion temperature which is the temperature at which the residual ash becomes fluid. The ash contains minerals that the plants pick up from the soil and these minerals and the concentrations in a particular sample varies with each field and species of grass. The minerals in the ash influence the temperature at which the ash becomes fluid. When fluid ash cools it clumps together and often forms a hard clinker that can coat the components of the boiler in contact with the ash (Figure 32, page 59). Clinker and scale formation results in boiler operation and maintenance issues that can be difficult and time consuming to deal with. Large clinker pieces can restrict the air flow in the combustion chamber and they often jam ash removal augers. In extreme cases this requires the manual chipping of the clinker or slag to remove it from the boiler components which is time consuming. Higher ash fusion temperatures make it

less likely that clinkers or scale will form during the combustion process. The wood pellet samples had ash fusion temperatures in excess of 2,630 °F and no clinkers were observed during the testing. The 100% Switchgrass pellets had an ash fusion temperature 90 °F lower than the 100% softwood (Vermont Wood Pellet) pellets and only 40 °F lower for the 50% softwood / 50% hardwood (Energex) pellets. The Enviro Energy mulch hay pellets and the Reed Canarygrass pellets had an ash fusion temperature of 2,520 °F making them more likely to form clinkers which they did when the ash was left to cool between boiler heating cycles (Figure 32, page 59). We did not do ash fusion tests on the 50% grass / 50% wood chip 2" diameter puck samples but based on the findings in the BERC report (Sherman, 2011), we would expect the samples with some wood in them to have lower ash fusion temperatures than the 100% grass samples.

# Chlorine

Chlorine is a micronutrient which exists in the soil and it is absorbed by grasses and trees. Grasses typically contain higher levels of chlorine than trees or wood. When chlorine is combusted it can produce a corrosive gas that can attack the interior surfaces of heating equipment and the flue. For this reason the moving step grate (Figure 30, page 58) and the first and half of the second pass turbulators in the Evoworld boiler are constructed of stainless steel (Figures 10-11, page 48). The flue lining was constructed with 316 grade stainless steel with a 304 grade stainless steel outer jacket which have greater resistance to chlorine and sulfur that might be present in the flue gases. The 100% softwood (Vermont Wood Pellet) pellets had only 27 mg/gram of Chlorine, the 50% softwood / 50% hardwood (Energex) pellets had 102 mg/g, the Ag. Biomass (227 mg/g) and the Giant Miscanthus 2" diameter pucks (352 mg/g) had the lowest levels of chlorine among the grass samples, while the Enviro Energy mulch hay pellets (3,703 mg/g) and the Reed Canarygrass 2" diameter pucks (3,312 mg/g) had the highest levels. Not surprisingly the grass samples blended with percentages of wood all had lower chlorine levels than the 100% grass samples.

# Sulfur (SO2)

The presence of high levels of sulfur in a fuel source is an issue when sulfur is combusted it combines with oxygen to form Sulfur Dioxide (SO2) which is the chemical that causes acid rain. When sulfur dioxide condenses in heating equipment it is corrosive to the steel components. For this reason many boilers and flue liners, including the Evoworld boiler have stainless steel components in the areas that may experience contact with sulfur dioxide. In the Evoworld boiler, the step grate that forms the bottom of the combustion chamber, the first pass turbulators, the lower section of the second pass turbulators, and the flue liner are all constructed with stainless steel as a precaution.

The wood pellets tested had only 1-6 ppm of SO2, the grass samples tested with the highest levels of SO2 were the Enviro Energy mulch hay pellets that had average levels

between 74 - 93 ppm in the two test periods. The other 100% grass and 50% grass / 50% wood chip 2" diameter puck samples had SO2 levels from 0-4 ppm.

## Carbon Monoxide (CO)

Carbon Monoxide (CO) is a byproduct when any carbon containing fuel source is combusted incompletely. The presence of Carbon Monoxide in the environment in high concentrations is dangerous to any living breathing organism because it readily replaces oxygen in the bloodstream and can be fatal in cases of prolonged exposure. Carbon Monoxide as a product of combustion is a concern for air quality regulatory authorities because CO in the combustion gases is typically accompanied by other pollutants and other volatile organic compounds (VOC's) that form during incomplete combustion. In the U.S. the EPA sets maximum CO performance levels for heating equipment. CO levels were monitored because they help to indicate how well or poorly the various samples were performing as they were combusted in the Evoworld boiler. During the test runs we adjusted the fuel delivery rate and the air feed rate ranges in the Evoworld control software to allow the boiler sensors to automatically adjust these inputs during the combustion cycle. The goal was to have the lowest CO levels while also maintaining a low oxygen level while maximizing the calculated efficiency level. The data indicates that as we got better at adjusting the fuel and combustion air feed rates the CO levels decreased for all the samples while the efficiency increased. The data shows higher CO levels for the earlier testing period (March - June, 2015) and lower levels during the later round of testing when we worked with Christopher Callahan (October - November, 2015). All of the 100% grass samples had CO levels that were lower than the wood pellet samples, with Giant Miscanthus being the lowest. Notably both the 100% Mulch hay and 100% Ag Biomass 2" diameter pucks produced CO levels that were lower than the wood pellets. The 50% grass / 50% wood chip 2" diameter puck samples had CO levels that were similar to the 100% grass 2" diameter puck samples and significantly lower than the 100% grass pellet results.

#### Nitric Oxide (NO)

Nitric Oxide emissions are a product of combustion of fuels that contain nitrogen and is one of the particulates that contribute to smog and acid rain. Their production is increased with higher temperature combustion. Higher levels of NO are less desirable. In our testing the Enviro Energy mulch hay pellets and the Giant Miscanthus samples had lower levels of NO than the wood pellets. The other grasses tested yielded NO levels that were almost twice that of the wood pellets or the Enviro Energy mulch hay pellets or the Enviro Energy mulch hay pellets or the Giant Miscanthus pucks. The 50% grass / 50% wood chip 2" diameter puck samples had lower NO levels than the 100% grass samples but slightly higher levels than the wood pellets.

#### Comparison with the BERC Report Findings (Sherman, 2011)

The design features in the Evoworld HC100 Eco boiler proved to be up to the challenge of handling most of the issues that are typical when grass biomass is burned in a smaller commercial boiler. We thought it would be useful to retest many of the same species of grass and grass blended pellet samples in the Evoworld boiler that were tested in the BERC report authored by Adam Sherman in 2011 (Sherman, 2011). The combustion testing in the BERC report was done in a 500,000 BTU/Hour rated SolaGen wood pellet boiler. The SolaGen boiler larger than the Evoworld unit and it did not have a perforated combustion shelf where primary air is introduced below the fuel pile. The SolaGen boiler introduced primary air from the sides of the combustion chamber. Both boilers relied on the new fuel coming into the combustion chamber to push the burning fuel forward where it would be conveyed out of the boiler by the ash removal auger into a storage container. The SolaGen boiler air and fuel feed rates could be adjusted through the control software but the boiler software could not continuously adjust these inputs during the combustion process the way the Evoworld boiler does.

In general the results for the various grass species tested were consistent. In a few cases there were differences. The BERC report only tested 1/4" diameter pellet fuel and they found that some of the 100% grass pellet samples did not hold together as well as the grass/wood blend samples. The 1/4" pellets for this project were manufactured by Bob Miller at Enviro Energy and their process produced a dense, hard pellet that held its shape. The BERC report found that the Switchgrass samples had the lowest ash content of the grasses tested with 4.3%. In this project the Giant Miscanthus 2" diameter pucks yielded 3.9% ash and mulch hay pellets had 4.98% ash. The Switchgrass pellets tested in the BERC report had contained 2% more calorific energy than the 100% softwood (Vermont Wood Pellet) pellets had 7.6% more calorific energy than the Switchgrass pucks, and the 50% softwood / 50% hardwood (Energex) pellets had only 3.6% more calorific energy than the Switchgrass 2" diameter pucks.

The BERC report also tested grass/wood blended pellets in 6%, 12%, and 25% percentages of the grass species tested. When we retested these same blended samples in the Evoworld boiler we saw similar trends to the BERC findings. The higher percentages of wood had higher calorific values, higher combustion efficiency, lower CO, SO2 and Chlorine levels than the 100% grass samples. There were fewer distinctions in the ash fusion temperatures and the NO levels.

In both reports, not surprisingly, the wood pellet samples had higher ash fusion temperatures than the grass samples tested with Switchgrass being the closest with an ash fusion temperature within 40° F of the 50% softwood / 50% hardwood (Energex) pellets tested. All of the grasses tested had lower combustion efficiency than the wood pellets, with the Ag Biomass sample being within 1.2% of the 50% softwood / 50% hardwood (Energex) pellets. All of the grasses tested had higher NO and Chlorine

amounts, but only the Enviro Energy mulch hay pellets had higher SO2 levels than the wood pellets sampled.

The BERC study used an EPA certified emission testing service with a portable laboratory to provide particulate emission data that showed the mulch hay sample to have the highest particulates followed by Reed Canarygrass and Switchgrass, with the wood pellets having the lowest particulate levels. We tested particulate emissions for the Evoworld boiler using the Wohler RP72 smoke test pump sample method and the wood pellet samples had higher smoke test numbers than all of the grass samples. The sophistication of the sampling methods and the design differences between the boilers may explain this difference.

The BERC report concluded that grass fuels and the issues associated with them are best suited to the commercial users; and that more research is needed to identify boilers that can handle grass fuel and the economic feasibility of making and distributing grass or grass/wood blended fuel. At the time the BERC project research was done Evoworld boilers were not being imported or built in the U.S. and there were fewer options available to densify grass biomass into a pellet or a puck form.

# Conclusions and Recommendations

The data obtained in the project confirmed that the Evoworld HC 100 Eco wood chip boiler could burn a variety of grass species, grass/wood blends, and handle two different fuel size forms efficiently and cleanly. The data obtained confirmed that the goals of this project were met.

This project provides new data on the operational performance and costs of operating a production wood chip boiler made in the U.S. with ASME and U.L. certification that efficiently and cleanly burns a variety of grass grown in Vermont and the U.S.

This project would benefit any farm, light industrial plant, or a facility served by a central heating plant in a location that provides access to grass biomass fuel sources and the space to store and handle them in bulk. This project would be especially beneficial to farm operators who have the capability to harvest grass biomass from non-prime agricultural fields, abandoned pasture land, roadsides, or erosion buffer strips that are typically cut only once a season.

Operating a boiler of this size and type on locally grown mulch quality hay, grass biomass or agricultural crop residue rather than harvesting grown trees for chips or pellets presents numerous benefits. Natural resource protection including reducing soil erosion, runoff, and reducing water contamination from soil minerals are obvious benefits because land can be left in perennial grass cover. Perennial grasses are a crop that grows back each season and can be grown on marginal soils or non-prime agricultural areas. The Evoworld boiler we tested offers a viable alternative to burning wood biomass fuel because it can handle the issues unique to burning grass biomass.

Being able to locally grow, harvest, densify and burn a grass biomass fuel keeps dollars in the local economy which is a major economic benefit (Wilson, 2014).

Analysis by Christopher Callahan in his 2016 report based on data collected during this project demonstrated that harvesting, densifying and burning locally harvested grass or other forms of agricultural biomass can compare favorably with the present price of wood chips, wood pellets, and less than # 2 fuel oil (Callahan, 2016 and the table on page 28). This project demonstrated that when the cost of petroleum fuels increase, agricultural biomass and grass fuel can represent a viable fuel source that every farm has access to.

The cost to purchase and install a wood chip boiler with features similar to the Evoworld model we tested exceeds the cost for a similarly sized # 2 fuel oil boiler by two times for our facility, and it could be higher depending on the application (Budget Estimate, page 85). The fact that the Evoworld boiler was designed to handle wood chips allows it to accept a variety of biomass fuels types and form sizes. The cost per unit for some of

these biomass fuels allows the payback period for the installation to be reduced over time (Callahan, 2016).

The limiting factor to using agricultural biomass or grass as a fuel for space heat today remains the lack of sources to densify the biomass into 1/4" pellets or 2" diameter pucks. The data collected as a part of this project and analysis performed by Christopher Callahan indicated that the cost to produce the 2" diameter pucks would come down if a steady market demand for these pucks existed (Callahan, 2016).

Based on our experience during this project we recommend adding a sweeper arm or paddle to the firebox combustion shelf where the primary air is introduced (Figure 7, page 46). Activating this sweeper arm at the beginning of each programmed cleaning cycle would remove the unburned residue and any clinkers between each burn cycle. We believe that a modification to the fire box such as this should allow this boiler to operate continuously on grass fuel in these size forms.

#### Opportunities for future study

In this project a great deal was learned about how to optimize the combustion of different grasses, blends of biomass, and form sizes. I believe it would be beneficial to continue to work with the 1/4" diameter pellet sized fuel to solve the issues we experienced with clinker formation and decreasing combustion performance.

Given the success we achieved burning 2" diameter pucks it would be interesting to test other form sizes such as commercially available cubes or larger diameter pellets.

We intend to more closely monitor the hours of operation following the complete cleaning of the boiler tubes, sand blasting and brushing the stainless steel turbulators, and the replacement of the carbon steel turbulators in the second pass tubes. It would be useful to know if the rusting we experienced over the summer and fall of 2016 was caused in any part by the by-products of the grass combustion, or simply due to humidity in the air being drawn through the boiler when it was shut down.

Given the success we had with a variety of grasses, blends and wood pellets, I would like to test other types of biomass or crop residue in a densified form. Fuel sources for consideration could include shredded paper, cardboard, invasive plants such as buckthorn and honey suckle, aquatic nuisance weeds, and waste from food industry processing.

Having identified the need to remove partially burned fuel from the boiler's combustion shelf, it would be useful to work out a solution for that issue, make the necessary modifications, and test the operation of the boiler after making the modification until that problem has been solved. A sketch of what this modification might look like can be found in Figure 7 on page 46.

We were fortunate to have an opportunity to contribute to the research on grass biomass combustion in small sized commercial boilers and we look forward to continuing to work with the Evoworld boiler.

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Appendices & Project Photos

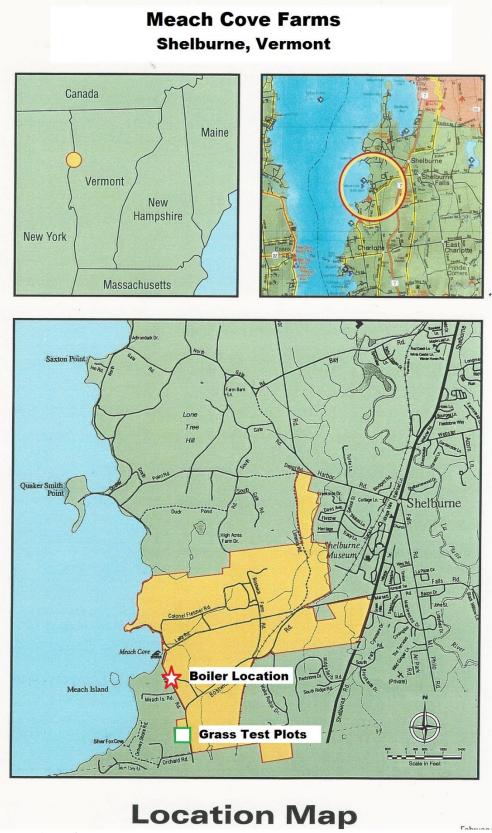


Figure 1 Meach Cove Farms Location Map

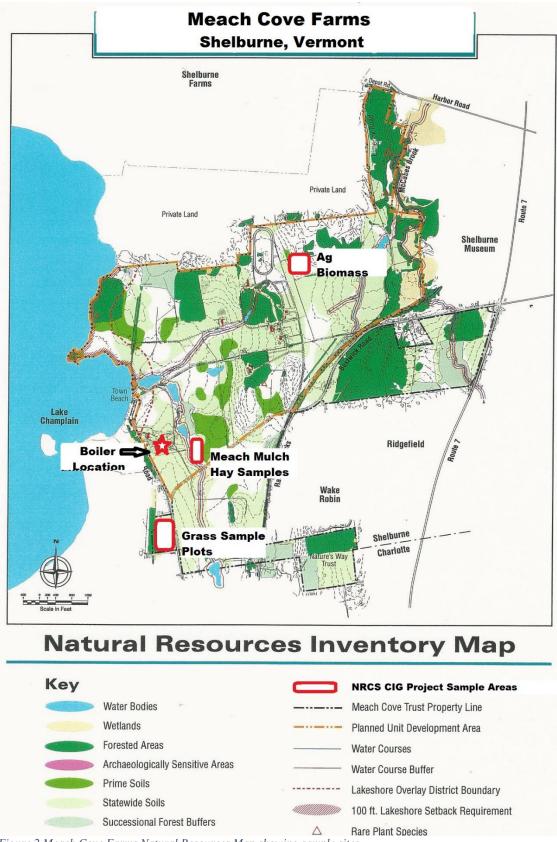
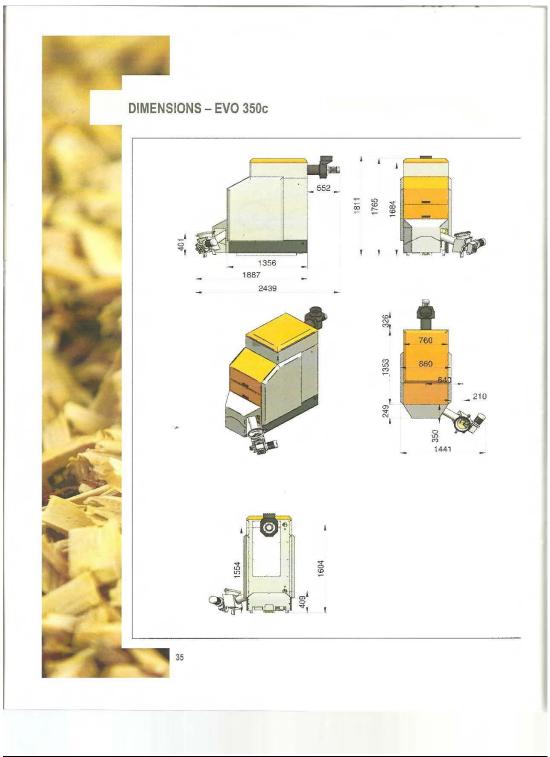


Figure 2 Meach Cove Farms Natural Resources Map showing sample sites

# Evoworld HC 100 (350C) Eco Boiler Specifications

Max. aliable bolier temperature (°F)       185       185       194         Permited operating pressure (sp)       43.5       5.6         CE labeling (acc. to low-voltage directive) UL2S23. ASME Sec IV       CE/UL/ASME       CE/UL/ASME<				AND A DOWNLOAD	
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Total depth (Inch)       65       71.5       100         Boller hold, (Inch)       59.5       77.7       52.6         Boller hold, (Inch)       61.4       70       63.7         Ever height (Inch)       61.6       17.3       22.2         Ventilistion height (Inch)       61.6       17.3       22.2         Ventilistion height (Inch)       61.6       17.3       22.2         Ventilistion height (Inch)       61.5       70       61.5         Boller tube connection diameter (Inch)       7.87       11.8       15.75         VATER       Ventilistion height (Inch)       6.1.2       7       7         Max. wood chip size       6.30 - 6.50       6.30 - 6.50       6.30 - 6.50         Max. wood chip water content       w 35       w 35       w 35         Ach REMOVAL       auto       auto       auto       auto         As record chip water content       1 ½       2       4         Refurm (Inch)       1	Boiler width (inch)				
Boler height (inch) 99.5* 77* 92.5* Boler bube connection height (inch) 51.2 77.13 80.7 Flow height (inch) 61.4 70 88.7 Return height (inch) 16.1 17.3 22.2 Ventation height (inch) 17.87 11.8 15.75 Ventation height (inch) 17.87 11.8 15.75 Ventation height (inch) 16.1 7.87 11.8 15.75 Ventation height (inch) 17.87 11.8 15.75 Ventation height (inch) 18.2 12.7 7 7 Max wood chip size 0.39 - 65.0 0.90 - 65.0 0.90 - 65.0 Max wood chip size 0.39 - 65.0 0.90 - 65.0 0.90 - 65.0 Max wood chip size 0.39 - 65.0 0.90 - 65.0 0.90 - 65.0 Max wood chip size 0.39 - 65.0 0.90 - 65.0 0.90 - 65.0 Max wood chip size 0.30 - 0.00 - 0.1 0.00 0.1 - 0.3 / 10 - 30 0.1 - 0.3 / 10 - 30 0.1 - 0.3 / 10 - 30 0.1 - 0.3 / 10 - 30 0.1 - 0.3 / 10 - 30 0.1 - 0.3 / 10 - 30 0.1 - 0.3 / 10 - 30 0.1 - 0.3 / 10 - 30 0.1 - 0.3 / 10 - 30 0.1 - 0.3 / 10 - 30 0.0 - 0.1 / 0 - 10 0.0	Boiler depth (inch)				
Boller tube connection height (inch) 61:2 71:3 80.7 Few height (inch) 61:4 70 83.7 Return height (inch) 61:5 70 81:5 Boller tube connection diameter (inch) 7:7 11:8 15:75 Ventilation height (inch) 60 18:5 70 81:5 Boller tube connection diameter (inch) 7:7 11:8 15:75 VATER Water content (gals.) 40 60 180 Return action for the second diameter (inch) 7:7 7 7 7 Max wood chip size 6.30 - 650 6.30 - 650 6.30 - 650 Max. wood chip size 6.30 - 650 6.30 - 650 6.30 - 650 Max. wood chip size 6.30 - 650 6.30 - 650 6.30 - 650 Max. wood chip size 6.30 - 650 6.30 - 650 7 Max. wood chip size 7.7 7 Max wood chip size 7.7 7 Contrastion chamber temperature (TF) 7 Contrastion chamber temperature (T					
Flow height (inch)       61.4       70       63.7         Return height (inch)       61.5       70       61.5         Baier tube connection diameter (inch)       7.87       11.8       15.75         Watter content (gals.)       40       60       160         Watter content (gals.)         Watter Content         Boline Maxwood Chip water content         Watter Content         Watter Content         Colspan="2">Colspan="2">Colspan="2">Colspan="2">Colspan="2">Colspan="2">Colspan="2">Colspan="2">Colspan="2">Colspan="2"Colspan="2"Colspan="2"Colspan="2"Colspan="2"Colspan="2"Cols					
Ventiliation height (inch)       61.5       70       81.5         Boiler tube connection diameter (inch)       7.87       11.8       15.75         VATER       40       60       190         FUE       7       7       7         Max wood chip size       6.30       6.50       6.30       6.50         Max wood chip size       6.30       6.50       6.30       6.50         Max wood chip size       6.30       6.50       6.30       6.50         For Construct       35       w.35       w.35       w.35         ASH REMOVAL       40       auto       auto       auto       auto         Return (inch)       1.½       2       4       4         Return (inch)       1.½       2       4       4         Required negative pressure at full load (mbar/Pa)       0,1 - 0.3/10 - 30       0,1 - 0.3/10 - 30       0,1 - 0.3/10 - 30         Required negative pressure at full load (mbar/Pa)       0,1 - 0.3/10 - 10       0,0 - 0,1 / 0 - 10       0,0 - 0,1 / 0 - 10       0,0 - 0,1 / 0 - 10         Constation chamber temperature (°F)       ca.1630       ca.1630       ca.1630       ca.1630         Co at full load (mg/m)       103       122       133       422	Flow height (inch)				
Bolier tube connection diameter (inch)       7.87       11.8       15.75         WATER	Return height (inch)				
Water content (gals)         40         60         160           FUE         7         7         7           Max wood rbip size         G.30 - G.50         G.30 - G.50         G.30 - G.50         G.30 - G.50           Max wood rbip size         G.30 - G.50         G.50         G.30 - G.50         G.50         G.50         G.50         G.50         G.50         G.50         G.50         G.50	Ventilation height (inch)				-
Water content (galis)       40       60       180         FUEL       7       7         Ash box volume (cu. ft.)       2.12       7       7         Max. wood chip water content       w 35       w 35       w 35         Max. wood chip water content       w 35       w 35       w 35         Ash fremoval       auto       auto       auto         CONNECTIONS       11%       2       4         Return (inch)       11%       2       4         Return (inch)       11%       2       4         Required negative pressure at full load (mbar/Pa)       0,1 - 0,3 / 10 - 30       0,1 - 0,1 / 0 - 10         Constation chade, fing/m?)       Ca 1830       ca 1830<	Boiler tube connection diameter (inch)	7.87	11.8	15.75	The second second
EVEL         2.12         7         7           Max. wood chip size         C 30 - G 50         C 30 - G 50         C 30 - G 50           Max. wood chip size         0 30 - G 50         C 30 - G 50         C 30 - G 50           Max. wood chip size         0 30 - G 50         W 35         W 35           ASH REMOVAL         auto         auto         auto         auto           Ash removal         auto         auto         auto         auto           600NECTIONS         1%         2         4           Required negative pressure at full load (mbar/Pa)         0,1 - 0,3/10 - 30         0,1 - 0,3/10 - 30           Construction chamber temperature (°F)         ca. 1830         ca. 1830         ca. 1830           Co at full load (mg/m²)         102         272         1523         423           NOx at tylin load (mg/m²)         1083         107*         104         3107*           HO at stril load (mg/m²)         103         53         57*         103         53           Dust at full load (mg/m²)         103         5*         5         6         6         6           Dust at full load (mg/m²)         103         5*         5         5         5         5         6         6 <td>WATER</td> <td>THE REAL PROPERTY AND</td> <td></td> <td></td> <td>6 30</td>	WATER	THE REAL PROPERTY AND			6 30
Ash box volume (cu ft.)       2.12       7       7         Max. wood chip size       G.30 - G.50       G.90 - G.50       G.90 - G.50         Max. wood chip size       w.35       w.35       w.35         Ash removal         auto       auto       auto       auto         Ash removal         Colspan="2">Ash removal         Ash removal         Colspan="2">Ash removal         Colspan="2">Ash removal         Colspan="2">Ash removal         Colspan="2">Colspan="2"Colspa="2"Col	Water content (gais.)	40	60	160	and the same
Max. wood chip size       G 30 - G 50         Max. wood chip water content       w 35       w 35       w 35       w 35         Ast removal         auto       auto         auto       auto         CONNECTIONS         ENVISION DATA         Required negative pressure at full load (mbar/Pa)       0,1 - 0,3 / 10 - 30       0,1 - 0,3 / 10 - 30       0,1 - 0,3 / 10 - 30       0,1 - 0,3 / 10 - 30       0,1 - 0,3 / 10 - 30       0,1 - 0,3 / 10 - 30       0,1 - 0,3 / 10 - 30       0,1 - 0,3 / 10 - 30       0,1 - 0,3 / 10 - 30       0,1 - 0,3 / 10 - 30       0,1 - 0,3 / 10 - 30       0,1 - 0,3 / 10 - 30       0,1 - 0,3 / 10 - 30       0,1 - 0,3 / 10 - 30       Colspan="2">Colspan="2"       Colspan="2"	FUEL			1 - 10 010 - 11	
Max. wood chip water content       w 35       w 35       w 35         ASH REMOVAL       auto       auto       auto       auto         Ash removal       auto       auto       auto       auto         GONNECOTIONS       11½       2       4         Return (inch)       11½       2       4         Return (inch)       11½       2       4         CONNECOTIONS       11½       2       4         Required negative pressure at full load (mbar/Pa)       0,1 - 0,3 / 10 - 30       0,1 - 0,3 / 10 - 30       0,1 - 0,3 / 10 - 30         Required negative pressure at parl load (mbar/Pa)       0,0 - 0,1 / 0 - 10       0,0 - 0,1 / 0 - 10       0,0 - 0,1 / 0 - 10       0,0 - 0,1 / 0 - 10         Co at tuil load (mg/m <sup>3</sup> )       212 <sup>3</sup> 53 <sup>3</sup> 42 <sup>3</sup> 73 <sup>3</sup> NOX at parl load (mg/m <sup>3</sup> )       10 <sup>8</sup> 107 <sup>2</sup> 162 <sup>2</sup> HC at parl load (mg/m <sup>3</sup> )       1 <sup>8</sup> 1 <sup>3</sup> <2 <sup>2</sup> Dust at full load (mg/m <sup>3</sup> )       1 <sup>8</sup> 1 <sup>3</sup> <2 <sup>2</sup> LC at full load (mg/m <sup>3</sup> )       1 <sup>8</sup> 1 <sup>3</sup> <2 <sup>2</sup> Dust at parl load (mg/m <sup>3</sup> )       1 <sup>8</sup> 1 <sup>3</sup> <2 <sup>2</sup> Dust at parl load (mg/m <sup>3</sup> )       0 <sup>4</sup> 0,4 <td></td> <td></td> <td></td> <td></td> <td>141</td>					141
ASH REMOVAL         Ash removal       auto       auto       auto       auto         GONNECTIONS					
Ash removal       auto       auto       auto       auto         CONNECTIONS         Flow (inch)       1½       2       4         Return (inch)       1½       2       4         Return (inch)       1½       2       4         EMMISION DATA		W 35	W 35	w 35	C. P
Flow (inch)       1 ½       2       4         Return (inch)       1 ½       2       4         Return (inch)       1 ½       2       4         EMMISION DATA         Required negative pressure at part load (mbar/Pa)       0,1-0,3 / 10-30       0,1-0,3 / 10-30       0,1-0,3 / 10-30       0,0-0,1 / 0-10         Colspan="2">Colspan="2"Colspa="2"Colspan="2"Col	ASH REMOVAL Ash removal	auto	auto	auto	1
Flow (inch)       1 ½       2       4         Return (inch)       1 ½       2       4         Return (inch)       1 ½       2       4         EMMISION DATA         Required negative pressure at part load (mbar/Pa)       0,1-0,3 / 10-30       0,1-0,3 / 10-30       0,1-0,3 / 10-30       0,0-0,1 / 0-10         Colspan="2">Colspan="2"Colspa="2"Colspan="2"Col	CONNECTIONS				Sala - P
	Flow (inch)	1 1/2	2	4	State of
EMMISION DATA           Reguired negative pressure at full load (mbar/Pa)         0,1 - 0,3 / 10 - 30         0,1 - 0,3 / 10 - 30         0,1 - 0,3 / 10 - 30         0,1 - 0,3 / 10 - 30         0,1 - 0,3 / 10 - 30         0,1 - 0,3 / 10 - 30         0,1 - 0,3 / 10 - 30         0,1 - 0,3 / 10 - 30         0,1 - 0,3 / 10 - 30         0,1 - 0,3 / 10 - 30         0,1 - 0,3 / 10 - 30         0,1 - 0,3 / 10 - 30         0,1 - 0,3 / 10 - 30         0,1 - 0,3 / 10 - 30         0,1 - 0,3 / 10 - 30         0,0 - 0,1 / 0 - 10         0,1 / 0,2 / 0,1         0,1 - 0,1 / 0,1 / 0,1 / 0,2         10         10 + 12 + 1 + 2         162 + 10 + 10 + 10 + 10 + 10 + 10 + 10 + 1	Return (inch)	1 1/2	2	4	1000
Required negative pressure at full load (mbar/Pa)       0,1 - 0,3 / 10 - 30       0,1 - 0,3 / 10 - 30       0,1 - 0,3 / 10 - 30       0,1 - 0,3 / 10 - 30       0,1 - 0,3 / 10 - 30       0,1 - 0,3 / 10 - 30       0,1 - 0,3 / 10 - 30       0,0 - 0,1 / 0 - 10       0.0 - 0,1 / 0 - 0,2       0.0 - 0,2       0.1 - 0,2       0.0 - 0,2       0.1 - 0,2       0.0 - 0,2       0.1 - 0,2       0.0 - 0,2       0.0 - 0,2       0.1 - 0,			STATE OF STATE		m
Required negative pressure at part load (mbar/Pa)       0,0-0,1/0-10       0,0-0,1/0-10       0,0-0,1/0-10       0,0-0,1/0-10         Combustion chamber temperature (*F)       ca. 1830       ca. 1830       ca. 1830       ca. 1830         CO at tuil load (mg/m <sup>3</sup> )       1212       533       423         CO at part load (mg/m <sup>3</sup> )       1103       1272       1624         NOX at full load (mg/m <sup>3</sup> )       1103       1073         HC at full load (mg/m <sup>3</sup> )       1083       1073         HC at full load (mg/m <sup>3</sup> )       1043       1073         HC at full load (mg/m <sup>3</sup> )       103       53         Dust at full load (mg/m <sup>3</sup> )       103       53         Dust at full load (mg/m <sup>3</sup> )       103       53         ELECTRIC FOWER CONSUMPTION       200/240 V 1- or 3- 220/240 V 1- or 3		0,1 - 0,3 / 10 - 30	0,1-0,3/10-30	0,1 - 0,3 / 10 - 30	t - L
CO at full load (mg/m <sup>3</sup> )       212 <sup>3</sup> 53 <sup>3</sup> 42 <sup>3</sup> CO at part load (mg/m <sup>3</sup> )       48 <sup>3</sup> 73 <sup>3</sup> 162 <sup>3</sup> NOX at full load (mg/m <sup>3</sup> )       10 <sup>3</sup> 127 <sup>3</sup> 162 <sup>3</sup> NOX at part load (mg/m <sup>3</sup> )       10 <sup>3</sup> 127 <sup>3</sup> 162 <sup>3</sup> NOX at full load (mg/m <sup>3</sup> )       4 <sup>2</sup> 1 <sup>3</sup> <2 <sup>3</sup> HC at full load (mg/m <sup>3</sup> )       4 <sup>2</sup> 1 <sup>3</sup> <2 <sup>3</sup> Dust at full load (mg/m <sup>3</sup> )       1 <sup>2</sup> 1 <sup>2</sup> 1 <sup>3</sup> Dust at full load (mg/m <sup>3</sup> )       10 <sup>3</sup> 5 <sup>3</sup> ELECTIC POWER CONSUMPTION       220/240 V 1- or 3-       220/240 V 1- or 3-       220/240 V 1- or 3-         Standby (W)       5       6       6       6         Power consumption at full load in % of full load       0.4       0.3       0.3         Power consumption at part load in % of part load       0.2       0.1       0.2         1) excl. exhaust fan / stoker 2) excl. chimney box 3) emissions data based on 13 % O2 dry       4) tested with exhaust cyclone	Required negative pressure at part load (mbar/Pa)				-
CO at part load (mg/m <sup>3</sup> )       48 <sup>a</sup> 73 <sup>a</sup> NOX at full load (mg/m <sup>3</sup> )       110 <sup>a</sup> 127 <sup>a</sup> 162 <sup>a</sup> NOX at part load (mg/m <sup>3</sup> )       108 <sup>a</sup> 107 <sup>a</sup> HC at full load (mg/m <sup>3</sup> )       4 <sup>a</sup> 1 <sup>a</sup> 2 <sup>a</sup> HC at full load (mg/m <sup>3</sup> )       4 <sup>a</sup> 1 <sup>a</sup> -         Dust at full load (mg/m <sup>3</sup> )       1 <sup>a</sup> 1 <sup>a</sup> -         Dust at full load (mg/m <sup>3</sup> )       1 <sup>a</sup> 1 <sup>a</sup> -         Dust at part load (mg/m <sup>3</sup> )       1 <sup>a</sup> 5 <sup>a</sup> -         ELECTRIC POWER CONSUMPTION       Standby (W)       5 <sup>a</sup> 6 <sup>b</sup> Standby (W)       5 <sup>b</sup> 6 <sup>b</sup> 6         Power consumption at part load in % of part load       0,2 0,1 0,2       0,2         1) excl. exhaust fan / stoker 2) excl. chimney box 3) emissions data based on 13 % O2 dry       4) tested with exhaust cyclone	Combustion chamber temperature (°F)				10
NOx at full load (mg/m <sup>2</sup> )       110 <sup>3</sup> 127 <sup>3</sup> 162 <sup>3</sup> NOx at part load (mg/m <sup>2</sup> )       108 <sup>3</sup> 107 <sup>2</sup> HC at tull load (mg/m <sup>2</sup> )       4 <sup>3</sup> 1 <sup>3</sup> <2 <sup>3</sup> HC at part load (mg/m <sup>2</sup> )       1 <sup>3</sup> 1 <sup>3</sup> <2 <sup>3</sup> Dust at full load (mg/m <sup>2</sup> )       1 <sup>3</sup> 1 <sup>3</sup> Dust at part load (mg/m <sup>2</sup> )       1 <sup>3</sup> 1 <sup>3</sup> Dust at part load (mg/m <sup>3</sup> )       10 <sup>3</sup> 5 <sup>3</sup> ELECTRIC POWER CONSUMPTION       220/240 V 1 <sup>-</sup> or 3 <sup>-</sup> 3 <sup>-</sup> Standby (W)       5       6       6         Power consumption at full load in % of full load       0.4       0.3       0.3          Power consumption at part load in % of part load       0.2       0.1       0.2          1) excl. exhaust fan / stoker       2) excl. chimney box       3) emissions data based on 13 % O2 dry       4) tested with exhaust cyclone				42 3	
NOx at part load (mg/m <sup>3</sup> )         108 <sup>a</sup> 107 <sup>a</sup> HC at full load (mg/m <sup>3</sup> )         4 <sup>a</sup> 1 <sup>a</sup> <2 <sup>a</sup> HC at part load (mg/m <sup>3</sup> )         1 <sup>a</sup> 1 <sup>a</sup> Dust at full load (mg/m <sup>3</sup> )         1 <sup>a</sup> 1 <sup>a</sup> Dust at full load (mg/m <sup>3</sup> )         10 <sup>a</sup> 5 <sup>a</sup> Dust at part load (mg/m <sup>3</sup> )         10 <sup>a</sup> 5 <sup>a</sup>				162.3	
HC at full load (mg/m <sup>3</sup> )       4 <sup>3</sup> 1 <sup>3</sup> <2 <sup>3</sup> HC at part load (mg/m <sup>3</sup> )       1 <sup>a</sup> 1 <sup>a</sup>				102	1001
HC at part load (mg/m <sup>3</sup> )       1 <sup>3</sup> Dust at trail load (mg/m <sup>3</sup> )       20 <sup>3</sup> 39 <sup>3</sup> 57 <sup>3</sup> Dust at part load (mg/m <sup>3</sup> )       10 <sup>3</sup> 5 <sup>3</sup> ELECTRIC POWER CONSUMPTION       Standby (M)       5       6       6         Standby (W)       5       6       6       6         Power consumption at full load in % of full load       0.4       0.3       0.3         Power consumption at part load in % of part load       0.2       0.1       0.2         1) excl. exhaust fan / stoker       2) excl. chimney box       3) emissions data based on 13 % O2 dry         4) tested with exhaust cyclone       4       13 % O2 dry	HC at full load (mg/m <sup>3</sup> )			<23	A LE M
Dust at part load (mg/m³)     10 <sup>3</sup> 5 <sup>3</sup> ELECTRIC POWER CONSUMPTION     Supply needed     220/240 V 1~ or 3~ 220/240	HC at part load (mg/m³)				and the second second
ELECTRIC POWER CONSUMPTION         Supply needed       220/240 V 1~ or 3~ 220/240 V 1~	Dust at full load (mg/m <sup>3</sup> )			57 3	-
Supply needed       220/240 V 1~ or 3~ 220/240 V 1~ or 3~ 220/240 V 1~ or 3~         Standby (W)       5       6       6         Power consumption at full load in % of full load       0.4       0.3       0.3         Power consumption at part load in % of part load       0.2       0.1       0.2         1) excl. exhaust fan / stoker       2) excl. chimney box       3) emissions data based on 13 % O2 dry         4) tested with exhaust cyclone       0       0.2       0.1       0.2	Dust at part load (mg/m <sup>3</sup> )	10 3	53		
Standby (W)       5       6       6         Power consumption at full load in % of full load       0.4       0.3       0.3         Power consumption at part load in % of part load       0.2       0.1       0.2         1) excl. exhaust fan / stoker       2) excl. chimney box       3) emissions data based on 13 % O2 dry         4) tested with exhaust cyclone       0       0.2       0.1       0.2	ELECTRIC POWER CONSUMPTION	in a second			-
Power consumption at full load in % of full load 0.4 0.3 0.3 Power consumption at part load in % of part load 0.2 0.1 0.2 1) excl. exhaust fan / stoker 2) excl. chimney box 3) emissions data based on 13 % O2 dry 4) tested with exhaust cyclone	Supply needed			22	
Power consumption at part load in % of part load 0,2 0,1 0,2 1) excl. exhaust fan / stoker 2) excl. chimney box 3) emissions data based on 13 % O2 dry 4) tested with exhaust cyclone					Con Part
4) tested with exhaust cyclone	Power consumption at part load in % of part load				-
4) tested with exhaust cyclone	1) excl exhaust fan / stoker 2) excl chimneu hou 3) emissions date h	ased on 13 % O2 dov			The loss
		ased on 13 % O2 dry			1
8					
8				8	
8				And and a state of the state of	Charles -
				8	Contraction of the
				Ser. Ser	8

Figure 3 Evoworld HC 100 (350C) Eco boiler Specifications



# Evoworld HC 100 (350C) Eco Boiler Dimensions in Millimeters

Figure 4 Evoworld HC 100 (350C) Eco Boiler Dimensions

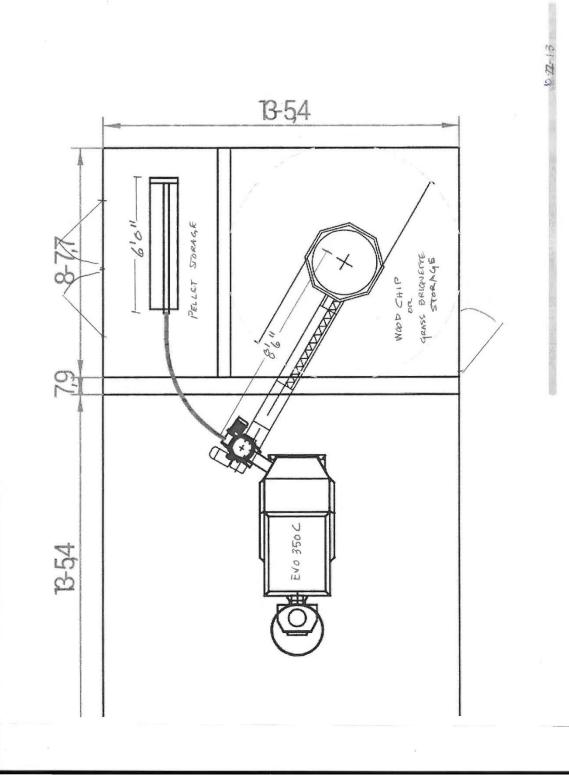


Figure 5 Evoworld boiler fuel system layout, 10-22-2013

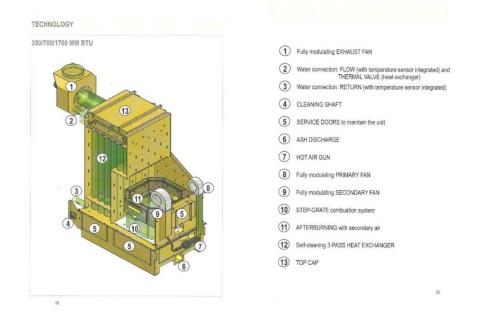


Figure 6 Evoworld boiler parts diagram and key

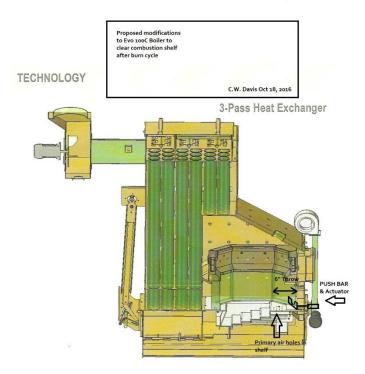


Figure 7 Evoworld boiler with modifications to clear combustion shelf, 10-18-2016

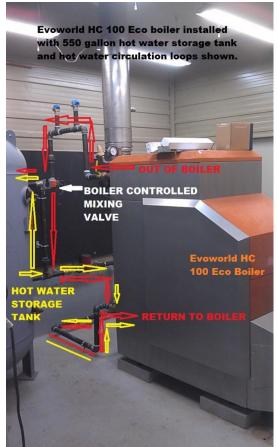


Figure 8 Evoworld boiler and buffer tank loop, 2-22-2017

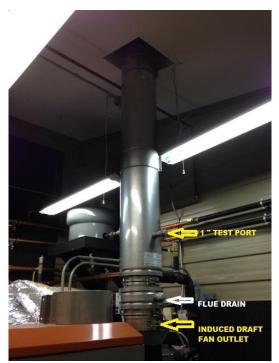


Figure 9 Evoworld HC 100 Eco boiler - 8" flue showing test port, 6-23-2015



Figure 10 Close-up of turbulators new and 890 hours of operation, 12-20-2016

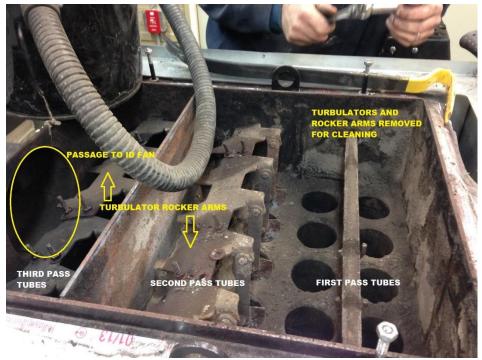


Figure 11 Top of boiler open for cleaning after 890 hours of operation, 12-20-2016

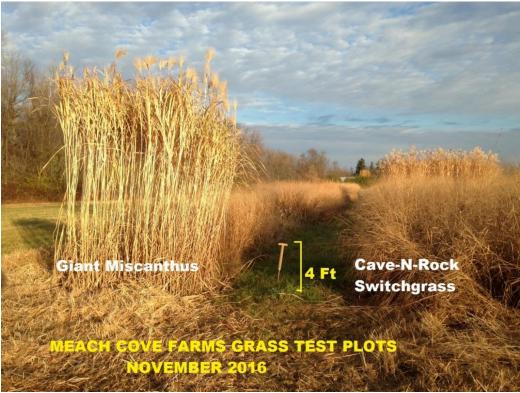


Figure 12 Meach Cove Farms grass test plots, 11-15-2016



Figure 13 Switchgrass round bales - Meach Cove 11-15-2016



Figure 14 Meach Cove Ag Biomass bales before grinding, 11-23-2015 (Photo courtesy of C. Callahan)



Figure 15 Meach cove Ag biomass square bales with leaves, 11-23-2015(Photo courtesy of C. Callahan)

# 2" Puck Production



Figure 16 Adam Dantzscher explains biomass densification equipment (BHS "Slugger"), August 2015



Figure 17 1/4" diameter pellet form and 2" diameter "puck" form



Figure 18 Pucks in bulk bags at Meach Cove in storage waiting for testing



Figure 19 Evoworld chip conveyor in fuel bin, 2" puck fuel, 2015



Figure 20 Evoworld HC 100 wood chip conveyor loaded with 2" pucks, March 2015



Figure 21 Mulch hay pucks during combustion cycle, March 2015

# **Pellet Production**



Figure 22 Enviro Energy, Wells Bridge, NY - Hay chopping equipment, 12-6-2011



Figure 23 Enviro Energy pellet plant interior, grinder and dryer, 12-6-2011



Figure 24 Bob Miller (left) and his son Mike Miller, Enviro Energy, 12-6-2011



Figure 25 Enviro Energy 1/4" Diameter mulch hay pellets

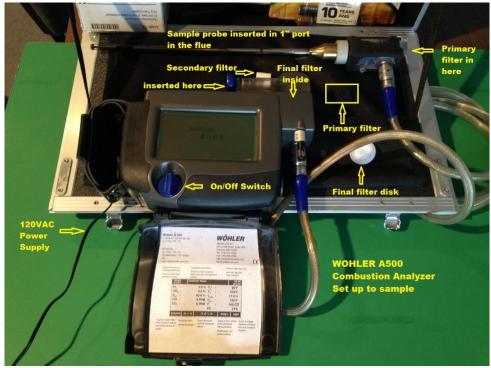


Figure 26 Wohler A500 Emission Analyzer



Figure 27 Wohler RP72 Smoke Test Pump

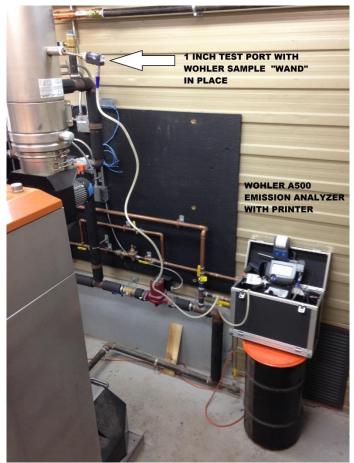


Figure 28 Wohler A500 set-up to sample, March 2015



Figure 29 Wohler A500 screen view, mulch hay pellet test, and 3-16-2015

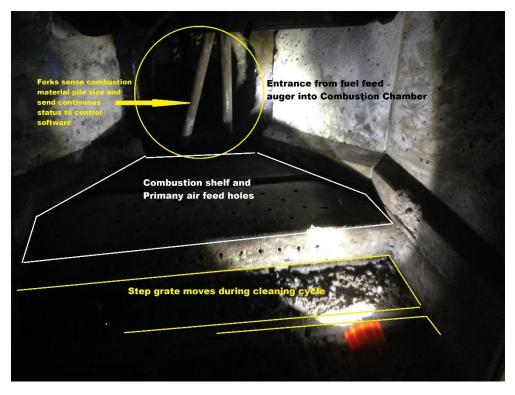


Figure 30 Clean combustion chamber with components labeled, 2015

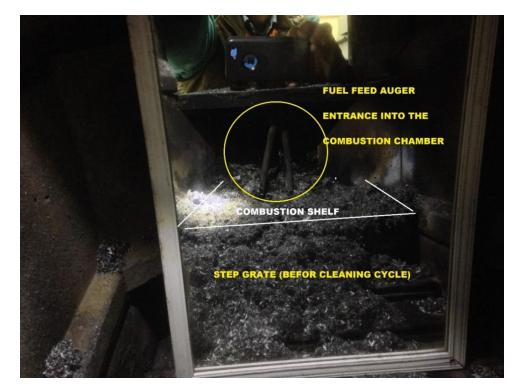


Figure 31 Grass puck post burn residue in the combustion chamber, 2015



Figure 32 Evoworld HC 100 combustion chamber with grass pellet residue, March 2015



Figure 33 Enviro Energy hay pallets, clinker, 3-10-2015



Figure 34 Sid Bosworth presenting to a UVM Biomass Energy class at Meach Cove, 3-25-2016



Figure 35 Sid Bosworth, UVM Extension, tapes a report for WCAX TV 3 Across the Fence, Sept. 2015



Figure 36 Fox 22/44 reporter does a broadcast on the project, 10-24-2015



Figure 37 WCAX Channel 3 Across the Fence report being taped, 10-29-2015



#### WHEN

9 a.m.-noon Friday, October 23rd and Saturday, October 24th, 2015. Choose the most convenient day.

#### WHERE

Meach Cove Farms 310 Beach Road, Shelburne, VT (off Bostwick Road. 1.6 miles west of US Route 7)

#### WHY

Vermont-grown grasses are being used to heat a 4,200 square foot commercial building with emissions comparable to wood . This is the first project in New England to showcase grass test plots, densification equipment and a biomass boiler that is burning the grass. Come learn about how it works, the challenges and successes, and the future of alternative energy!

# TO FLUE OPEN HOUSE

**FIELD** 

GRASS PELLET HEATING EQUIPMENT COMBUSTION OPTIMATIZATION PROJECT

#### FOR MORE INFORMATION ONLINE

meachcovefarms.org EMAIL cdavis@meachcovefarms.org PHONE (802) 985-9218

This project was funded through a Conservation Innovation Grani (CIG), administered by the Natural Resources Conservation Service. CIG's stimulate the development of innovative approaches and technologies for conservation on farms, ranches and forest lands. Funding for CIG conse from the Environmental Quality Incentives Program, part of the 2014 Farm Sill. USDA is an equal opportunity employer and provider.

Figure 38 Field to Flue Open House poster, October 2015



Figure 39 Meach Cove Farms Open House display presentation, 10-23-2015

# Raw Combustion Data

## Field Combustion Measurements March-June 2015

100%	VT Woo	d Pine	Pellet	s								
Run #1	Stack Temp	Blend:	100%	VT Wood				Test date:	3/13/2015			+
Time	۴	02	CO	CO2	EFF	Ex Air	NO	SO2	Smoke Test	Fuel feed	Fan speed	Pa
7:46:00	375	10.60%	187	10.10%	81.00%	102.00%	52	1				
8:05:32	372	10.20%	190	10.40%	81.70%	94.00%	52	0	9			
8:15:59	390	10.40%	294	10.20%	80.90%	98.00%	52	1				
Avg	379	10.40%	224	10.23%	81.20%	98.00%	52	1	9			
Run #2	Stack Temp	Blend:	100%	VT Wood				Test date:	4/2/2015			-
Time	۰F	02	CO	CO2	EFF	Ex Air	NO	SO2	Smoke Test	Fuel feed	Fan speed	Pa
2:04:05	370	11.30%	1123	0.00%	0.00%	0.00%	50	10		.8/1.0/1.2	90/90/20	
3:11:48	404	10.90%	1438	9.80%	79.90%	108.00%	35	27	>9	.1.2	88/90/20M	i 🗌
3:20:27	399	12.00%	962	8.70%	78.60%	133.00%	27	16		1.2	82/10/22A	
Avg	391	11.40%	1174	6.17%	52.83%	80.33%	37	18	>9			
Run #3	Stack Temp	Blend:	100%	VT Wood				Test date:	4/3/2015			-
Time	°F	02	CO	CO2	EFF	Ex Air	NO	SO2	Smoke Test	Fuel feed	Fan speed	Pa
11:20:27	339	12.50%	406	8.20%	80.70%	147.00%	43	3		.8/1.0/1.2	80/10/22A	
11:34:34	379	11.40%	302	9.30%	80.30%	119.00%	42	0	>9	1.2	79/10/22	
11:56:21	384	15.30%	41	5.50%	72.10%	268.00%	7	0		1.2	77/10/22	
Avg	367	13.07%	250	7.67%	77.70%	178.00%	31	1	>9			
Run #4	Stack Temp	Blend:	100%	VT Wood				Test date:	4/10/2015			-
Time	۴F	02	со	CO2	EFF	Ex Air	NO	SO2	Smoke Test	Fuel feed	Fan speed	Pa
10:31:27	370	11.50%	1098	9.20%	80.10%	121.00%	42	14		1.2	79/20/22	15
11:02:46	386	14.70%	119	6.10%	73.20%	233.00%	9	0	>9		84/20/22	16
11:17:34	397	15.90%	58	4.90%	68.10%	312.00%	6	3			83/20/22	16
Avg	384	14.03%	425	6.73%	73.80%	222.00%	19	6	>9			
100% VT Wood												
Avg	380	12.23%	518	7.70%	71.38%	144.58%	35	6	>9			

100%	Energe	k Wood	d Blenc	Pellets								
Run #1	Stack Temp	Blend:	100%	Energex Wo	od Blend			Test date:	3/4/2015			
Time	°F	02	CO	CO2	EFF	Ex Air	NO	SO2	Smoke Test	Fuel feed	Fan speed	Pa
3:44:23	341	9.70%	82	10.90%	83.70%	86.00%	72	1				
3:58:53	339	9.50%	66	11.10%	84.40%	83.00%	69	0	7			
4:17:54	329	15.70%	659	5.10%	75.80%	296.00%	33	4				
Avg	336	11.63%	269	9.03%	81.30%	155.00%	58	2	7			
Run #2	Stack Temp	Blend:	100%	Energex Wo	od Blend			Test date:	4/10/2015			-
Time	°F	02	CO	CO2	EFF	Ex Air	NO	SO2	Smoke Test	Fuel feed	Fan speed	Ра
2:40:15	352	14.80%	243	6.00%	75.60%	239.00%	48	2		1.2	76/20/22	14
3:01:29	381	9.40%	245	11.20%	82.20%	81.00%	65	1	9	1.2	76/20/22	14
3:20:37	395	9.40%	351	11.20%	81.70%	81.00%	64	4		1.2	76/18/23	15
Avg	376	11.20%	280	9.47%	79.83%	133.67%	59	2	9			
100%												
Energex												
Wood												
Blend Avg	356	11.42%	274	9.25%	80.57%	144.33%	59	2	8			

<b>6</b>				Hay Pe								+
Run #1 Time	Stack Temp °F	Blend: O2		Hay (Enviro ) CO2	Energy) EFF	Ex Air	NØ	*************	3/10/2015	Fuelfeed	HELISEES	
	******		CO			**********		SO2	Smoke	Fuelfeed	Fan speed	Pa
7:49:33		15.60%	2857	5.20%	73.30%	289.00%	107	14	-			+
8:08:59		14.40%	39	6.40%	76.20%	218.00%	120	27	8			+
8:25:57	363	14.60%	2688	6.20%	87.20%	228.00%	128	19				_
Avg	353	14.87%	1861	5.93%	78.90%	245.00%	118.3333	20	8			
Run #2	Stack Temp	Blend:	100%	Hay (Enviro I	Energy)			Test date:	3/23/2015			
Time	٩F	<b>O</b> 2	CO	CO2	EFF	Ex Air	NO	SO2	Smoke	Fuel feed	Fan speed	Pa
1:30:16	208	18.90%	1669	2.00%	69.20%	900.00%	44	26		.4/.5/.8	85/25/22	
1:51:23	212	19.20%	1475	1.70%	64.50%	999.00%	39	139	>9	.4/.6/.8	70/60/40	+
2:06:25	213	19.40%	1387	1.50%	60.50%	999.00%	40	99			78/60/28	+
Avg	211	19.17%	1510	1.73%	64.73%	966.00%	41	88	>9			-
Run #3	Stack Temp	Blend :	100%	Mulch Hay				Test date:	3/27/2015			
Time	۴	02	CO	CO2	EFF	Ex Air	NO	SO2	Smoke	Fuel feed	Fan speed	Pa
1:41:32	366	10.60%	3562	10.10%	81.80%	102.00%	138	66		.8/1.0/1.5	84/70/19	
1:58:13	363	11.30%	0	9.40%	81.40%	116.00%	122	231	5	1.5	88/70/19	
2:19:02	341	15.20%	0	5.60%	75.80%	262.00%	106	20		1.5	88/70/19	
Avg	357	12.37%	1187	8.37%	79.67%	160.00%	122	106	5			
Run #4	Stack Temp	otaal	100%	Mulch Hay				Test date:	3/30/2015			
Run #4 Time	Stack temp °F	O2	100% CO	CO2	EFF	Ex Air	NO	SO2	Smoke	Fuel feed	Fan speed	
11:20:09	375	11.00%	2000	9.70%	88.80%	110.00%	159	66	amore	.6/.8/1.2	85/83/19	_ rd
					1		159	95	7	.0/.0/1.2		+
11:34:46		12.30%	2000	8.40%	88.60%	141.00%			1		86/83/19	+
11:48:06	375 372	11.30% 11.53%	2000	9.40% 9.17%	88.70% 88.70%	116.00% 122.33%	148 153.3333	68 76	7		86/83/19	
Avg	572	11.35%	2000	9.17%	00.7070	122.55%	100.0000	70	/			
Run #5	Stack Temp	Blend:	100%	Mulch Hay				Test date:	3/30/2015			
Time	٩¢	02	CO	CO2	EFF	Ex Air	NO	SO2	Smoke	Fuel feed	Fan speed	Pa
2:07:03		10.10%	3000	10.50%	91.00%	93.00%	133	171		.6/.8/1.2	82/80/20	
		11.50%	3000	9.20%	88.30%	121.00%	151	43	9	1.2	87/85/20	+
		12.80%	181	7.90%	87.80%	156.00%	142	28		1.2	90/85/20	+
2:19:33	375	17.80%				100.00/0		20			23,03,20	1
2:19:33 2:34:34					89.03%	123.33%	142	81	9			
2:19:33	375 362	12.80%	2060	9.20%	89.03%	123.33%	142	81	9			

### Field Combustion Measurements March-June 2015- continued

Run #1	Stack Temp	Blend:	100%	Switchgrass				Test date:	3/6/2015			
Time	°F	02	CO	CO2	EFF	Ex Air	NO	SO2	Smoke	Fuel feed	Fan speed	0
									SHOKE	rueneeu	rail specu	1.0
3:16:18	325	13.20%	202	7.50%	79.80%	169.00%	158	0				
3:29:02	347	12.10%	238	8.60%	80.20%	136.00%	151	0				
4:07:05	273	17.70%	220	3.20%	70.10%	536.00%	63	2				
Avg	315	14.33%	220	6.43%	76.70%	280.33%	124	1				
									- / /			
Run #2	Stack Temp	***********		Switchgrass					3/13/2015			123
lime	°F	02	CO	CO2	EFF	Ex Air	NÒ	SO2	Smoke	Fuel feed	Fan speed	P
11:51:26	257	18.40%	387	2.50%	66.10%	708.00%	62	3		.4/.6/.8	80/20/35	
12:09:28	242	18.60%	200	2.30%	66.20%	775.00%	47	0			75/30/40	
12:29:28	221	18.50%	170	2.40%	70.80%	740.00%	61	1	7		85/30/40	
12:49:23	246	18.70%	106	2.20%	64.80%	813.00%	63	0			85/30/40	
1:04:54	231	19.40%	134	1.50%	55.50%	999.00%	40	0				
Avg	239	18.72%	199	2.18%	64.68%	807.00%	57	1	7			
tun #3	Stack Temp	Blend:	100%	Switchgrass				Test date:	3/24/2015			
lime	٩F	02	CO	CO2	EFF	Ex Air	NO	SO2	Smoke	Fuel feed	Fan speed	P
11:56:33	271	17.50%	553	3.40%	71.40%	500.00%	75	0		.4/.6/.9	100/60/28	
12:18:13	240	18.40%	386	2.50%	68.80%	708.00%	60	0		.4/.6/1.0	90/50/22	
12:34:09	235	18.50%	647	2.40%	68.40%	740.00%	60	0	7	.4/.6/1.0	90/50/22	
2:15:34	334	10.30%	147	10.30%	83.00%	96.00%	182	0	,	.4/.6/.8	80/0/30	$\vdash$
4vg	270	16.18%	433	4.65%	72.90%	511.00%	94	0	7		30/0/30	⊢
148	270	10.1070	433	4.0370	72.5070	511.00%	54	U	,			
tun #4	Stack Temp	Plands	1009/	Switchgrass				Tast datas	3/25/2015			
<u></u>					eee	<b>F</b> -2 A 1-2	810			Fuel feed	Polo do citar	
îme	°F	02	co	CO2	EFF	Ex Air	NO	<b>SO2</b>	Smoke		Fan speed	Pi
1:19:43	206	19.10%	252	1.80%	65.30%	999.00%	59	0		.4/.5/1.6	75/25/25	
1:32:20	239	18.60%	408	2.30%	67.10%	775.00%	73	0	7	.4/.5/1.6	74/40/20	
1:50:59	237	18.80%	406	2.10%	65.70%	855.00%	66	0		.4/.5/2.0	74/75/20	L
Avg	227	18.83%	355	2.07%	66.03%	876.33%	66	0	7			
Run #5	Stack Temp	Blend:	100%	Switchgrass				Test date:	4/1/2015			
lime.	۴	02	СО	CO2	EFF	Ex Air	NÖ	<b>SO2</b>	Smoke	Fuel feed	Fan speed	Pa
12:12:33	348	14.40%	435	6.40%	88.20%	218.00%	112	0		.8/1.0/1.2	90/90/20	
12:28:22	348	14.10%	924	6.70%	88.50%	204.00%	118	8	9	1.5	92/90/20	
12:47:58	336	15.10%	432	5.70%	88.50%	256.00%	124	0		1.2	88/90/20	
Avg	344	14.53%	597	6.27%	88.40%	226.00%	118	3	9			
Run #6	Stack Temp	Blend:	100%	Switchgrass				Test date:	4/1/2015			
Time	°F	02	со	CO2	EFF	Ex Air	NO	<b>SO2</b>	Smoke	Fuel feed	Fan speed	Pi
3:07:50	375	10.30%	2400	0.00%	0.00%	0.00%	130	7		.8/1.2/1.2	92/90/20	
3:26:31	354	14.50%	507	0.00%	0.00%	0.00%	101	0	>9	1.3	92/90/20	
3:44:24	354	14.90%	525	0.00%	0.00%	0.00%	101	0	75	1.3	90/90/20	
Avg	360	13.23%	1144	0.00%	0.00%	0.00%	115	2	>9	1.5	50/ 50/ 20	<u> </u>
100	500	13.2370	1144	0.0070	0.0070	0.0070	115	-				
Run #7	Stack Temp	Blend:	100%	Switchgrass				Test date:	4/2/2015			
lime	°F	02	co	CO2	EFF	Ex Air	NO	502	Smoke	Fuel feed	Fan speed	p-
8:36:24	368	12.00%	920	0.00%	0.00%	0.00%	79	3	SHORE	.8/1.2/1.3		<u> </u>
8:54:22	308	12.00%	342	0.00%	0.00%	0.00%	65	0	8	1.3	91/90/20	$\vdash$
									0		90/90/20 88/90/20	-
9:15:53	329	16.30%	388	0.00%	0.00%	0.00%	95	0	8	1.3	00/90/20	-
Avg	348	14.23%	550	0.00%	0.00%	0.00%	80	1	0			
<b>≀un #8</b>	Ctack T	Plored	1000	Curitoko				Tort date	A [C 1304-			
	Stack Temp		*****	Switchgrass				Test date:				-
lime	°F	02	co	CO2	EFF	Ex Air	NO	\$O2	Smoke	Fuel feed	Fan speed	
	327	20.20%	37	70.00%	0.00%	0.00%	15	0		.6/1.0/1.2	10/73m/22	-
12:13:01	343	14.90%	724	5.90%	75.50%	244.00%	88	0	none taken	.6/1.0/1.2	90/80m/22	
12:23:30		15.90%	355	4.90%	74.30%	312.00%	65	0		1.5	76/88m/10	n
12:23:30 12:38:05	320			20 020/	49.93%	185.33%	56	0				
12:23:30 12:38:05	320 330	17.00%	372	26.93%								
12:23:30 12:38:05 Avg	330											
12:23:30				20.93% Switchgrass				Test date:	4/13/2015			
12:23:30 12:38:05 Avg Run #9	330				EFF	Ex Air	NO	Test date: SO2	4/13/2015 Smoke	Fuel feed	Fan speed	Pi
12:23:30 12:38:05 Avg Run #9	330 Stack Temp	Blend:	100%	Switchgrass		<b>Ex Air</b> 156.00%	NO 117			Fuel feed .8/1.0/1.4	Fan speed 76/50/22	
12:23:30 12:38:05 Avg Run #9	330 Stack Temp °F	Blend: O2	100% CO	Switchgrass CO2	EFF			<b>SO</b> 2				1
12:23:30 12:38:05 Avg Run #9 12:50:03 1:09:17	330 Stack Temp *F 341 330	Blend: 02 12.80% 14.90%	100% CO 592 259	Switchgrass CO2 7.90% 5.90%	<b>EFF</b> 80.10% 76.70%	156.00% 244.00%	117 107	<b>SO2</b>	Smoke	.8/1.0/1.4 1.4	76/50/22 77/50/22	12
12:23:30 12:38:05 Avg Run #9 12:50:03 1:09:17 1:27:33	330 Stack Temp °F 341 330 329	Blend: 02 12.80% 14.90% 15.00%	100% CO 592 259 384	Switchgrass CO2 7.90% 5.90% 5.80%	<b>EFF</b> 80.10% 76.70% 76.70%	156.00% 244.00% 250.00%	117 107 113	<b>502</b> 2 0 0	Smoke	.8/1.0/1.4	76/50/22	12
12:23:30 12:38:05 Avg Run #9 12:50:03 1:09:17	330 Stack Temp *F 341 330	Blend: 02 12.80% 14.90%	100% CO 592 259	Switchgrass CO2 7.90% 5.90%	<b>EFF</b> 80.10% 76.70%	156.00% 244.00%	117 107	<b>\$O2</b> 2 0	Smoke	.8/1.0/1.4 1.4	76/50/22 77/50/22	P: 12 19

## Field Combustion Measurements March-June 2015- continued

6% - 2	4% Swi	tch Gra	ss Pel	lets								
Run #1	Stack Temp	Blend:	6%	Switchgrass (	<b>S</b> 5)			Test date:	3/5/2015			
Time	۴	02	CO	CO2	EFF	Ex Air	NO	<b>SO2</b>	Smoke Test	Fuel feed	Fan speed	Pa
2:40:14	375	9.10%	108	11.50%	82.40%	76.00%	76	3				
2:51:20	379	9.60%	78	11.00%	81.80%	84.00%	72	0				
3:02:14	372	9.90%	101	10.70%	81.80%	89.00%	70	0				$\square$
Avg	375	9.53%	96	11.07%	82.00%	83.00%	73	1				
Run #1	Stack Temp	Blend:	12%	Switchgrass (	<b>S4)</b>			Test date:	3/6/2015			
Time	٩F	<b>O</b> 2	CO	CO2	EFF	Ex Air	NO	SO2	Smoke	Fuel feed	Fan speed	Pa
8:35:35	365	9.30%	190	11.30%	82.40%	79.00%	82	1				
8:42:45	381	8.90%	93	11.70%	82.20%	74.00%	82	0				
8:59:12	390	9.60%	87	11.00%	81.40%	84.00%	79	7				
Avg	379	9.27%	123	11.33%	82.00%	79.00%	81	3				
Run #1	Stack Temp	Blends	24%	Switchgrass				Test date:	3/6/2015			
Time	٩F	02	CO	CO2	EFF	Ex Air	NO	SO2	Smoke Test	Fuel feed	Fan speed	Pa
11:26:37	354	9.90%	131	10.70%	82.60%	89.00%	93	0				
11:32:44	356	9.50%	127	11.10%	82.90%	83.00%	94	1				
11:47:53	370	10.00%	92	10.60%	81.80%	91.00%	94	1				
Avg	360	9.80%	117	10.80%	82.43%	87.67%	94	1				

### Field Combustion Measurements March-June 2015- continued

	Stack Temp	Blend:		Switchgrass	oucks(10-1	2% moistu	re)	Test date:	4/7/2015			
Time	°F	02	со	CO2	EFF	Ex Air	NO	502	Smoke Test	Fuel feed	Fan speed	P
1:38:24	375	13.70%	459	7.00%	76.30%	188.00%	103	0			97/50/22	
1:54:21	374	13.80%	627	6.90%	76.40%	192.00%	103	0	9		96/45/22	
2:14:30	370	11.00%	465	9.70%	80.90%	110.00%	138	0			84/42/22	
2:18:06	383	11.00%	419	9.70%	80.30%	110.00%	135	0			88/44/22	1
Avg	376	12.38%	493	8.33%	78.48%	150.00%	115	0	9			
Run #2	Stack Temp	Blend:		Switchgrass	oucks(10-1	2% moistu	re)	Test date:	4/8/2015			+
Time	۴	02	CO	CO2	EFF	Ex Air	NO	SO2	Smoke Test	Fuel feed	Fan speed	P
11:48:06	386	11.70%	336	9.00%	79.20%	126.00%	105	0		1.5/3.0/5.0	87/44/22	1
12:03:14	383	12.70%	447	8.00%	77.90%	153.00%	109	0	8	5.0/3.5sec	87/45/22	1
12:17:36	383	12.10%	420	8.60%	78.90%	136.00%	107	0		5.0/5sec	87/45/22	1
Avg	384	12.17%	401	8.53%	78.67%	138.33%	107	0	8		- , -,	
Run #2	Stack Temp	Blend:		Switchgrass	oucks(10-1	2% moistu	re)	Test date:	4/8/2015			+
Time	°F	O2	со	CO2	EFF	Ex Air	NO		Smoke Test	Fuel feed	Fan speed	P
2:40:27	384	11.70%	520	9.00%	79.20%	126.00%	109	0		5.0/5sec	88/44/22	
3:12:58	383	14.60%	480	6.20%	73.60%	228.00%	71	0	7	,	93/50/22	1
3:36:32	393	13.70%	531	7.00%	75.40%	188.00%	88	1			92/50/22	1
Avg	387	13.33%	510	7.40%	76.07%	180.67%	89	0	7		52,00,22	
	· · · · · · · · · · · · · · · · · · ·	Blend:				2% moistu			4/14/2015			1.2
Time 9:51:47 10:28:46	<b>°F</b> 339 338	<b>02</b> 14.60% 15.10%	<b>CO</b> 491 511	<b>CO2</b> 6.20% 5.70%	EFF 76.80% 75.70%	Ex Air 228.00% 256.00%	NO 86 78			Fuel feed 1.5/3.0/5.0	Fan speed 82/50/22 83/50/22	
9:51:47	339 338	<b>02</b> 14.60%	491	<b>CO2</b> 6.20%	EFF 76.80%	Ex Air 228.00%	<b>NO</b> 86	<b>SO2</b> 0	Smoke Test 7		82/50/22 83/50/22	
9:51:47 10:28:46 10:50:16	339 338	<b>02</b> 14.60% 15.10%	491 511	<b>CO2</b> 6.20% 5.70%	EFF 76.80% 75.70%	Ex Air 228.00% 256.00%	NO 86 78	<b>SO2</b> 0 2	Smoke Test 7	1.5/3.0/5.0	82/50/22 83/50/22	:
9:51:47 10:28:46 10:50:16 Avg	339 338 347	02 14.60% 15.10% 13.80% 14.50%	491 511 520	CO2 6.20% 5.70% 6.90%	EFF 76.80% 75.70% 78.30% 76.93%	Ex:Air 228.00% 256.00% 192.00% 225.33%	NO 86 78 88 88 84	SO2           0           2           1           1	Smoke Test 7	1.5/3.0/5.0	82/50/22 83/50/22	:
9:51:47 10:28:46	339 338 347 341	02 14.60% 15.10% 13.80% 14.50%	491 511 520	CO2 6.20% 5.70% 6.90% 6.27%	EFF 76.80% 75.70% 78.30% 76.93%	Ex:Air 228.00% 256.00% 192.00% 225.33%	NO 86 78 88 88 84	SO2           0           2           1           1	Smoke Test 7 7 6/3/2015	1.5/3.0/5.0	82/50/22 83/50/22	1
9:51:47 10:28:46 10:50:16 Avg Run #4	339 338 347 341 Stack Temp	02 14.60% 15.10% 13.80% 14.50% Blend:	491 511 520 507	CO2 6.20% 5.70% 6.90% 6.27% Switchgrass	EFF 76.80% 75.70% 78.30% 76.93% pucks(+-18	Ex Air 228.00% 256.00% 192.00% 225.33% % moisture	86 78 88 88 84	502 0 2 1 1 Test date:	Smoke Test 7 7 6/3/2015	1.5/3.0/5.0	82/50/22 83/50/22 83/50/22	1
9:51:47 10:28:46 10:50:16 Avg Run #4	339 338 347 341 Stack Temp	02 14.60% 15.10% 13.80% 14.50% Blend 02	491 511 520 507 <b>CO</b>	6.20% 5.70% 6.90% 6.27% Switchgrass CO2	EFF 76.80% 75.70% 78.30% 76.93% pucks(+-18 EFF	Ex Air 228.00% 256.00% 192.00% 225.33% % moisture Ex Air	NO 86 78 88 88 84 9 NO	SO2           0           2           1           1           Test date:           SO2	Smoke Test 7 7 6/3/2015	1.5/3.0/5.0	82/50/22 83/50/22 83/50/22	1
9:51:47 10:28:46 10:50:16 Avg Run #4 Time 11:24:25 11:42:34	339 338 347 341 Stack Temp ?F 345 374	02 14.60% 15.10% 13.80% 14.50% Blend 12.60% 12.90%	491 511 520 507 <b>CO</b> 603	CO2           6.20%           5.70%           6.90%           6.27%           Switchgrass           CO2           8.10%           7.80%	EFF 76.80% 75.70% 78.30% 76.93% pucks(+:18 EFF 80.10% 78.30%	Ex Air 228.00% 256.00% 192.00% 225.33% % moisture Ex Air 150.00% 159.00%	NO 86 78 88 84 84 84 84 84 84 84 84 84 84 84 84	0 2 1 Test date: 502 3	Smoke Test 7 7 6/3/2015 Smoke Test	1.5/3.0/5.0	82/50/22 83/50/22 83/50/22	1
9:51:47 10:28:46 10:50:16 Avg Run #4 Time 11:24:25	339 338 347 341 Stack Temp °F 345	02 14.60% 15.10% 13.80% 14.50% Blend 12.60%	491 511 520 507 <b>CO</b> 603 366	CO2           6.20%           5.70%           6.90%           6.27%           Switchgrass           CO2           8.10%	EFF 76.80% 75.70% 78.30% 76.93% 76.93% pucks(+-18 EFF 80.10%	Ex Air 228.00% 256.00% 192.00% 225.33% % moisture Ex Air 150.00%	NO           86           78           88           84           NO           110           105	0 2 1 1 Test date: \$02 3 0	Smoke Test 7 7 6/3/2015 Smoke Test	1.5/3.0/5.0	82/50/22 83/50/22 83/50/22	1
9:51:47 10:28:46 10:50:16 Avg Run:#4 Time 11:24:25 11:42:34 11:52:56 AVG	339 338 347 341 Stack Temp ?F 345 374 365	02 14.60% 15.10% 13.80% 14.50% <b>Blend</b> 12.60% 12.90% 14.50% 13.33%	491 511 520 507 <b>CO</b> 603 366 292	CO2           6.20%           5.70%           6.90%           6.27%           Switchgrass           CO2           8.10%           7.80%           6.30%	EFF 76.80% 75.70% 78.30% 76.93% 9ucks(+-12 EFF 80.10% 78.30% 75.40% 77.93%	Ex Air 228.00% 256.00% 192.00% 225.33% % moisture Ex Air 150.00% 159.00% 223.00% 177.33%	NO 86 78 88 84 NO 110 105 79 98	SO2           0           2           1           Test date:           SO2           3           0           1	Smoke Test 7 6/3/2015 Smoke Test 7 7	1.5/3.0/5.0	82/50/22 83/50/22 83/50/22	
9:51:47 10:28:46 10:50:16 Avg Run:#4 Time 11:24:25 11:42:34 11:52:56 AVG Run:#5	339 338 347 341 Stack Temp F 345 374 365 361	02 14.60% 15.10% 13.80% 14.50% <b>Blend</b> 12.60% 12.90% 14.50% 13.33%	491 511 520 507 <b>CO</b> 603 366 292	CO2           6.20%           5.70%           6.90%           6.27%           Switchgrass           CO2           8.10%           7.80%           6.30%           7.40%	EFF 76.80% 75.70% 78.30% 76.93% 9ucks(+-12 EFF 80.10% 78.30% 75.40% 77.93%	Ex Air 228.00% 256.00% 192.00% 225.33% % moisture Ex Air 150.00% 159.00% 223.00% 177.33%	NO 86 78 88 84 NO 110 105 79 98	SO2         0           2         1           1         1           Test date:         SO2           3         0           1         1           Test date:         SO2	Smoke Test 7 6/3/2015 Smoke Test 7 7	1.5/3.0/5.0 1.5/3.0/5.0 Fuel feed	82/50/22 83/50/22 83/50/22	
9:51:47 10:28:46 10:50:16 Avg Run:#4 Time 11:24:25 11:42:34 11:52:56 AVG Run:#5	339 338 347 341 Stack Temp F 345 374 365 361 Stack Temp	02 14.60% 15.10% 13.80% 14.50% Blend 12.60% 12.90% 14.50% 13.33% Blend	491 511 520 507 <b>CO</b> 603 366 292 420	CO2           6.20%           5.70%           6.90%           6.27%           Switchgrass           CO2           8.10%           7.80%           6.30%           7.40%           Switchgrass	EFF 76.80% 75.70% 78.30% 76.93% 9ucks(+-18 80.10% 78.30% 75.40% 77.93% 9ucks(+-18	Ex Air 228.00% 256.00% 192.00% 225.33% % moisture Ex Air 150.00% 159.00% 223.00% 177.33% % moisture	NO 86 78 88 84 NO 110 105 79 98	SO2         0           2         1           1         1           Test date:         SO2           3         0           1         1           Test date:         SO2	Smoke Test 7 6/3/2015 Smoke Test 7 7 6/3/2015	1.5/3.0/5.0 1.5/3.0/5.0 Fuel feed	82/50/22 83/50/22 83/50/22 Fan speed	
9:51:47 10:28:46 10:50:16 Avg Run:#4 11:24:25 11:42:34 11:52:56 AVG Run:#5 Time 1:21:29	339 338 347 341 Stack Temp 7 345 374 365 361 Stack Temp 327	02 14.60% 15.10% 13.80% 14.50% 12.60% 12.60% 12.90% 14.50% 13.33% Blend 13.33%	491 511 520 507 <b>CO</b> 603 366 292 420 <b>CO</b>	CO2           6.20%           5.70%           6.90%           6.27%           Switchgrass           CO2           8.10%           7.80%           6.30%           7.40%           Switchgrass           CO2           5.00%	EFF 76.80% 75.70% 78.30% 76.93% 500cks(+-18 80.10% 78.30% 75.40% 77.93% 500cks(+-18 EFF 74.30%	Ex Air 228.00% 256.00% 192.00% 225.33% % moisture Ex Air 150.00% 159.00% 223.00% 177.33% % moisture Ex Air 304.00%	NO 86 78 88 84 10 110 105 79 98 98	SO2           0           2           1           1           Test date:           SO2           3           0           1           1           Test date:           SO2           3           0           1           SO2	Smoke Test 7 6/3/2015 Smoke Test 7 6/3/2015 Smoke Test	1.5/3.0/5.0 1.5/3.0/5.0 Fuel feed	82/50/22 83/50/22 83/50/22 Fan speed Fan speed 100/38/40	
9:51:47 10:28:46 10:50:16 Avg Run #4 11:24:25 11:42:34 11:52:56 AVG Run #5 Time 1:21:29 1:32:24	339 338 347 341 Stack Temp °F 345 365 361 Stack Temp °F 327 323	02         14.60%         15.10%         13.80%         14.50%         Blend         12.60%         12.90%         14.50%         13.33%         Blend         02         15.80%         16.90%	491 511 520 507 <b>CO</b> 603 366 292 420 <b>CO</b> 191 140	CO2           6.20%           5.70%           6.90%           6.27%           Switchgrass           CO2           8.10%           7.80%           6.30%           7.40%           Switchgrass           CO2           5.00%           3.90%	EFF 76.80% 75.70% 78.30% 76.93% 900cks(+-18 80.10% 78.30% 75.40% 77.93% 900cks(+-18 EFF 74.30% 70.10%	Ex Air 228.00% 256.00% 192.00% 225.33% <b>% moisture</b> Ex Air 150.00% 159.00% 223.00% 177.33% <b>% moisture</b> Ex Air 304.00% 412.00%	NO           86           78           88           84           NO           110           105           79           98           NO           73           56	SO2           0           2           1           1           Test date:           SO2           3           0           1           Test date:           SO2           3           0           1           0           1           0           1           0           1           0           1           0           1           0           1           0           1	Smoke Test 7 6/3/2015 Smoke Test 7 7 6/3/2015	1.5/3.0/5.0 1.5/3.0/5.0 Fuel feed	82/50/22 83/50/22 83/50/22 Fan speed Fan speed 100/38/40 100/38/40	
9:51:47 10:28:46 10:50:16 Avg Run #4 11:24:25 11:42:34 11:52:56 AVG Run #5 Time 1:21:29 1:32:24 1:45:37	339 338 347 341 Stack Temp 345 374 365 361 Stack Temp ?F 327 323 323	02         14.60%         15.10%         13.80%         14.50%         Blend         12.60%         12.90%         14.50%         13.33%         Blend         13.33%         Blend         15.80%         16.90%         15.90%	491 511 520 507 <b>CO</b> 603 366 292 420 <b>CO</b> 191 140 214	CO2           6.20%           5.70%           6.90%           6.27%           Switchgrass           CO2           8.10%           7.80%           6.30%           7.40%           Switchgrass           CO2           5.00%           3.90%           4.90%	EFF 76.80% 75.70% 78.30% 76.93% 900Cks(+-18 80.10% 75.40% 77.93% 900Cks(+-18 EFF 74.30% 70.10% 74.40%	Ex Air 228.00% 256.00% 192.00% 225.33% <b>% moisture</b> Ex Air 150.00% 159.00% 223.00% 177.33% <b>% moisture</b> Ex Air 304.00% 412.00%	NO           86           78           88           84           110           105           79           98           NO           73           56           76	SO2           0           2           1           1           Test date:           SO2           3           0           1           Test date:           SO2           0           1           0           1           0           1           0           1           0           1           0           1           0	Smoke Test 7 6/3/2015 Smoke Test 7 7 6/3/2015 Smoke Test 5.5	1.5/3.0/5.0 1.5/3.0/5.0 Fuel feed	82/50/22 83/50/22 83/50/22 Fan speed Fan speed 100/38/40	
9:51:47 10:28:46 10:50:16 Avg Run:#4 11:24:25 11:42:34 11:52:56 AVG Run:#5 Time 1:21:29 1:32:24	339 338 347 341 Stack Temp °F 345 365 361 Stack Temp °F 327 323	02 14.60% 15.10% 13.80% 14.50% 12.60% 12.60% 12.90% 14.50% 13.33% Blend 02 15.80% 16.90%	491 511 520 507 <b>CO</b> 603 366 292 420 <b>CO</b> 191 140	CO2           6.20%           5.70%           6.90%           6.27%           Switchgrass           CO2           8.10%           7.80%           6.30%           7.40%           Switchgrass           CO2           5.00%           3.90%	EFF 76.80% 75.70% 78.30% 76.93% 900cks(+-18 80.10% 78.30% 75.40% 77.93% 900cks(+-18 EFF 74.30% 70.10%	Ex Air 228.00% 256.00% 192.00% 225.33% <b>% moisture</b> Ex Air 150.00% 159.00% 223.00% 177.33% <b>% moisture</b> Ex Air 304.00% 412.00%	NO           86           78           88           84           NO           110           105           79           98           NO           73           56	SO2           0           2           1           1           Test date:           SO2           3           0           1           Test date:           SO2           3           0           1           0           1           0           1           0           1           0           1           0           1           0           1           0           1	Smoke Test 7 6/3/2015 Smoke Test 7 6/3/2015 Smoke Test	1.5/3.0/5.0 1.5/3.0/5.0 Fuel feed	82/50/22 83/50/22 83/50/22 Fan speed Fan speed 100/38/40 100/38/40	

Run #1	Stack Temp	Blend:	100%	<b>Reed Canary</b>	Grass (MC	F)		Test date:	3/11/2015			
Time	۴	02	CO	CO2	EFF	Ex Air	NO	SO2	Smoke	Fuel feed	Fan speed	Pa
1:35:10	307	16.70%	144	4.10%	71.90%	388.00%	73	0		.4/.6/.8	77/20/22	
1:47:52	294	17.20%	100	3.60%	70.50%	453.00%	68	0	7	.4/.6/.6	77/30/22	
2:18:35	285	17.80%	142	3.10%	67.90%	556.00%	56	0		.4/.6/.8	85/40/22	T
Avg	295	17.23%	129	3.60%	70.10%	465.67%	66	0	7			_
Run #2	Stack Temp	Blend:	100%	Reed Canary	Grass (MC	F)		Test date:	3/26/2015			-
Time	۴F	02	со	CO2	EFF	Ex Air	NO	SO2	Smoke	Fuel feed	Fan speed	Pa
9:31:12	339	12.00%	481	8.70%	80.80%	133.00%	120	0		.8/1.0/1.2	76/76/16	
9:47:54	354	11.80%	824	8.90%	80.50%	128.00%	119	1	>9	.8/1.0/1.5	81/76/18	1
10:16:54	323	13.10%	373	7.60%	80.20%	166.00%	117	6	-	.6/1.0/1.5	78/76/16	1
Avg	339	12.30%	559	8.40%	80.50%	142.33%	119	2	>9			
Run #3	Stack Temp	Blend:	100%	Reed Canary	Grass (MC	FI		Test date:	3/27/2015			-
Time	°F	02	CO	CO2	EFF	Ex Air	NO	SO2	Smoke	Fuel feed	Fan speed	Pa
8:05:31	361	9.10%	1440	11.50%	83.00%	76.00%	130	10		.6/1.0/1.5	79/76/16	10.00
8:16:11	354	12.00%	387	8.70%	80.60%	133.00%	120	3	>9	.6/.8/1.5	79/76/16	+
8:31:21	350	13.50%	181	7.20%	78.60%	180.00%	104	4		.6/.8/1.5	83/76/16	1
Avg	355	11.53%	669	9.13%	80.73%	129.67%	118	6	>9			
Run #4	Stack Temp	Blend:	100%	Reed Canary	Grass (MC	F)		Test date:	3/31/2015			-
Time	۰F	02	СО	CO2	EFF	Ex Air	NO	SO2	Smoke	Fuel feed	Fan speed	Pa
8:34:20	366	7.30%	3999	13.30%	90.30%	53.00%	124	48		.6/.8/1.2	76/88/20	1
8:51:54	379	9.50%	3000	11.10%	89.30%	83.00%	135	0	9	1.2	75/88/20	1
9:11:05	370	11.20%	285	9.50%	89.00%	114.00%	128	0		1.2	74/88/20	1
Avg	372	9.33%	2428	11.30%	89.53%	83.33%	129	16	9			
Run #5	Stack Temp	Blend:	100%	Reed Canary	Grass (MC	F)		Test date:	3/31/2015			-
Time	°F	02	CO	CO2	EFF	Ex Air	NO	SO2	Smoke	Fuel feed	Fan speed	Pa
12:13:37	383	12.50%	3000	8.20%	87.70%	147.00%	94	0		.6/.8/1.2	80/88/20	
12:28:27	375	12.90%	255	7.80%	87.80%	159.00%	121	0	>9	1.2	90/88/20	
12:43:13	375	13.10%	417	7.60%	87.70%	166.00%	117	0		1.2	91/88/20	
Avg	378	12.83%	1224	7.87%	87.73%	157.33%	111	0	>9			_
Run #6	Stack Temp	Blend:	100%	Reed Canary	Grass (MC	F)		Test date:	4/1/2015			-
Time	°F	02	CO	CO2	EFF	Ex Air	NO	SO2	Smoke	Fuel feed	Fan speed	Pa
8:35:12	392	11.40%	303	9.30%	87.90%	119.00%	139	0		.8/1.0/1.2	90/88/20	T
8:50:40	379	13.60%	254	7.10%	0.00%	0.00%	114	1	8	.8/1.0/1.2	90/88/20	1
9:05:10	368	13.90%	466	6.80%	87.50%	196.00%	108	1		1.2	90/88/20	Τ
		42.070/	341	7.73%	58.47%	105.00%	120	1	8			
Avg	380	12.97%	341	1.13/0	30.4770	105.0070	120		0			

				ss Pellet				<del>2002-0000</del>	2/10/2015			-
	Stack Temp	****		Reed Canary	<u>,</u>				3/10/2015			12
Time	°F	02	CO	CO2	EFF	Ex Air	NO		Smoke Test	Fuel feed	Fan speed	P
10:45:28	370	12.50%	276	8.20%	79.40%	147.00%	54	3				_
11:00:29	386	10.40%	186	10.20%	81.40%	98.00%	67	0				
11:12:47	384	11.00%	245	9.70%	80.70%	110.00%	63	4				
Avg	380	11.30%	236	9.37%	80.50%	118.33%	61	2				
Run #1	Stack Temp	Blend:	12%	Reed Canary	Grass (R3)			Test date:	3/11/2015			
Time	°F	02	CO	CO2	EFF	Ex Air	NO	SO2	Smoke	Fuel feed	Fan speed	Ρ
7:18:16	318	13.50%	167	7.20%	80.80%	180.00%	59	1				
7:30:25	356	11.60%	128	9.10%	81.40%	123.00%	72	0				
7:47:48	379	11.10%	124	9.60%	81.00%	112.00%	77	0				
Avg	351	12.07%	140	8.63%	81.07%	138.33%	69	0				
		w						49949999				
	Stack Temp			Reed Canary					3/11/2015		<b>.</b> 	12
Time	°F	02	CO	CO2	EFF	Ex Air	NO	SO2	Smoke Test	Fuel teed	Fan speed	P
11:16:40	347	16.30%	319	4.50%	75.40%	347.00%	50	3				
11:29:06	312	16.60%	251	4.20%	73.00%	377.00%	50	0				_
11:45:21	303	16.60%	193	4.20%	73.90%	377.00%	50	0				
Avg	321	16.50%	254	4.30%	74.10%	367.00%	50	1				-
6-24% Reed												
Canany		1										
Canary Avg	351	0	210	0	1	2	60	1	7.25			
Avg 6% - 2	351 <b>4% Mul</b> Stack Temp	ch Hay	v Pellet		1	2		1 Test date:				
Avg 6% - 2	4% Mul	ch Hay	v Pellet	S		2		-		Fuel feed	Fan speed	P
Avg 6% - 2 Run #1	4% Mul Stack Temp	ch Hay Blend:	v Pellet	S Mulch Hay				Test date:	3/9/2015	Fuel feed	Fan speed	P
Avg 6% - 2 Run #1 Time	4% Mul Stack Temp °F	ch Hay <sup>Blend:</sup> 02	Pellet	S Mulch Hay CO2	EFF	Ex Air	NO	Test date: SO2	3/9/2015	Fuel feed	Fan speed	P
Avg 6% - 2 Run #1 Time 8:56:05	4% Mul Stack Temp °F 392	<b>ch Hay</b> Blend: 02 10.20%	Pellet 6% co 375	S Mulch Hay CO2 10.40%	<b>EFF</b> 80.90%	<b>Ex Air</b> 94.00%	<b>NO</b> 68	Test date: SO2 1	3/9/2015	Fuel feed	Fan speed	P
Avg 6% - 2 Run #1 Time 8:56:05 9:05:24	<b>4% Mul</b> Stack Temp *F 392 395	<b>ch Hay</b> Blend: 02 10.20% 10.10%	Pellet 6% CO 375 169	S Mulch Hay CO2 10.40% 10.50%	<b>EFF</b> 80.90% 81.00%	<b>Ex Air</b> 94.00% 93.00%	<b>NO</b> 68 73	Test date: SO2 1 1	3/9/2015	Fuel feed	Fan speed	P
Avg 6% - 2 Run #1 Time 8:56:05 9:05:24 9:18:06 9:24:18	<b>4% Mul</b> Stack Temp <b>*F</b> 392 395 406	ch Hay Blend: 02 10.20% 10.10% 10.70%	7 Pellet 6% 20 375 169 278	S Mulch Hay CO2 10.40% 10.50% 10.00%	EFF 80.90% 81.00% 80.00%	<b>Ex Air</b> 94.00% 93.00% 104.00%	NO 68 73 71	Test date: SO2 1 2	3/9/2015	Fuel feed	Fan speed	P
Avg 6% - 2 Run #1 Time 8:56:05 9:05:24 9:18:06 9:24:18 Avg	<b>4% Mul</b> Stack Temp 392 395 406 406 400	ch Hay Blend: 02 10.20% 10.10% 10.70% 10.50% 10.38%	Pellet 6% 20 375 169 278 190 253	S Mulch Hay CO2 10.40% 10.50% 10.00% 10.20% 10.28%	EFF 80.90% 81.00% 80.00% 80.40% 80.58%	<b>Ex Air</b> 94.00% 93.00% 104.00% 100.00%	NO 68 73 71 73	Test date SO2 1 1 2 0 1	3/9/2015 Smoke Test	Fuel feed	Fan speed	<b>P</b>
Avg 6% - 2 Run #1 Time 8:56:05 9:05:24 9:18:06 9:24:18 Avg Run #1	<b>4% Mul</b> Stack Temp 392 395 406 406 400 Stack Temp	ch Hay Blend: 02 10.20% 10.10% 10.70% 10.50% 10.38% Blend:	Pellet 6% 20 375 169 278 190 253 122%	S Mulch Hay CO2 10.40% 10.50% 10.00% 10.20% 10.28% Mulch Hay (1	EFF 80.90% 81.00% 80.00% 80.40% 80.58%	Ex Air 94.00% 93.00% 104.00% 100.00% 97.75%	NO 68 73 71 73 71	Test date: SO2 1 1 2 0 1 Test date:	3/9/2015 Smoke Test 3/9/2015			
Avg 6% - 2 Run #1 Time 8:56:05 9:05:24 9:18:06 9:24:18 Avg Run #1 Time	4% Mul Stack Temp 392 395 406 406 400 Stack Temp	ch Hay Blend: 02 10.20% 10.10% 10.70% 10.50% 10.38% Blend: 02	Pellet 6% 2C0 375 169 278 190 253 253 12% C0	S Mulch Hay CO2 10.40% 10.50% 10.00% 10.20% 10.28% Mulch Hay (1 CO2	EFF 80.90% 81.00% 80.00% 80.40% 80.58% W3) EFF	Ex Air 94.00% 93.00% 104.00% 100.00% 97.75% Ex Air	NO 68 73 71 73 71 71 71 NO	Test date: SO2 1 1 2 0 1 Test date: SO2	3/9/2015 Smoke Test	Fuel feed	Fan speed	
Avg 6% - 2 Run #1 Time 8:56:05 9:05:24 9:18:06 9:24:18 Avg Run #1 Time 11:49:52	<b>4% Mul</b> Stack Temp 392 395 406 406 400 Stack Temp <b>*</b> <b>*</b> <b>*</b> <b>*</b> <b>*</b> <b>*</b> <b>*</b> <b>*</b>	ch Hay Blend: 02 10.20% 10.10% 10.70% 10.50% 10.38% Blend: 02 11.30%	Pellet 6% 375 169 278 190 253 12% CO 152	S Mulch Hay CO2 10.40% 10.50% 10.00% 10.20% 10.28% Mulch Hay (I CO2 9.40%	EFF 80.90% 81.00% 80.00% 80.40% 80.58% W3) EFF 81.60%	Ex Air 94.00% 93.00% 104.00% 97.75% Ex Air 116.00%	NO           68           73           71           73           71           90	Test date: 502 1 1 2 0 1 Test date: 502 1	3/9/2015 Smoke Test 3/9/2015			
Avg 6% - 2 Run #1 Time 8:56:05 9:05:24 9:18:06 9:24:18 Avg Run #1 Time 11:49:52 11:58:51	4% Mul           Stack Temp           392           395           406           406           400           Stack Temp           *F           343           370	ch Hay Blend: 02 10.20% 10.10% 10.70% 10.50% 10.38% Blend: 02 11.30% 9.30%	Pellet 6% 2C0 375 169 278 190 253 253 190 253 253 253 253 253 253 253 253 253 253	S Mulch Hay CO2 10.40% 10.50% 10.00% 10.20% 10.28% Mulch Hay ( CO2 9.40% 11.30%	EFF 80.90% 81.00% 80.00% 80.40% 80.58% W3) EFF 81.60% 82.40%	Ex Air 94.00% 93.00% 104.00% 100.00% 97.75% Ex Air 116.00% 79.00%	NO 68 73 71 73 71 71 71 <b>NO</b> 90 106	Test date: 502 1 1 2 0 1 Test date: 5	3/9/2015 Smoke Test 3/9/2015			
Avg 6% - 2 Run #1 8:56:05 9:05:24 9:18:06 9:24:18 Avg Run #1 11:49:52 11:58:51 12:06:56	4% Mul Stack Temp 392 395 406 406 400 Stack Temp 9 343 370 406	ch Hay Blend: 02 10.20% 10.10% 10.50% 10.38% Blend: 02 11.30% 9.30% 8.80%	Pellet 6% 270 375 169 278 190 253 253 190 253 12% CO 152 169 186	S Mulch Hay CO2 10.40% 10.50% 10.00% 10.20% 10.28% Mulch Hay (1 CO2 9.40% 11.30% 11.80%	EFF 80.90% 81.00% 80.00% 80.40% 80.58% W3) EFF 81.60% 82.40% 81.50%	Ex Air 94.00% 93.00% 104.00% 100.00% 97.75% Ex Air 116.00% 79.00% 72.00%	NO 68 73 71 73 71 71 8 00 90 106 109	Test date: 502 1 1 2 0 1 Test date: 5 0	3/9/2015 Smoke Test 3/9/2015			
Avg 6% - 2 Run #1 Time 8:56:05 9:05:24 9:18:06 9:24:18 Avg Run #1 Time 11:49:52 11:58:51 12:06:56	4% Mul           Stack Temp           392           395           406           406           400           Stack Temp           *F           343           370	ch Hay Blend: 02 10.20% 10.10% 10.70% 10.50% 10.38% Blend: 02 11.30% 9.30%	Pellet 6% 2C0 375 169 278 190 253 253 190 253 253 253 253 253 253 253 253 253 253	S Mulch Hay CO2 10.40% 10.50% 10.00% 10.20% 10.28% Mulch Hay ( CO2 9.40% 11.30%	EFF 80.90% 81.00% 80.00% 80.40% 80.58% W3) EFF 81.60% 82.40%	Ex Air 94.00% 93.00% 104.00% 100.00% 97.75% Ex Air 116.00% 79.00%	NO 68 73 71 73 71 71 71 <b>NO</b> 90 106	Test date: 502 1 1 2 0 1 Test date: 5	3/9/2015 Smoke Test 3/9/2015			
Avg 6% - 2 Run #1 Time 8:56:05 9:05:24 9:18:06 9:24:18 Avg Run #1 Time 11:49:52 11:58:51 12:06:56 Avg	4% Mul Stack Temp 392 395 406 406 400 Stack Temp 9 343 370 406	Ch Hay Blend: 02 10.20% 10.10% 10.70% 10.50% 10.38% Blend: 02 11.30% 9.30% 8.80% 9.80%	Pellet 6% 375 169 278 190 253 12% CO 152 169 186 169	S Mulch Hay CO2 10.40% 10.50% 10.00% 10.20% 10.28% Mulch Hay (1 CO2 9.40% 11.30% 11.80%	EFF 80.90% 81.00% 80.00% 80.40% 80.58% W3) EFF 81.60% 82.40% 81.50% 81.83%	Ex Air 94.00% 93.00% 104.00% 100.00% 97.75% Ex Air 116.00% 79.00% 72.00%	NO 68 73 71 73 71 71 8 00 90 106 109	Test date: 502 1 1 2 0 1 Test date: 5 0	3/9/2015 Smoke Test 3/9/2015 Smoke			
Avg 6% - 2 Run #1 Time 8:56:05 9:05:24 9:18:06 9:24:18 Avg Run #1 Time 11:49:52 11:58:51 12:06:56 Avg	4% Mul Stack Temp 392 395 406 406 400 Stack Temp 9 8 343 370 406 373	Ch Hay Blend: 02 10.20% 10.10% 10.70% 10.50% 10.38% Blend: 02 11.30% 9.30% 8.80% 9.80%	Pellet 6% 375 169 278 190 253 12% CO 152 169 186 169	S Mulch Hay CO2 10.40% 10.50% 10.00% 10.20% 10.28% Mulch Hay ( CO2 9.40% 11.30% 11.80% 10.83%	EFF 80.90% 81.00% 80.00% 80.40% 80.58% W3) EFF 81.60% 82.40% 81.50% 81.83%	Ex Air 94.00% 93.00% 104.00% 97.75% Ex Air 116.00% 79.00% 72.00%	NO 68 73 71 73 71 71 8 00 90 106 109	Test date: SO2 1 1 2 0 1 Test date: SO2 1 5 0 2 Test date:	3/9/2015 Smoke Test 3/9/2015 Smoke	Fuelfeed		
Avg 6% - 2 Run #1 Time 8:56:05 9:05:24 9:18:06 9:24:18 Avg Run #1 11:49:52 11:58:51 12:06:56 Avg Run #1	4% Mul Stack Temp 392 395 406 406 400 Stack Temp 9 343 370 406 373 Stack Temp	Ch Hay Blend: 10.20% 10.10% 10.70% 10.50% 10.38% Blend: 9.30% 8.80% 9.80% Blend:	Pellet 6% 20 375 169 278 190 253 12% CO 152 169 186 169 24%	S Mulch Hay CO2 10.40% 10.50% 10.00% 10.20% 10.28% Mulch Hay ( CO2 9.40% 11.30% 11.80% 10.83% Mulch Hay (	EFF 80.90% 81.00% 80.00% 80.40% 80.58% V3) EFF 81.60% 82.40% 81.50% 81.83%	Ex Air 94.00% 93.00% 104.00% 97.75% Ex Air 116.00% 79.00% 72.00% 89.00%	NO           68           73           71           73           71           NO           90           106           109           102	Test date: SO2 1 1 2 0 1 Test date: SO2 1 5 0 2 Test date:	3/9/2015 Smoke Test 3/9/2015 Smoke 3/9/2015	Fuelfeed	Fan speed	P
Avg 6% - 2 Run #1 Time 8:56:05 9:05:24 9:18:06 9:24:18 Avg Run #1 11:49:52 11:58:51 12:06:56 Avg Run #1 Time Run #1 Time	4% Mul Stack Temp *F 392 395 406 406 400 Stack Temp *F Stack Temp *F	Ch Hay Blend: 10.20% 10.10% 10.50% 10.50% 10.38% Blend: 9.30% 8.80% 9.80% Blend: 02	Pellet 6% 375 169 278 190 253 12% CO 152 169 186 169 186 169 24% CO	S Mulch Hay CO2 10.40% 10.50% 10.00% 10.20% 10.28% Mulch Hay ( CO2 9.40% 11.30% 11.80% 10.83% Mulch Hay ( CO2	EFF 80.90% 81.00% 80.00% 80.40% 80.58% EFF 81.60% 82.40% 81.50% 81.83%	Ex Air 94.00% 93.00% 104.00% 100.00% 97.75% Ex Air 116.00% 79.00% 72.00% 89.00%	NO 68 73 71 73 71 71 <b>NO</b> 90 106 109 102 <b>NO</b>	Test date: 502 1 1 2 0 1 Test date: 502 1 5 0 2 Test date: 502	3/9/2015 Smoke Test 3/9/2015 Smoke 3/9/2015	Fuelfeed	Fan speed	
Avg 6% - 2 Run #1 Time 8:56:05 9:05:24 9:18:06 9:24:18 Avg Run #1 11:49:52 11:58:51 12:06:56 Avg Run #1 Time 2:18:48	4% Mul Stack Temp *F 392 395 406 406 400 Stack Temp *F 298	Ch Hay Blend: 10.20% 10.10% 10.50% 10.50% 10.38% Blend: 9.30% 8.80% 9.80% Blend: 02 11.30% 9.30%	Pellet 6% 375 169 278 190 253 12% CO 152 169 186 169 186 169 24% CO 164	S Mulch Hay CO2 10.40% 10.50% 10.00% 10.20% 10.28% Mulch Hay ( CO2 9.40% 11.30% 11.80% 10.83% Mulch Hay ( CO2 4.90%	EFF 80.90% 81.00% 80.00% 80.40% 80.58% W3) EFF 81.60% 82.40% 81.50% 81.83% W2] EFF 76.30%	Ex Air 94.00% 93.00% 104.00% 100.00% 97.75% Ex Air 116.00% 79.00% 72.00% 89.00% Ex Air 312.00%	NO           68           73           71           73           71           NO           90           106           109           102           NO           66	Test date: 502 1 1 2 0 1 Test date: 502 1 5 0 2 Test date: 502 0 2 0 0 0 0 0 0 0 0 0 0 0 0 0	3/9/2015 Smoke Test 3/9/2015 Smoke 3/9/2015	Fuelfeed	Fan speed	P

90

1

7->9

## Field Combustion Measurements March-June 2015-continued

6-24% Mulch Hay

Avg

374

0

217

0

1

100%	Energex	Wood	l Blend	Pellets								
Run #1	Stack Temp	Blend:	100%	Energex Wo	od Blend			Test date:	10/14/2015			
Time	°F	02	CO	CO2	EFF	Ex Air	NO	SO2	Smoke Test	Fuel feed	Fan speed	Pa
1:35:42	307	12.00%	319	8.70%	83.10%	133.00%	59	1	>9	baseline set	tings	
2:15:47	343	9.50%	364	11.10%	83.80%	83.00%	66	0	>9	higher feed	4,6	8
2:28:47	379	8.60%	432	12.00%	83.10%	69.00%	73	0				10;+-1
2:36:19	386	9.20%	450	11.40%	82.50%	78.00%	70	0				
2:38:04	386	9.30%	378	11.30%	82.40%	79.00%	70	2		80/20/25		12;+-1
2:43:10	386	10.10%	268	10.50%	81.60%	93.00%	67	0		80/20/25		14;+-1
Avg	365	9.78%	369	10.83%	82.75%	89.17%	68	1	>9			

### Field Combustion Measurements October - November 2015

100%	Enviro	Energy	Hay p	ellets								
Run #1	Stack Temp	Blend:						Test date	11/30/2015			
Time	°F	02	CO	CO2	EFF	Ex Air	NO	\$02	Smoke Test	Fuel feed	Fan speed	Pa
11:52:00	249	18.30%	1185	2.60%	68.20%	678.00%	54	23			71/90/12	
11:58:38	235	18.80%	813	2.10%	65.10%	855.00%	48	118			69/90/12	
12:06:15	217	19.40%	549	1.50%	58.90%	999.00%	37	139	7		65/90/12	
Avg	234	18.83%	849	2.07%	64.07%	844.00%	46	93	7			

Run #1	Stack Temp	Blend:		Switchgrass	oucks(10-1	2% moistu	re)	Test date:	10/14/2015			
Time	۶F	02	CO	CO2	EFF	Ex Air	NO	<b>\$O2</b>	Smoke Test	Fuel feed	Fan speed	Pa
8:52:17	271	17.90%	251	3.00%	69.30%	577.00%	46	0		Higher/45%	fill level	
9:03:52	300	16.30%	342	4.50%	75.00%	347.00%	75	0		-		
9:13:02	332	14.40%	351	6.40%	78.10%	218.00%	98	0	7	45% feed in	firebox	
9:29:36	357	13.90%	223	6.80%	77.60%	196.00%	102	0				
9:30:10	361	13.30%	230	7.40%	78.60%	173.00%	109	0	7			
9:53:25	345	13.60%	97	7.10%	79.00%	184.00%	99	0	6	underpass 1	5->5Pa;5->1	%Pa
9:58:24	356	12.70%	101	8.00%	79.90%	153.00%	113	0				
Avg	332	0	228	0	1	3	92	0	7			
Run #2	Stack Temp	Blend:		Switchgrass	oucks(17%	moisture)		Test date:	11/19/2015			
Time	۴	02	CO	CO2	EFF	Ex Air	NO	SO2	Smoke Test	Fuel feed	Fan speed	Pa
10:17:43	365	11.40%	388	9.30%	81.00%	119.00%	114	8		17% moistu	re	7.0 pa
10:24:28	368	13.50%	209	7.20%	77.70%	180.00%	99	0	6	70% humidi	ty	2.0 top
10:34:23	370	12.80%	256	7.90%	78.90%	156.00%	108	0				
10:42:41	361	13.70%	240	7.00%	77.90%	188.00%	93	0				
10:50:26	347	14.60%	241	6.20%	76.80%	228.00%	90	0				
Avg	362	13.20%	267	7.52%	78.46%	174.20%	101	2	6			
Run #3	Stack Temp	Blend:		Switchgrass (	ucks(15%	moisture)		Test date:	11/23/2015			
Time	°F	02	CO	CO2	EFF	Ex Air	NO	SO2	Smoke Test	Fuel feed	Fan speed	Pa
10:40:34	357	13.60%	481	7.10%	77.20%	184.00%	98	0		15% moistu	re	jet 5.0 pa
10:46:11	357	13.60%	481	7.10%	77.20%	184.00%	98	0	6	5% humidity	1	tolerance 2.0 top
Avg	357	13.60%	481	7.10%	77.20%	184.00%	98	0	6			
SW grass												
pucks												

50% S	witchgr											
Run #1	Stack Temp											
Time	٩°	02	CO	CO2	EFF	Ex Air	NO	SO2	Smoke Test	<b>Fuel feed</b>	Fan speed	Pa
02:02:19	239	17.10%	271	3.20%	75.20%	536.00%	56	0				
02:07:05	253	17.40%	219	3.40%	75.10%	483.00%	66	0				
02:13:55	253	17.70%	231	3.20%	73.50%	536.00%	57	0				
02:18:34	267	18.00%	195	2.90%	69.70%	600.00%	50	0	8.5	2:27		
Avg	253	17.55%	229	3.18%	73.38%	538.75%	57	0	8.5			

100%	Reed Ca	anary G										
Run #1	Stack Temp	Blend:	100%	Reed Canary	Grass (MC	<b>(F)</b>		Test date:	11/17/2015			
Time	۴F	02	CO	CO2	EFF	Ex Air	NO	SO2	Smoke	Fuel feed	Fan speed	Pa
3:31:51	325	13.70%	207	7.00%	79.10%	188.00%	106	0		8% moisture; 53.6% humidity		
3:39:25	361	13.60%	185	7.10%	77.30%	184.00%	131	0		used 2100%	SW puck se	ttings
3:44:16	354	16.50%	160	4.30%	68.40%	367.00%	83	0	7			
Avg	347	14.60%	184	6.13%	74.93%	246.33%	107	0	7			

### Field Combustion Measurements October - November 2015-continued

# 50% Reed Canary Grass/50% Wood pucks

30/0 1		iui y G									
Run #1	Stack Temp	Blend:						Test date	11/18/2015		
Time	۴	02	CO	CO2	EFF	Ex Air	NO	SO2	Smoke Test	<b>Fuel feed</b>	Fan speed Pa
10:18:49	357	14.30%	272	6.50%	76.30%	213.00%	118	0	0	20% moistu	re;53% humidity
10:22:56	348	13.50%	210	7.20%	78.50%	180.00%	336	0	6		
10:30:01	354	13.90%	144	6.80%	77.50%	196.00%	126	0	0		
10:33:14	345	13.70%	151	7.00%	78.40%	188.00%	135	0	0		
10:37:55	336	14.90%	163	5.90%	76.40%	244.00%	107	0	6		
Avg	348	14.06%	188	6.68%	77.42%	204.20%	164	0	6		

100% Miscanthus pucks												
Run #1	Stack Temp	Blend:						Test date:	11/18/2015			
Time	°F	02	CO	CO2	EFF	Ex Air	NO	SO2	Smoke Test	Fuel feed	Fan speed	Pa
11:56:04	361	13.50%	172	7.20%	78.20%	180.00%	70	0		16% moisture; 53% humidity		
12:01:44	343	14.20%	96	6.60%	77.80%	209.00%	63	0	5			
12:08:53	361	14.20%	82	6.60%	76.70%	209.00%	62	0				
12:15:00	350	14.60%	66	6.20%	76.50%	228.00%	59	0	4			
12:36:24	345	13.70%	54	7.00%	78.90%	188.00%	66	0				
12:42:34	345	13.70%	54	7.00%	78.90%	188.00%	66	0				
Avg	351	13.98%	87	6.77%	77.83%	200.33%	64	0	4.5			

# 50% Miscanthus/50% Wood pucks

30/0 11	nocunt	145/ 50	/0 0000	a pacito								
Run #1	Stack Temp	Blend:						Test date:	11/18/2015			
Time	۴	02	CO	CO2	EFF	Ex Air	NÖ	<b>SO2</b>	Smoke Test	Fuelfeed Fa	in speed	Pa
3:14:49	314	15.80%	128	5.00%	75.40%	304.00%	75	0	6	53% humidity		2
3:35:55	329	16.30%	122	4.50%	72.40%	347.00%	65	0	6			
Avg	322	16.05%	125	4.75%	73.90%	325.50%	70	0	6			

100% MC Mulch Hay pucks												
Run #1 Stack Temp Blend:				11% moistur	e		Test date: 11/24/2015					
Time	۴	02	CO	CO2	EFF	Ex Air	NO	<b>SO2</b>	Smoke Test	Fuel feed	Fan speed	Pa
12:51:47	350	15.80%	288	5.00%	71.90%	304.00%	84	0			97/48/35	12;+-5
12:57:53	379	12.70%	229	8.00%	78.10%	153.00%	131	0			97/48/35	
1:02:48	377	13.20%	195	7.50%	77.30%	169.00%	122	0	5.5			
1:06:10	366	13.90%	194	6.80%	76.50%	196.00%	114	0	5		97/48/35	10-12;+-5
Avg	368	13.90%	227	6.83%	75.95%	205.50%	113	0	5.25			

50% N	/C Mulo	h Hay	& 50%	Wood p	oucks							
Run #1	Stack Temp	Blend:		21% moistur	e			Test date:	11/23/2015			
Time	۴	02	co	CO2	EFF	Ex Air	NO	SO2	Smoke	Fuel feed	Fan speed	Pa
2:58:22	289	16.50%	288	4.30%	74.90%	367.00%	80	0		21% moist.	90/38/38	5;+-2.5
3:07:12	307	16.30%	229	4.50%	74.20%	347.00%	86	0	6		85/38/38	
3:13:52	314	16.00%	195	4.80%	74.80%	320.00%	92	0				
3:22:48	320	16.10%	233	4.70%	74.10%	329.00%	88	8	6		90/38/38	
Avg	308	16.23%	236	4.58%	74.50%	340.75%	86	0	6			

100%	Ag. Bioi	mass p	ucks									
Run #1	Stack Temp	Blend:						Test date:	11/23/2015			
Time	°F	02	CO	CO2	EFF	Ex Air	NO	<b>SO2</b>	Smoke Test	Fuel feed	Fan speed	Pa
11:43:45	354	14.60%	294	6.20%	75.50%	228.00%	113	0				
11:46:27	368	12.70%	269	8.00%	78.60%	153.00%	136	0				
11:50:25	141	11.90%	233	8.80%	90.40%	131.00%	145	0	5.5			
12:55:15	366	10.50%	293	10.20%	81.60%	100.00%	156	0			85/40/25	8;+-4
Avg	307	12.43%	272	8.30%	81.53%	153.00%	138	0	5.5			

## Field Combustion Measurements October - November 2015-continued

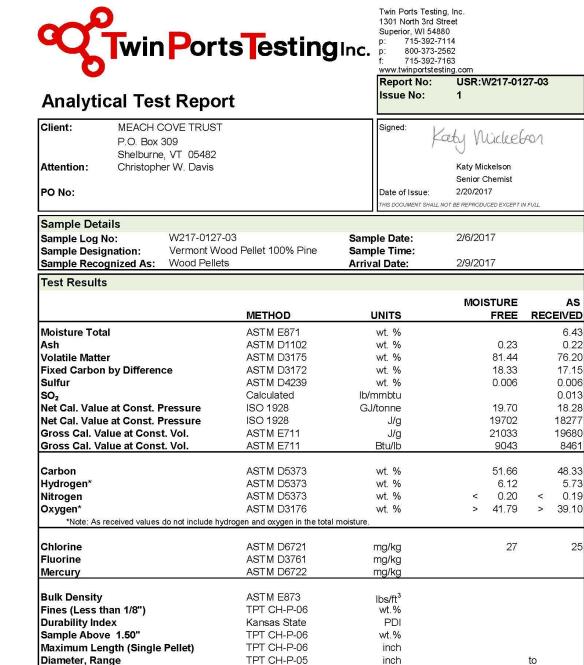


Twin Ports Testing, Inc. USR:W217-0127-01 Issue No: 1

**Analytical Test Report** 

Client:	MEACH C	COVE TRUST			Signed:	121 10			
	P.O. Box					Kachy M	ideef	601	
						/	nener	i on t	
		e, VT 05482				0			
Attention:	Christoph	er W. Davis				Katy Mich	kelson		
						Senior C	hemist		
PO No:					Date of Issu	e: 2/20/201	7		
					THIS DOCUMENT	SHALL NOT BE REPRODUC	CED EXCEPT II	FULL	
Sample Detai	ls								
Sample Log No	o:	W217-0127-0	1	Sam	ole Date:	2/6/201	7		
Sample Design		Energex, Canada 50%	Softwood/50% Hardwood	100 Contract -	ole Time:				
Sample Recog		Wood Pellets			al Date:	2/9/201	7		
Cample Recog	ilizeu As.	Wood F clicto			a Date.	2101201			
Test Results									
						MOIS	TURE		AS
			METHOD		INUTO	MOIS		DEC	
			METHOD		JNITS		FREE	REC	EIVED
Moisture Total			ASTM E871		wt. %				5.16
Ash			ASTM D1102		wt. %		0.68		0.65
Volatile Matter			ASTM D3175		wt. %		80.62		76.47
Fixed Carbon b		<b>CO</b>	ASTM D3172		wt. %		18.69		17.73
Sulfur	by Different		ASTM D4239		wt. %		0.010		0.009
				lle /m			0.010		
SO2			Calculated		nmbtu		10.05		0.021
Net Cal. Value			ISO 1928	GJ	/tonne		18.85		17.76
Net Cal. Value			ISO 1928		J/g		18854		17756
Gross Cal. Val	ue at Const	t. Vol.	ASTM E711		J/g		20165		19125
Gross Cal. Valu	ue at Const	t. Vol.	ASTM E711		Btu/lb		8670		8223
Carbon			ASTM D5373		wt. %		50.24		47.64
Hydrogen*			ASTM D5373		wt. %		6.02		5.71
Nitrogen			ASTM D5373		wt. %	<	0.20	<	0.19
Oxygen*			ASTM D3176		wt. %	>	42.85	>	40.64
	ceived values	do not include hydr	ogen and oxygen in the	total moisture			12.00		10.01
Note. As ici	cerved values	do not include nyur	ogen and oxygen in the	total moisture.					
Chlorine			ASTM D6721		mg/kg		102		97
Fluorine			ASTM D3761		mg/kg		102		57
In the state of the second second			ASTM D5701		0 0				
Mercury			AST VI D0/22		mg/kg				
Dully Danaity					2				
Bulk Density	4 10 11		ASTM E873		lbs/ft <sup>3</sup>				
Fines (Less that			TPT CH-P-06		wt.%				
Durability Inde			Kansas State		PDI				
Sample Above	1.50"		TPT CH-P-06		wt.%				
Maximum Leng	gth (Single	Pellet)	TPT CH-P-06		inch				
Diameter, Rang	ge	e	TPT CH-P-05		inch			to	
Diameter, Aver			TPT CH-P-05		inch				I
Stated Bag We			TPT CH-P-01		lbs				I
Actual Bag We			TPT CH-P-01		lbs				
¥					100		_	_	
Comments									

<b>U</b>	win Ports	estingInc.	Superior, WI 5488 p: 715-392-71 p: 800-373-25 f: 715-392-71 www.twinportstest <b>Report No:</b> <b>Issue No:</b> <i>This report replaces all p</i>	114 162 63 ing.com USR:W217-0127-01 1
Client: Attention: PO No:	MEACH COVE TRUST P.O. Box 309 Shelburne VT Christopher W. Davis	05482	Signed:	Katy Mickelson Senior Chemist 2/20/2017
			Checking and and an approximations	OT BE REPRODUCED EXCEPT IN FULL
Sample Detai Sample Log No Sample Design Sample Recog	et in the second	ood/50% Hardwood Samp	ble Date: ble Time: al Date:	2/6/2017 2/9/2017
Test Results				
		H FUSION - ASTM D1857		
	Initial Def. Temp. Softening Temp. Hemispherical Temp. Fluid Temp.	Reducing Atmosphere	2530 ° F 2600 ° F 2625 ° F 2630 ° F	
	nitial Def. Temp. Softening Temp. Hemispherical Temp. Fluid Temp.	Oxidizing Atmosphere	2500 ° F 2565 ° F 2575 ° F 2625 ° F	
	MINERAL A	NALYSIS OF ASH - ASTM	D3682	
	Silicon Dioxide in Ash Aluminum Oxide in Ash Titanium Dioxide in Ash Iron Oxide in Ash Calcium Oxide in Ash Calcium Oxide in Ash Potassium Oxide in Ash Sodium Oxide in Ash Sulfur Trioxide in Ash Phosphorus Pentoxide in Ash Barium Oxide in Ash Barium Oxide in Ash Manganese Dioxide in Ash Undetermined Total		wt.           wt.	%       %       %       %       %       %       %       %       %       %       %       %       %       %       %       %       %       %



TPT CH-P-05

TPT CH-P-01

TPT CH-P-01

inch

lbs

lbs

Diameter, Average

Stated Bag Weight

Actual Bag Weight

Comments

75

AS

6.43

0.22

76.20

17.15

0.006

0.013

18.28

18277

19680

8461

48.33

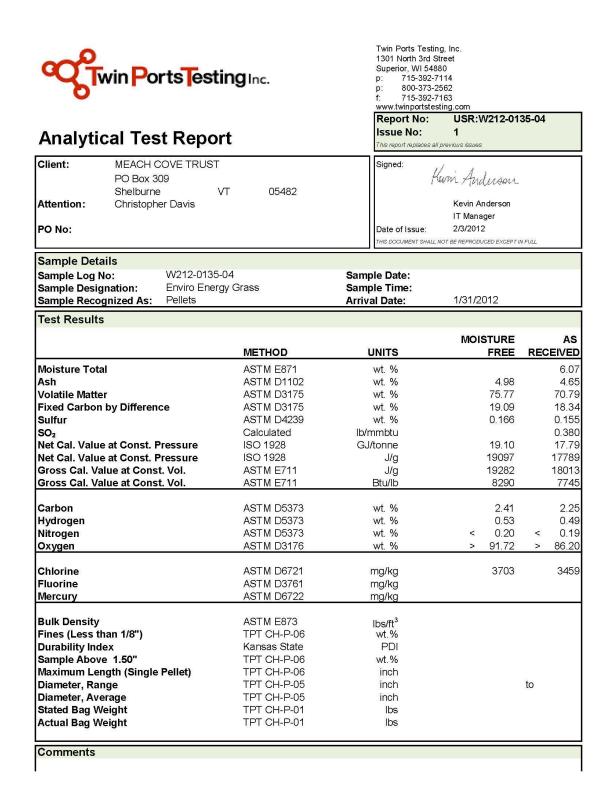
5.73

0.19

25

39.10

	win Ports estin	Superior, WI 54880           p:         715-392-7114           p:         800-373-2562           f:         715-392-7163           www.twinportstesting.com           Report No:           USR:W217-0127-03           Issue No:           1           This report replaces all previous issues
Client: Attention: PO No:	MEACH COVE TRUST P.O. Box 309 Shelburne VT 05482 Christopher W. Davis	Signed: Katy Mickelson Senior Chemist Date of Issue: 2/20/2017 THIS DOCUMENT SHALL NOT BE REPRODUCED ENCEPT IN FULL
Sample Detail Sample Log No Sample Design Sample Recog	o: W217-0127-03 nation: Vermont Wood Pellet 100% Pine	Sample Date: 2/6/2017 e Sample Time: Arrival Date: 2/9/2017
Test Results	ASH FUSION - AS	STM D1857
	Reducing Atmo Initial Def. Temp. Softening Temp. Hemispherical Temp. Fluid Temp. Oxidizing Atmo Initial Def. Temp. Softening Temp. Hemispherical Temp. Fluid Temp.	2680 ° F >2680 ° F >2680 ° F >2680 ° F
	MINERAL ANALYSIS OF A Silicon Dioxide in Ash Aluminum Oxide in Ash Titanium Dioxide in Ash Iron Oxide in Ash Calcium Oxide in Ash Calcium Oxide in Ash Potassium Oxide in Ash Sodium Oxide in Ash Sodium Oxide in Ash Sulfur Trioxide in Ash Strontium Oxide in Ash Barium Oxide in Ash Manganese Dioxide in Ash Undetermined Total	ASH - ASTM D3682 wt. % wt. %



Ŭ		ts esting Inc.		Twin Ports Testing           1301 North 3rd Str           Superior, WI 54880           p:         715-392-71           p:         800-373-25           f:         715-392-71           www.twinportstesti           Report No:           Issue No:	eet 0 14 62 63
Analytic	alles	t Report		This report replaces all p	
Client: Attention:	MEACH C PO Box 30 Shelburne Christophe	VT 05482	2	Signed:	win Anderson Kevin Anderson
PO No:	Christophe			Date of Issue: THIS DOCUMENT SHALL NO	IT Manager 2/3/2012 Dr Be REPRODUCED EXCEPT IN FULL
Sample Detai	ls				
Sample Log No Sample Desigr Sample Recog	o: nation:	W212-0135-04 Enviro Energy Grass Pellets	Sam	ple Date: ple Time: al Date:	1/31/2012
Test Results					
		ASH FUSION	- ASTM D1857		
	Initial Def. Softening Hemisphe Fluid Tem	Temp. Temp. rical Temp.	Atmosphere	2340 ° F 2420 ° F 2470 ° F 2520 ° F	
	Initial Def. Softening Hemisphe	Temp.	Atmosphere	2430 ° F 2500 ° F 2550 ° F	
	Fluid Tem			2610 ° F	
	-	MINERAL ANALYSIS	OF ASH - ASTM		
	Aluminum	oxide in Ash I Oxide in Ash Dioxide in Ash e in Ash		wt. wt. wt. wt.	%
	Magnesiu Potassiun	Dxide in Ash m Oxide in Ash n Oxide in Ash vide in Ash		wt. wt. wt.	%
	Sulfur Trie Phosphor Strontium	xide in Ash oxide in Ash us Pentoxide in Ash Oxide in Ash		wt. wt. wt. wt.	%
	Manganes Undeterm	xide in Ash se Dioxide in Ash ined		wt. wt. wt.	%
Comments	Total			wt.	%



 Twin Ports Testing, Inc.

 1301 North 3rd Street

 Superior, WI 54880

 p:
 715-392-7114

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 800-373-2562

 f:
 715-392-7163

 www.twinportstesting.com

 Report No:
 USR:W212-0135-01

 Issue No:
 1

This report replaces all previous issues

1

Issue No:

## **Analytical Test Report**

Analytic		and the second second second second		This report replaces		
Client: Attention: PO No:	MEACH C PO Box 30 Shelburne Christophe	e VT	05482	Date of Issue:	Kevin Anduraou Kevin Anderson IT Manager 2/3/2012	I FULL
Sample Deta						
Sample Log N Sample Desig Sample Recog	nation:	W212-0135-0 Meach Cove F Pellets		Sample Date: Sample Time: Arrival Date:	1/31/2012	
Test Results	i i					
			METHOD	UNITS	MOISTURE FREE	AS RECEIVEI
Moisture Tota	d		ASTM E871	wt. %		8.5
Ash			ASTM D1102	wt. %	4.54	4.1
Volatile Matte			ASTM D3175	wt. %	77.41	70.3
Fixed Carbon	by Differen	ce	ASTM D3175	wt. %	17.95	16.8
Sulfur			ASTM D4239	wt. %	0.097	0.08
SO2			Calculated	lb/mmbtu		0.22
Net Cal. Value			ISO 1928	GJ/tonne	17.83	16.1
Net Cal. Value		C. (C. C. C	ISO 1928	J/g	17830	1610
Gross Cal. Va	lue at Const	t. Vol.	ASTM E711	J/g	19102	1737
Gross Cal. Va	lue at Const	t. Vol.	ASTM E711	Btu/lb	8213	746
Carbon			ASTM D5373	wt. %	46.39	42.1
Hydrogen			ASTM D5373	wt. %	5.84	5.3
Nitrogen			ASTM D5373	wt. %	0.51	0.4
Oxygen			ASTM D3176	wt. %	42.62	39.3
Chlorine			ASTM D6721	mg/kg	1041	94
Fluorine			ASTM D3761	mg/kg	1041	54
Mercury			ASTM D6722	mg/kg		
				2		
Bulk Density	an 1/0"		ASTM E873	lbs/ft <sup>3</sup>		
Fines (Less th			TPT CH-P-06 Kansas State	wt.% PDI		
Durability Inde Sample Above			TPT CH-P-06	wt.%		
Sample Above Maximum Len		Pollot)	TPT CH-P-06 TPT CH-P-06	inch		
Diameter, Ran		reney	TPT CH-P-00	inch		to
Diameter, Ran Diameter, Ave			TPT CH-P-05	inch		10
Stated Bag W			TPT CH-P-03	lbs		
Actual Bag W			TPT CH-P-01	lbs		
Actual Rac We	cigill			105		

Client:       MEACH COVE TRUST PO Box 309 Shelburne       VT       05482         Attention:       Christopher Davis       Signed:       Jum Adduessi Hum Anderson IT Manager Date of Issue:       Z220212 Trest Covert Statut Sta	Client:       MEACH COVE TRUST PO Box 309 Shelburne       VT       05482         Attention:       Christopher Davis       Figned:       Kevin Anderson IT Menager         PO No:       Sample Details       Sample Date:       242012         Sample Details       Sample Date:       Sample Date:       Sample Date:         Sample Details       Meach Cove Reed Canary       Sample Date:       1/31/2012         Sample Recognized as:       Pellets       Arrival Date:       1/31/2012         Test Results       ASH FUSION - ASTM D1857       Reducing Atmosphere       1/31/2012         Initial Def. Temp.       2430 ° F       Pellets       1/31/2012         Oxidizing Atmosphere       Initial Def. Temp.       2450 ° F       Pellets         Initial Def. Temp.       2450 ° F       Pellet O ° F       Pellet O ° F         Oxidizing Atmosphere       Initial Def. Temp.       2450 ° F       Pellet O ° F         Initial Def. Temp.       2450 ° F       Pellet O ° F       Pellet O ° F         Softening Temp.       2450 ° F       Pellet O ° F       Pellet O ° F         Softening Temp.       2450 ° F       Pellet ° F       Pellet ° F         Memispherical Temp.       2450 ° F       Pellet ° F       Pellet ° F         Softening Te	•	vin PortsTes			Twin Ports Testing           1301 North 3rd Str           Superior, WI 5488           p:         715-392-71           p:         800-373-25           f:         715-392-71           www.twinportstest         Report No:           Issue No:         1000000000000000000000000000000000000	eet 0 14 62 63 ng.com USR:W212-0135-01 1		
Attention:       Christopher Davis       Kevin Anderson IT Manager         PO No:       Date of Issue:       22/2012         Sample Details       Sample Date:       Sample Date:         Sample Degination:       Meach Cove Reed Canary       Sample Date:         Sample Recognized as:       Pellets       Arrival Date:       1/31/2012         Test Results       Arrival Date:       1/31/2012         Contect of Issue:       2/20 ° F         Notice Initial Def. Temp.       2/20 ° F         Softening Temp.       2/340 ° F         Hemispherical Temp.       2/340 ° F         Fluid Temp.       2/340 ° F       5/3 </th <th>Attention:       Christopher Davis       Kevin Anderson IT Manager         PO No:       Date of Issue:       227012         Sample Details       Sample Date:       Sample Date:         Sample Details       Sample Date:       Sample Date:         Sample Recognized as:       Pellets       Arrival Date:       1/31/2012         Test Results       Arrival Date:       1/31/2012         Test Results         ASH FUSION - ASTM D1857         Reducing Atmosphere         Initial Def. Temp.       2230 ° F         Softening Temp.         Softening Temp.         Softening Temp.         Softening Temp.         Cidizing Atmosphere         Initial Def. Temp.       2450 ° F         Fluid Temp.       2450 ° F         Softening Temp.         Softening Temp.         Cidizing Atmosphere         Initial Def. Temp.       2640 ° F         Fluid Temp.       2640 ° F         Softening Temp.         Softening Temp.         Cidi on Ash         MINERAL ANALYSIS OF ASH - ASTM D3882         Silicon Dixi</th> <th>ē</th> <th>MEACH COVE TRUS PO Box 309</th> <th>ЭT</th> <th></th> <th>Signed:</th> <th>1</th>	Attention:       Christopher Davis       Kevin Anderson IT Manager         PO No:       Date of Issue:       227012         Sample Details       Sample Date:       Sample Date:         Sample Details       Sample Date:       Sample Date:         Sample Recognized as:       Pellets       Arrival Date:       1/31/2012         Test Results       Arrival Date:       1/31/2012         Test Results         ASH FUSION - ASTM D1857         Reducing Atmosphere         Initial Def. Temp.       2230 ° F         Softening Temp.         Softening Temp.         Softening Temp.         Softening Temp.         Cidizing Atmosphere         Initial Def. Temp.       2450 ° F         Fluid Temp.       2450 ° F         Softening Temp.         Softening Temp.         Cidizing Atmosphere         Initial Def. Temp.       2640 ° F         Fluid Temp.       2640 ° F         Softening Temp.         Softening Temp.         Cidi on Ash         MINERAL ANALYSIS OF ASH - ASTM D3882         Silicon Dixi	ē	MEACH COVE TRUS PO Box 309	ЭT		Signed:	1		
PO No: Date of Issue: 2/3/2012 Tree document swall, what we determined out of elements out of elements out of elements out out of elements out out out of elements out	PO No:     Date of Issue:     2/3/2012 Interconnect build. Not the High Rocket and Annual View Connect Annu	Attention:					Kevin Anderson		
Sample Log No:     W212-0135-01 Meach Cove Reed Canary     Sample Time: Sample Time:       Sample Recognized as:     Pellets     Arrival Date:     1/31/2012   Test Results       ASH FUSION - ASTM D1857       Reducing Atmosphere       Initial Def. Temp.     230 ° F       Softening Temp.     2450 ° F       Fluid Temp.     2520 ° F       Oxidizing Atmosphere       Initial Def. Temp.     2340 ° F       Fluid Temp.     2450 ° F       Fluid Temp.     2520 ° F       Oxidizing Atmosphere     Initial Def. Temp.       Initial Def. Temp.     2340 ° F       Fluid Temp.     2640 ° F       Softening Temp.     2640 ° F       Fluid Temp.     2640 ° F       Softening Temp.     2640 ° F       Silicon Dioxide in Ash     wt %       Aluminum Oxide in Ash     wt %       Magnesium Oxide in Ash     wt %       Magnesium Oxide in Ash     wt %       Sodium Oxide in Ash     wt %       Magnesium Oxide in Ash     wt %       Magnesium Oxide in Ash     wt %       Sodium Oxide in Ash     wt %       Sulfur Trioxide in Ash	Sample Log No:     W212-0135-01 Meach Cove Reed Canary     Sample Time: Sample Recognized as:       Pellets     Arrival Date:     1/31/2012   Test Results       Ash FUSION - ASTM D1857       Reducing Atmosphere       Initial Def. Temp.     2340 ° F       Softening Temp.     2450 ° F       Fluid Temp.     2450 ° F       Softening Temp.     2450 ° F       Fluid Temp.     2450 ° F       Softening Temp.     2450 ° F       Fluid Temp.     2640 ° F       Softening Temp.     2640 ° F       Fluid Temp.     2640 ° F       Softening Temp.     2640 ° F       Fluid Temp.     2640 ° F       Softening Temp.     2640 ° F       Fluid Temp.     2640 ° F       Softening Temp.     4550 ° F       Fluid Temp.     2640 ° F       Softening Temp.     4550 ° F       Fluid Temp.     2640 ° F       Softening Temp.     4550 ° F       Fluid Temp.     4550 ° F       Softening Temp.     4550 ° F       Softening Temp.     450 ° F	PO No:				0.0004304.0146036040300206	2/3/2012		
Sample Log No:     W212-0135-01 Meach Cove Reed Canary     Sample Time: Sample Recognized as:       Pellets     Arrival Date:     1/31/2012   Test Results       Ash FUSION - ASTM D1867       Reducing Atmosphere     Initial Def, Temp.     2230 ° F       Initial Def, Temp.     2340 ° F       Hemispherical Temp.     2450 ° F       Fluid Temp.     2520 ° F       Oxidizing Atmosphere     Initial Def, Temp.       Softening Temp.     2520 ° F       Oxidizing Atmosphere     Initial Def, Temp.       Softening Temp.     2520 ° F       Fluid Temp.     2550 ° F       Fluid Temp.     2640 ° F       MINERAL ANALYSIS OF ASH - ASTM D3682       Silicon Dioxide in Ash     wt. %       Aluminum Oxide in Ash     wt. %       Aluminum Oxide in Ash     wt. %       Magnesium Oxide in Ash     wt. %       Sodium Oxide in Ash     wt. %       Protassium Oxide in Ash     wt. %       Sulfur Trioxide in Ash     wt. %       Strontium Oxide in Ash     wt. %       Strontium Oxide in Ash     wt. %       Strontium Oxide in Ash <td< td=""><td>Sample Log No:     W212-0135-01 Meach Cove Reed Canary     Sample Time: Sample Recognized as:       Pellets     Arrival Date:     1/31/2012   Test Results       Ash FUSION - ASTM D1857       Reducing Atmosphere       Initial Def, Temp.     2340 ° F       Softening Temp.     2450 ° F       Fluid Temp.     2450 ° F       Initial Def, Temp.     2450 ° F       Fluid Temp.     2450 ° F       Fluid Temp.     2450 ° F       Initial Def, Temp.     2450 ° F       Bortening Temp.     2450 ° F       Fluid Temp.     2040 ° F       Softening Temp.     2450 ° F       Hemispherical Temp.     2040 ° F       Softening Temp.     2040 ° F       Fluid Temp.     2040 ° F       Softening Temp.     2040 ° F       Fluid Temp.     2050 ° F       Fluid Temp.     2050 ° F       Fluid Temp.     2050 ° F       Softening Temp.     400 ° F       Fluid Temp.     2040 ° F       Softening Temp.     400 ° F       Softening Temp.     400 ° F       Softening Temp.     400 °</td><th>Sample Deta</th><td>ils</td><td></td><td></td><td></td><td></td></td<>	Sample Log No:     W212-0135-01 Meach Cove Reed Canary     Sample Time: Sample Recognized as:       Pellets     Arrival Date:     1/31/2012   Test Results       Ash FUSION - ASTM D1857       Reducing Atmosphere       Initial Def, Temp.     2340 ° F       Softening Temp.     2450 ° F       Fluid Temp.     2450 ° F       Initial Def, Temp.     2450 ° F       Fluid Temp.     2450 ° F       Fluid Temp.     2450 ° F       Initial Def, Temp.     2450 ° F       Bortening Temp.     2450 ° F       Fluid Temp.     2040 ° F       Softening Temp.     2450 ° F       Hemispherical Temp.     2040 ° F       Softening Temp.     2040 ° F       Fluid Temp.     2040 ° F       Softening Temp.     2040 ° F       Fluid Temp.     2050 ° F       Fluid Temp.     2050 ° F       Fluid Temp.     2050 ° F       Softening Temp.     400 ° F       Fluid Temp.     2040 ° F       Softening Temp.     400 ° F       Softening Temp.     400 ° F       Softening Temp.     400 °	Sample Deta	ils						
ASH FUSION - ASTM D1857         Reducing Atmosphere         Initial Def, Temp.       2340 ° F         Softening Temp.       2450 ° F         Fluid Temp.       2520 ° F         Dividizing Atmosphere         Initial Def, Temp.         Oxidizing Colspan="2">Oxidizing Atmosphere         Initial Def, Temp.         Oxidizing Atmosphere         Initial Def, Temp.         Oxidizing Colspan="2">Oxidizing Atmosphere         Initial Def, Temp.         Oxidizing Atmosphere         MINERAL ANALYSIS OF ASH - ASTM D3682 <td <="" colspan="2" th=""><th>ASH FUSION - ASTM D1857         Reducing Atmosphere         Initial Def. Temp.       2340 ° F         Softening Temp.       2450 ° F         Huid Temp.       2450 ° F         Didizing Atmosphere       0         Initial Def. Temp.       2450 ° F         Softening Temp.       2450 ° F         Huid Temp.       2450 ° F         Huid Temp.       2550 ° F         Huid Temp.       2550 ° F         Huid Temp.       2640 ° F         MINERAL ANALYSIS OF ASH - ASTM D3682       0         Silicon Dioxide in Ash       wt %         Aluminum Oxide in Ash       wt %         Magnesium Oxide in Ash       wt %         Sulfur Trioxide in Ash       wt %         Manganese Dioxide in Ash       wt %</th><th>Sample Desig</th><th>nation: Meach Co</th><th></th><th>Sam</th><th>ple Time:</th><th>1/31/2012</th></td>	<th>ASH FUSION - ASTM D1857         Reducing Atmosphere         Initial Def. Temp.       2340 ° F         Softening Temp.       2450 ° F         Huid Temp.       2450 ° F         Didizing Atmosphere       0         Initial Def. Temp.       2450 ° F         Softening Temp.       2450 ° F         Huid Temp.       2450 ° F         Huid Temp.       2550 ° F         Huid Temp.       2550 ° F         Huid Temp.       2640 ° F         MINERAL ANALYSIS OF ASH - ASTM D3682       0         Silicon Dioxide in Ash       wt %         Aluminum Oxide in Ash       wt %         Magnesium Oxide in Ash       wt %         Sulfur Trioxide in Ash       wt %         Manganese Dioxide in Ash       wt %</th> <th>Sample Desig</th> <th>nation: Meach Co</th> <th></th> <th>Sam</th> <th>ple Time:</th> <th>1/31/2012</th>		ASH FUSION - ASTM D1857         Reducing Atmosphere         Initial Def. Temp.       2340 ° F         Softening Temp.       2450 ° F         Huid Temp.       2450 ° F         Didizing Atmosphere       0         Initial Def. Temp.       2450 ° F         Softening Temp.       2450 ° F         Huid Temp.       2450 ° F         Huid Temp.       2550 ° F         Huid Temp.       2550 ° F         Huid Temp.       2640 ° F         MINERAL ANALYSIS OF ASH - ASTM D3682       0         Silicon Dioxide in Ash       wt %         Aluminum Oxide in Ash       wt %         Magnesium Oxide in Ash       wt %         Sulfur Trioxide in Ash       wt %         Manganese Dioxide in Ash       wt %	Sample Desig	nation: Meach Co		Sam	ple Time:	1/31/2012
Reducing Atmosphere         Initial Def. Temp.       2340 ° F         Softening Temp.       2450 ° F         Hemispherical Temp.       2450 ° F         Fluid Temp.       2520 ° F         Oxidizing Atmosphere         Initial Def. Temp.         Oxidizing Atmosphere         Initial Def. Temp.         Softening Temp.         Oxidizing Atmosphere         Initial Def. Temp.         Softening Temp.         Oxidizing Atmosphere         Initial Def. Temp.         Oxidizing Atmosphere         Initial Def. Temp.         Softening Temp.         OXido ° F         Fluid Temp.       2640 ° F         INNERAL ANALYSIS OF ASH - ASTM D3682         Silicon Dioxide in Ash         wt %         Algo ° F         Silicon Dioxide in Ash         wt %         Algo ° F         Silicon Dioxide in Ash         wt %         MINERAL ANALYSIS OF ASH - ASTM D3682         Silicon Dioxide in Ash	Reducing Atmosphere         Initial Def. Temp.       2340 ° F         Softening Temp.       2450 ° F         Hemispherical Temp.       2520 ° F         Oxidizing Atmosphere         Initial Def. Temp.         Dividizing Atmosphere         Initial Def. Temp.       2450 ° F         Softening Temp.         2450 ° F         Hemispherical Temp.       2450 ° F         Fluid Temp.       2640 ° F         Softening Temp.         2640 ° F       Fluid Temp.         Softening Temp.         2640 ° F         MINERAL ANALYSIS OF ASH - ASTM D3682         Silicon Dioxide in Ash         Ather Softening Temp.         2640 ° F         Fluid Temp.         Divide in Ash         Ather Soften Softening Temp.         Colspan="2">Colspan= 2"Silicon Dioxide in Ash         Allow to %         Silicon Dioxide in Ash         Ather Soften S	Test Results							
Reducing Atmosphere         Initial Def. Temp.       2340 ° F         Softening Temp.       2450 ° F         Hemispherical Temp.       2450 ° F         Fluid Temp.       2520 ° F         Oxidizing Atmosphere         Initial Def. Temp.         Oxidizing Atmosphere         Initial Def. Temp.         Softening Temp.         Oxidizing Atmosphere         Initial Def. Temp.         Softening Temp.         Oxidizing Atmosphere         Initial Def. Temp.         Oxidizing Atmosphere         Initial Def. Temp.         Softening Temp.         OXido ° F         Fluid Temp.       2640 ° F         INNERAL ANALYSIS OF ASH - ASTM D3682         Silicon Dioxide in Ash         wt %         Algo ° F         Silicon Dioxide in Ash         wt %         Algo ° F         Silicon Dioxide in Ash         wt %         MINERAL ANALYSIS OF ASH - ASTM D3682         Silicon Dioxide in Ash	Reducing Atmosphere         Initial Def. Temp.       2340 ° F         Softening Temp.       2450 ° F         Hemispherical Temp.       2520 ° F         Oxidizing Atmosphere         Initial Def. Temp.         Dividizing Atmosphere         Initial Def. Temp.       2450 ° F         Softening Temp.         2450 ° F         Hemispherical Temp.       2450 ° F         Fluid Temp.       2640 ° F         Softening Temp.         2640 ° F       Fluid Temp.         Softening Temp.         2640 ° F         MINERAL ANALYSIS OF ASH - ASTM D3682         Silicon Dioxide in Ash         Ather Softening Temp.         2640 ° F         Fluid Temp.         Divide in Ash         Ather Soften Softening Temp.         Colspan="2">Colspan= 2"Silicon Dioxide in Ash         Allow to %         Silicon Dioxide in Ash         Ather Soften S								
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Hemispherical Temp.       2450 ° F         Fluid Temp.       2520 ° F         Oxidizing Atmosphere         Initial Def. Temp.         Softening Temp.         2450 ° F         Hemispherical Temp.         2550 ° F         Fluid Temp.         DINERAL ANALYSIS OF ASH - ASTM D3682         MINERAL ANALYSIS OF ASH - ASTM D3682         Silicon Dioxide in Ash         wt. %         Aluminum Oxide in Ash       wt. %         Aluminum Oxide in Ash       wt. %         Galcium Oxide in Ash       wt. %         Potassium Oxide in Ash       wt. %         Potassium Oxide in Ash       wt. %         Sulfur Trioxide in Ash       wt. %         Sulfur Trioxide in Ash       wt. %         Sulfur Trioxide in Ash       wt. %         Strontium Oxide in Ash       wt. %         Barium Oxide in Ash       wt. %         Manganese Dioxide in Ash       wt. %         Manganese Dioxide in Ash       wt. %	Hemispherical Temp.       2450 ° F         Fluid Temp.       2520 ° F         Oxidizing Atmosphere         Initial Def, Temp.       2450 ° F         Softening Temp.       2450 ° F         Hemispherical Temp.       2550 ° F         Fluid Temp.       2640 ° F         MINERAL ANALYSIS OF ASH - ASTM D3682         Silicon Dioxide in Ash         Aluminum Oxide in Ash       wt %         Aluminum Oxide in Ash       wt %         Iton Oxide in Ash       wt %         Calcium Oxide in Ash       wt %         Potassium Oxide in Ash       wt %         Sodium Oxide in Ash       wt %         Potassium Oxide in Ash       wt %         Sulfur Trioxide in Ash       wt %         Barium Oxide in Ash       wt %         Manganese Dioxide in Ash       wt %<								
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Analytical Test Report		Twin Ports Testin           1301 North 3rd S           Superior, WI 548           p:         715-392-7           p:         800-373-2           f:         715-392-7           www.twinportstes           Report No:           Issue No:           This report replaces all	Treet 80 114 562 163 ting.com USR:W212-01 1	35-02
Client: MEACH COVE TRUST PO Box 309 Shelburne V Attention: Christopher Davis PO No:	T 05482	Signed:	www. Anduson. Kevin Anderson IT Manager 2/3/2012 NOT BE REPRODUCED EXCEPT II	H FULL
Sample Details Sample Log No: W212-0135-I Sample Designation: Meach Cove Sample Recognized As: Pellets	02 Switch Grass	Sample Date: Sample Time: Arrival Date:	1/31/2012	
Test Results	METHOD	UNITS	MOISTURE	AS
Moisture Total Ash Volatile Matter Fixed Carbon by Difference Sulfur SO <sub>2</sub> Net Cal. Value at Const. Pressure Net Cal. Value at Const. Pressure Gross Cal. Value at Const. Vol. Gross Cal. Value at Const. Vol.	ASTM E871 ASTM D1102 ASTM D3175 ASTM D3175 ASTM D4239 Calculated ISO 1928 ISO 1928 ASTM E711 ASTM E711	wt. % wt. % wt. % wt. % Ib/mmbtu GJ/tonne J/g J/g Btu/lb	6.63 75.17 18.01 0.189 17.59 17593 18880 8117	8.0 6.0 17.0 0.17 0.44 15.9 1599 1720 742
Carbon Hydrogen Nitrogen Oxygen Chlorine Fluorine	ASTM D5373 ASTM D5373 ASTM D5373 ASTM D3176 ASTM D6721 ASTM D3761	wt. % wt. % wt. % mg/kg mg/kg	45.52 5.92 0.86 40.89 2517	41.6 5.2 0.7 37.9 230
Mercury Bulk Density Fines (Less than 1/8") Durability Index Sample Above 1.50" Maximum Length (Single Pellet) Diameter, Range Diameter, Average Stated Bag Weight Actual Bag Weight	ASTM D6722 ASTM D6722 ASTM E873 TPT CH-P-06 Kansas State TPT CH-P-06 TPT CH-P-06 TPT CH-P-05 TPT CH-P-05 TPT CH-P-01 TPT CH-P-01	Ibs/ft <sup>3</sup> wt.% PDI wt.% inch inch inch Ibs Ibs		to

Ŭ	vin Ports estin	gInc.	p: 80 f: 71 www.twin Report Issue N	th 3rd St WI 5488 5-392-7 10-373-29 5-392-7 portstest No: No:	reet 30 114 562 163 ting.com USR:W212-0135-02 1
Client:	MEACH COVE TRUST		This report in Signed:		previous issues
	PO Box 309			A	win Anderson
Attention:	Shelburne VT Christopher Davis	05482		Ċ	Kevin Anderson
Attention.	Chinatopher Davia				IT Manager
PO No:			Date of Is	sue:	2/3/2012
			THIS DOCUM	ENT SHALL N	NOT BE REPRODUCED EXCEPT IN FULL
Sample Detai	ls				
Sample Log N			Sample Date:		
Sample Desig			Sample Time		1010010
Sample Recog	nized as: Pellets		Arrival Date:		1/31/2012
Test Results					
	Α	SH FUSION - ASTM D18	857		
		Reducing Atmosphere	e		
	Initial Def. Temp.	5		230 ° F	
	Softening Temp.		23	860 ° F	:
	Hemispherical Temp.		24	150 ° F	
	Fluid Temp.		25	590 ° F	
		Ovidizing Atmocphore			
	Initial Def. Temp.	Oxidizing Atmosphere		335 ° F	:
	Softening Temp.		200	160 ° F	
	Hemispherical Temp.			545 ° F	
	Fluid Temp.			690 ° F	
	•				
	MINERAL	ANALYSIS OF ASH - A	STM D3682		
	Silicon Dioxide in Ash			wt.	%
	Aluminum Oxide in Ash				%
	Titanium Dioxide in Ash			wt.	
	Iron Oxide in Ash			wt.	
	Calcium Oxide in Ash			wt.	
	Magnesium Oxide in Ash			wt. wt	
	Potassium Oxide in Ash Sodium Oxide in Ash			wt.	57
	Sulfur Trioxide in Ash			wt.	
	Phosphorus Pentoxide in	Ash			%
	Strontium Oxide in Ash				%
	Barium Oxide in Ash				%
	Manganese Dioxide in As	h			%
	Undetermined			wt.	%
	Total			wt.	%
Comments					

## **Testing Methods**

The combustion testing followed the same series of steps. We would isolate the heat distribution system so that the boiler was only heating the 550 gallon buffer tank. The temperature of the buffer tank was noted before and after each test burn which allowed estimates of the efficiency of the test burns to be calculated (Callahan, 2016). The fuel feed auger was vacuumed of all prior sample residue. The firebox was manually scraped down and the cleaning cycle operated until the firebox was clear of any ash and residue from the previous burn cycle. The boiler was started and allowed to run through the typical cleaning, start up and ignition sequence. Once the boiler reached the "full load" combustion stage the Project Director would begin to take emission and smoke samples. Samples were taken at 10-15 minute intervals over the course of about an hour with the boiler operating at "full load". The data captured by the Wohler instrument and printed by the Wohler wireless printer as each sample was taken. Smoke test filters were labeled and stapled to the Wohler printouts as they were tested. We made adjustments to the air flow and fuel feed rates for the boiler during the test runs to minimize the CO levels and maximize the combustion efficiency.

Emission measurements with the Wohler A500 and the smoke tests were performed following the same process and as close to the same time interval for each test run by the Project Director for consistency. The raw data was transferred from the Wohler emission print outs and smoke test paper disks to the Excel spreadsheet manually by the Project Administrator.

USDA-NRCS-2011 Vermor	nt Conservation Ini	novation Grant (CIG	6) program
Meach Cove	Real Estate Trust	- 69-1644-11-08	
		Period 7/1/201	5 to 9/30/2015
		Current	Previous
	Current	Cumulative	Cumulative
Federal Share/Budget\$			
d. Equipment/\$32,000	\$0.00	\$43,532.80	\$43,532.80
e. Supplies/\$11,700	\$0.00	\$21,924.03	\$21,924.03
f. Contractual/\$29,700	\$0.00	\$7,943.17	\$7,943.17
Total/\$73,400	\$0.00	\$73,400.00	\$73,400.00
MCRET Cost Share/Budget\$			
a. Personnel/\$77,740	\$698.90	\$64,200.00	\$63,801.10
b. Fringe Benefits/\$36,400	\$219.88	\$21,189.71	\$20,969.83
c. Travel/\$1,500	\$0.00	\$522.54	\$522.54
e. Supplies/\$10,000	\$0.00	\$42,429.57	\$42,429.57
Total/\$125,640	\$918.78	\$128,341.82	\$127,723.04
Total Federal and MCRET	\$918.78	\$201,741.82	\$201,123.04

## Biomass Boiler vs. Oil Boiler Installation Budget Estimate

Meach Cove Farms Bi	omass Boile	r installatio	on w	orksheet		
October 2013 - Octob	er 2014				No Biomass I	boiler
					Add 2nd Oil b	oiler
Refit boiler room to V	T Code		\$	21,516.00	\$16,516.00	
Boiler + chip and pelle	et loaders		\$	41,553.00	\$-	
Rigger to install boiler			\$	1,750.00	\$-	
Add Buderus oil boiler	<sup>-</sup> (294K BTU)	& expansion	on ta	ank	\$ 5,000.00	
Add second 275 gal oi	il tank, tray &	k plumb it ι	лр		\$ 2,200.00	
Stainless steel Flue			\$	2,115.00	\$ 1,800.00	
Materials to build fue	l bins to cod	e	\$	2,100.00	\$-	
Plumbing contractor			\$	24,000.00	\$15,000.00	
Move oil boiler & inst	all tank		\$	3,000.00	\$ 3,000.00	
Additional electrical w	vork		\$	1,000.00	\$ 1,000.00	
Meach Cove labor			\$	15,000.00	\$ 7,500.00	
TOTAL			\$1	L12,034.00	\$52,016.00	
		Gallons	To	tal Cost		
Oil used 1-1-14 thru 7	-31-15	757	\$	2,844.00		
max price \$ 3.26/gal						
min price \$2.20/gal						
ave price \$2.70/gal						
				tons	cost/ton	Total Cost
Wood pellets used 10	/14/14 - 10/	30/15		16	\$269 - 279	\$4,304-4,464
Square feet heated	4,313.00					
Cubic feet heated	63,250.00					